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PREDICTION OF CRACK GROWTH IN AQUEOUS ENVIRONMENTS

Final Technical Report

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19. ABSTRACT (Continue on reverse if necessary and identify by block number) The report describes the results of a research program to simultaneously determine the mechanical and electrochemical process that occur within and near the tip of active stress corrosion and corrosion-fatigue cracks. Electrochemical/mechanical impedance analysis is one of the few techniques with this capability. Our approach was to make electrochemical/mechanical impedance measurements on HY80 steel in 3.5 wt% NaCl solutions under corrosion-fatigue conditions. The data were then analyzed by means of an AC transmission line model to determine the distribution of electrochemical and mechanical states within the crack and at the crack tip.					
The bulk (uncracked) electrochemical parameters were measured for both HY80 and Ti-6Al-4V by AC impedance techniques. The electromechanical impedance of HY80 was measured and found to be sensitive to crack wall area at frequencies above 1 Hz and more sensitive to the crack tip at mechanical frequencies below 0.1 Hz. A DC transmission line model of the growing corrosion-fatigue cracks constructed from data on HY80 undergoing corrosion-					
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fatigue was used to predict crack growth rates and potential and chemistry distributions within the crack. The predicted crack growth rates were in reasonable agreement with the experimentally measured values. The model also predicted a reasonable ΔK threshold for crack growth. At present the model treats the crack tip region rather simply, but several more realistic models exist that could be easily incorporated.

The results of this program have shown that a technique combining AC impedance, electrochemical/mechanical impedance, and transmission line modeling offers the potential to determine both the mechanical and electrochemical processes that occur within stress corrosion and corrosion-fatigue cracks. At present, it is one of the few techniques with this capability. The results did not conclusively show that the combination of AC impedance, electromechanical impedance, and transmission line modeling can be used to quantitatively predict crack growth rates because the transmission line model was not used to reproduce the electromechanical impedance. We recommend additional effort to use the transmission line model in conjunction with the electromechanical/electrochemical impedance to obtain the critical mechanical and chemical parameters at the crack tip. It is clear that, with more modeling and experimental work on a wider variety of materials, load cycles, and aqueous environments, the electrochemical/mechanical technique developed in this program can become an important research tool.



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Section 1

INTRODUCTION

1.1 BACKGROUND

The load-bearing capacity of most alloys can be degraded by a corrosive environment. Two common forms of environment-sensitive mechanical property degradation are stress corrosion cracking (SCC) and corrosion fatigue (CF). Both forms greatly influence the safety, reliability, and economics of many components used in military and commercial power generation, transportation, and energy conversion systems. Therefore, substantial effort has been made to understand environment-assisted crack growth, to identify and develop materials that have better environment resistance, and to formulate predictive models.¹⁻¹⁵

These efforts have resulted in various quantitative models being proposed for predicting SCC, CF, or other types of environment-assisted crack growth. Wei and Landes,¹⁰ for example, considered the crack growth rate in a CF situation to consist of the sum of the crack growth rate in an inert environment and the rate in the environment of interest. The Wei and Landes theory has been shown to explain adequately many features of the CF behavior of Ti and Ti-6Al-4V in NaCl solutions.¹¹ Furthermore, this work emphasized the need for a better understanding of the processes that occur at the crack tip, particularly at threshold load levels for crack growth and at low loading frequencies (< 1 Hz).

For SCC alone, Logan⁷ proposed a model for cracking in aqueous environments based on a slip-dissolution mechanism at the crack tip. This mechanism, now widely accepted,⁵⁻⁷ relates crack growth to the enhanced anodic dissolution current at the crack tip resulting from the intermittent mechanical rupture of an environmentally created film at the crack tip.

Logan's model has been modified to include a variety of rate-controlling processes that include repassivation rate, microcrack, solution renewal, and critical charge concepts.⁸ If the processes occurring within the crack were better understood, it would be possible to determine the appropriate slip-dissolution model for any given material, environment, and load application.

Quantitative modeling of the cracking process is difficult because it involves complex interactions between the cracking material, the environment, and the applied load. Because specimen microstructure, surface chemistry, electrochemistry, and loading conditions are expected to influence cracking behavior, they should be accounted for in attempts to model crack growth. Clearly, simultaneous characterization of the mechanical and electrochemical state at the crack tip is required for development of a reliable, predictive crack growth model.

The mechanical state at the crack tip is usually described in these models using classical fracture mechanics parameters such as the linear elastic stress intensity (K parameter)^{16,17} or, more recently, the elastic-plastic stress intensity (J parameter).^{18,19} Unfortunately, the electrochemical state of the crack tip is not so easily characterized because, until recently, no reliable experimental method existed that could either provide measurements directly within the crack or convert measurements made external to the crack into crack tip parameters. Some attempts have been made to measure the local chemistries that develop at crack tips by using microanalytical chemical techniques on specimens that are actually cracking or on artificial crevices that had been constructed to simulate stress corrosion cracks. However, most of the past crack growth models have used electrochemical data obtained on bulk specimens and have assumed that such data, for example, the free corrosion potential, are representative of values inside the crack, or these bulk values were extrapolated to crack tip values by means of some postulated model. However, crack growth rates predicted by such models can be several orders of magnitude different from those actually observed.^{20,21}

One possible method for evaluating the electrochemical state of material near a crack tip is the AC impedance technique. This technique, under development for the past several years,²²⁻²⁶ has only recently been applied to the problem of environmentally assisted cracking. This approach shows promise for determining crack tip electrochemical parameters by applying the transmission line model to deconvolve the measured AC impedance spectra of growing cracks.

1.2 PROGRAM OBJECTIVES

The above background discussion highlights the need to characterize simultaneously the electrochemical and mechanical states in a growing stress corrosion or corrosion fatigue crack. Thus, the objective of this research program was to generate electrochemical and mechanical data for actively growing corrosion fatigue cracks and then use these data to develop a preliminary predictive model for SCC and CF.

To accomplish these objectives we used standard fracture mechanics methods and analyses to characterize the mechanical state of the crack in Ti-6Al-4V and HY-80 steel in 3.5% NaCl solution and the AC impedance technique to characterize the electrochemical state. The electrochemical and mechanical data were used to calibrate a transmission line model, and this model was then used to predict quantitatively the electrochemical and mechanical state-at the tip of an actively growing crack.

This report describes the results of our efforts to meet these objectives. Section 2 describes the development of the transmission line model. Section 3 reviews the electrochemical and mechanical experimental techniques employed in this program and the results obtained. In Section 4 the transmission line model is presented along with the experimental data used to develop a predictive model for crack growth. Section 5 outlines the conclusions and recommendations for additional work.

Section 2

DEVELOPMENT OF THE DISCRETE TRANSMISSION LINE MODEL

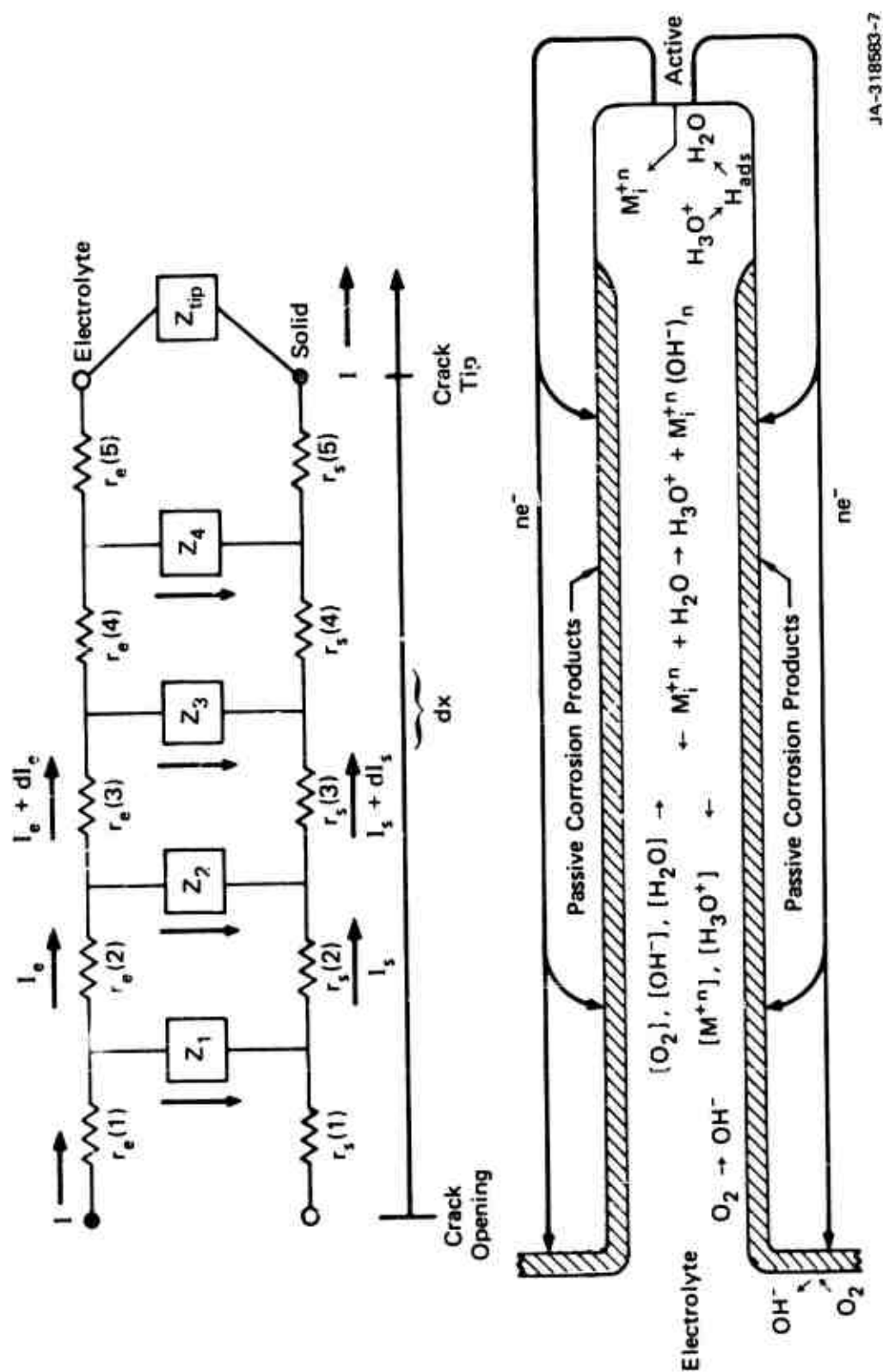
In the discrete transmission line model the stress corrosion or corrosion-fatigue crack is treated as a cracked electrode. The solid and electrolyte phases in the cracked electrode are represented by resistance elements parallel to the direction of the corrosion current flux, and the interfacial resistance is represented by an impedance distributed between the other two resistances. The electrode may be treated as "one-dimensional" if the potential (E), current flux (I), and reactant concentrations (c) vary only with the depth within the crack and not with the lateral position along the crack. In this case, the local values of E, I, and c may be replaced by their average values in a line perpendicular to the crack plane.

Ksenzheck and Stender²⁷ discussed the conditions that are applicable to transforming a three-dimensional problem into a one-dimensional one. The mathematical model for the electrical representation shown in Figure 1 requires solutions to a set of differential equations of the following form:

$$\frac{d^2 I_s}{dx^2} + \frac{d \ln(Z)}{dx} \frac{d I_s}{dx} - \frac{(r_s + r_e) I_s}{Z} = - \frac{r_e I}{Z} \quad (1)$$

$$\frac{d^2 I_e}{dx^2} + \frac{d \ln(Z)}{dx} \frac{d I_e}{dx} - \frac{(r_s + r_e) I_e}{Z} = - \frac{r_s I}{Z} \quad (2)$$

$$\frac{d^2 \Delta E}{dx^2} - \frac{(r_s + r_e)}{Z} \Delta E = 0 \quad (3)$$



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FIGURE 1 TRANSMISSION LINE MODEL FOR A CRACK IN AN AQUEOUS ENVIRONMENT

where subscripts e and s refer to the electrolyte and solid phases, Z is the interfacial impedance, x is distance into the crack, r is the resistance, $I = I_s + I_e$, and $\Delta E = E_a - E_e$.

For the simplest set of boundary conditions shown in Figure 1, corresponding to an electrolyte-filled right cylindrical crack in which r_s and r_e are independent of x and the solid and electrolyte phase current contacts are diametrically opposed, the transmission line impedance Z_{tl} is given by ²⁸

$$Z_{tl} = \frac{4r_s r_e + (r_s^2 + r_e^2) (e^{\gamma l} + e^{-\gamma l})}{(r_s + r_e) (e^{\gamma l} - e^{-\gamma l})} + \frac{r_s r_e l}{r_s + r_e} \quad (4)$$

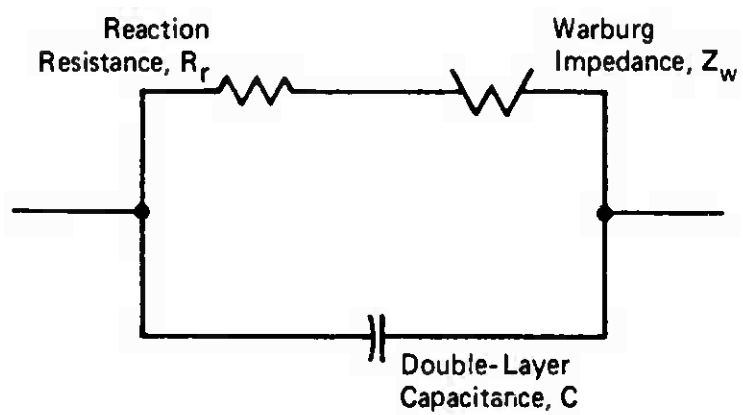
where l is the current crack length, and

$$\gamma = [(r_s + r_e)/Z_i]^{1/2} \quad (5)$$

The interfacial impedance, Z_i , in equation (5) is equivalent to that at a plane-parallel electrode. That is, it contains the information that would be available if it were possible to determine the electrochemical kinetic properties of each infinitesimal element, dx , of the electrode thickness in the x direction.

The conventional²²⁻²⁴ equivalent circuit for Z_i is shown in Figure 2. The components of this circuit contain the electrochemical kinetic parameters that are important in evaluating the behavior of a cracked electrode. Brief descriptions of these parameters follow.

Double-Layer Capacitance, C . The double-layer capacitance, C , is directly proportional to the area of the electrolyte/solid phase interface. Thus, given a knowledge of the double-layer capacitance per unit area, C' , under the prevailing conditions of reactant concentration, temperature, and potential, one can determine C by deconvolving the measured transmission line impedance. This value of C can then be used to estimate the total wetted area per unit electrode thickness,²⁸



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FIGURE 2 INTERFACIAL IMPEDANCE ELEMENT;
RANDLES' EQUIVALENT CIRCUIT

which we define as A' . Values of C' may be available from the literature or can be measured directly for a plane-parallel electrode of known area.

Warburg Coefficient, σ . At moderate frequencies ($\omega > 1 \text{ Hz}$), the Warburg impedance, Z_w , can be expressed as ^{22,24,29}

$$Z_w = \sigma(1 - j)\omega^{1/2} \quad (6)$$

where

$$\sigma = \frac{RT}{n^2 F^2 c A'' (2D)^{1/2}} \quad (7)$$

in which c is the reactant concentration and A'' expresses the electrode electrolyte area per unit length that is actively engaged in reaction. The other parameters in equation (7) have their usual meanings. The relationship between A' and A'' can be used to define an area efficiency that accounts for the presence of passive zones, which do not contribute to the cell current during crack growth.

Diffusion Layer Thickness, δ . At the limit of low frequency, an apparent resistive amount to the Warburg impedance is observed.²⁹⁻³² This resistance defines the steady-state DC operating behavior, and its value may be used in conjunction with σ to calculate the effective diffusion layer thickness, δ . In the derivation of equation (6), semi-infinite linear diffusion was assumed. However, in the wide regions near the crack mouth, natural convection will limit the thickness of the diffusion layer, whereas in the narrower regions near the crack tip, the dimension of the diffusion layer is proportional to the crack opening. Thus, we can account for the steady-state DC behavior^{22,30-35} in the model of the cracked electrode by introducing the Nernst diffusion layer thickness as a boundary condition.

Interfacial Reaction Resistance, R_r . The reaction resistance together with A'' and δ can be used to obtain information regarding the

electrode kinetics^{14,29,36} within the cracked electrode. The exchange current density, i_0 , can be determined from the relationship

$$R_T = RT/nFA'i_0 \quad (8)$$

When used in conjunction with the Stern-Geary relationship,³⁷ R_T provides a measure of the instantaneous corrosion rate within the crack.

Electrolyte Resistance, r_e . The electrolyte resistance per unit length in the cracked electrode, r_e , gives a measure of the amount, composition, and distribution of electrolyte in the crack. The electrolyte resistance is controlled primarily by the crack width and to a smaller extent by the diffusion of reactant species from the bulk electrolyte and the diffusion of reaction products from the crack tip.

Solid Electrode Resistance, r_s . The solid phase resistance per unit length in the cracked electrode, r_s , provides a measure of the resistive component in the cracked electrode. Reduction of the impedance data to obtain the parameters of interest for cracked electrodes involves applying nonlinear regression analysis to an impedance model or equivalent circuit. Broers and coworkers³⁸⁻⁴⁰ demonstrated the applicability of the transmission line model for characterizing porous electrodes in molten carbonate fuel cells, and we believe that these methods can be applied to a growing SC or CF crack.

An additional impedance element, Z_{tip} , has been included in Figure 1 to account for the special electrochemical characteristics of the crack tip. For example, if the crack grows by a mechanism of film rupture and anodic dissolution at the crack tip, then Z_{tip} can be represented as a special case of the equivalent circuit in Figure 2, with R_T determined by the exchange current density for metal dissolution (possibly involving terms for precipitation of oxide and repassivation). Under the conditions of a cyclic mechanical load, the area term A' in equation (8) must also be given as a periodic function about a mean value, A'_0 . In the simplest case, A' would be a linear function of the mechanical load or crack-opening displacement. Thus,

$$A_{tip} = A_{tip}^0 \sin(\omega t + \phi) \quad (9)$$

where ω is the frequency of the load variation, and ϕ is the phase delay between load variation and film rupture.

Equation (9) suggests a second method of evaluating the electrochemistry of the crack tip environment, using the transmission line model. Under a steady electrical bias (a small DC voltage more positive than the free corrosion potential), a DC current can be made to flow from the specimen to a suitable counterelectrode. This current originates with the anodic dissolution at the crack tip and is given by

$$I(\omega t) = \eta / R_r \quad (10)$$

where $\eta = V_{applied} - V_{free\ corrosion}$.

Substituting equation (9) into equation (8) and then substituting the resulting expression for R_r into equation (10) yields

$$I(\omega t) = \frac{\eta n F A_{tip}^0 \sin(\omega t + \phi) i_o}{RT} \quad (10a)$$

This expression for $I(\omega t)$ describes the crack tip current expected for cyclic load conditions.

This can be viewed as a sinusoidal current source originating at the crack tip. The current source is situated where the interfacial reaction resistance (R_r in Figure 2) is placed in Z_{tip} in Figure 1.

Alternatively, we can define an electrochemical/mechanical impedance,

$$Z_{em} = Z/I \quad (11)$$

which may be examined as a function of the frequency (and amplitude) of the mechanical load variation.

The advantage of an electrochemical/mechanical impedance study is that the perturbation is applied exactly at the point of interest (the crack tip). In the alternative method, a variable frequency electrical potential variation is applied to the mouth of a crack in a specimen cycled with a constant frequency mechanical load; however, this results in a perturbation that decreases in amplitude at the crack tip as the crack increases in length.

Section 3

EXPERIMENTAL METHODS AND RESULTS

3.1 TEST MATERIALS AND ENVIRONMENT

Two test materials were used in this program: a titanium alloy (Ti-6Al-4V) and a medium-strength low-alloy steel (HY 80). These materials were selected because of their possible application in submarine hull structures and for the range of electrochemical and corrosion-fatigue behavior these materials cover. The chemistry and mechanical properties of the Ti-6Al-4V and HY 80 are given in Tables 1 and 2, and the microstructures are shown in Figure 3. Note that the HY 80 has a bainitic microstructure typical of a quench and temper heat treatment, whereas the Ti-6Al-4V exhibits an alpha-beta structure typical of the mill-produced hot-rolled and annealed condition.

The test environment selected for this program was the standard 3.5% NaCl solution. This environment was created by dissolving the appropriate amount of reagent grade NaCl in deionized water. This solution was aerated and continuously refreshed into the test chamber at a rate of about 1 liter/hr.

3.2 ELECTROCHEMICAL/MECHANICAL EXPERIMENTS

To generate the electrochemical/mechanical data needed for the transmission line model, we performed three types of AC impedance-based experiments in this program: (1) planar (uncracked) electrode experiments to characterize the bulk electrochemical properties of the materials without any mechanical loading, (2) cracked electrode experiments to characterize the voltage/current response during active loading of a crack, and (3) cracked electrode electromechanical impedance experiments to characterize the voltage displacement response during active loading of a crack.

Table 1

PROPERTIES OF HY80 STEEL
(5.08-cm-thick plate, Mil-S-16216H, ASTM Grain Size 8)

Elemental Analysis		Heat Treatment	Mechanical Properties ^a	
Element	wt%		Parameter	Value
C	0.17	Austentized at 1010°C for 120 minutes and water quenched;	σ_{ys}	87.8 ksi
Mn	0.34		σ_{uts}	106 ksi
P	0.010		%E	23.7%
S	0.10	Tempered at 682°C for 120 minutes and air cooled.	%RA	66.7%
Si	0.23		CVN	95 ft-lb
Cr	1.56			at -120°F
Ni	2.88			
Mo	0.24			
Cu	0.17			
Ti	0.001			
V	0.001			

^aDefinitions:

σ_{ys} = 0.2% offset yield strength.

σ_{uts} = ultimate tensile strength.

%E = percent total tensile elongation to failure.

%RA = reduction in area of necked region at fracture.

CVN = charpy V-notch impact energy; CVN was determined under the following conditions: Type A, notch V, full size, longitudinal orientations.

Table 2

PROPERTIES OF T1-6Al-4V
(AMS 4911, 40.6-cm-thick plate)

Elemental Analysis		Heat Treatment	Mechanical Properties ^a	
Element	wt%		Parameter	Value
C	0.03	Hot rolled and annealed	σ_{ys}	131 ksi
Al	6.25		σ_{uts}	143 ksi
Fe	0.07		$\%E$	12.4
V	3.95		$\%RA$	26.3
O ₂	0.162			
N ₂	0.015			
H ₂	0.002			

^aDefinitions:

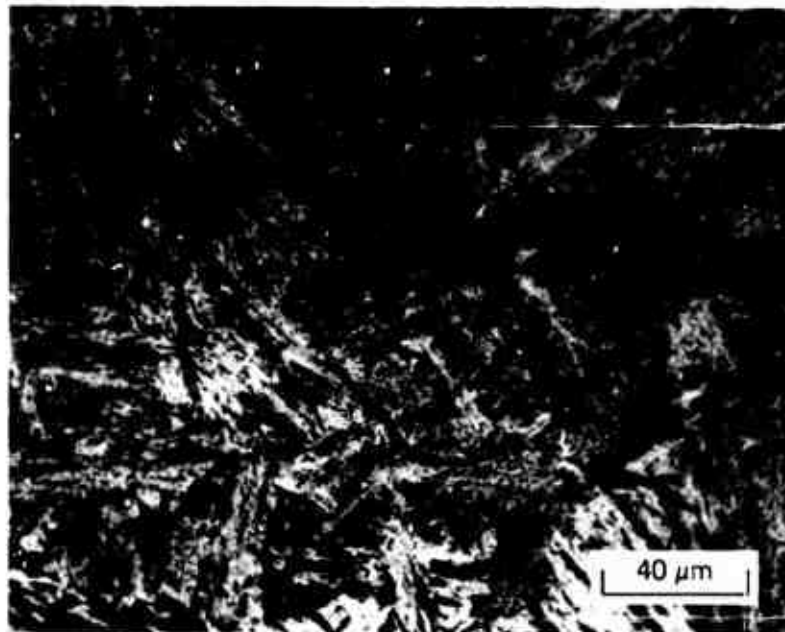
σ_{ys} = 0.2% offset yield strength.

σ_{uts} = ultimate tensile strength.

$\%E$ = percent total tensile elongation to failure.

$\%RA$ = percent reduction in area of necked region at fracture.

CVN = charpy V-notch impact energy.



(a) HY80 (Looking onto plane of crack path)



(b) Ti-6Al-4V (Looking onto plane of crack path)

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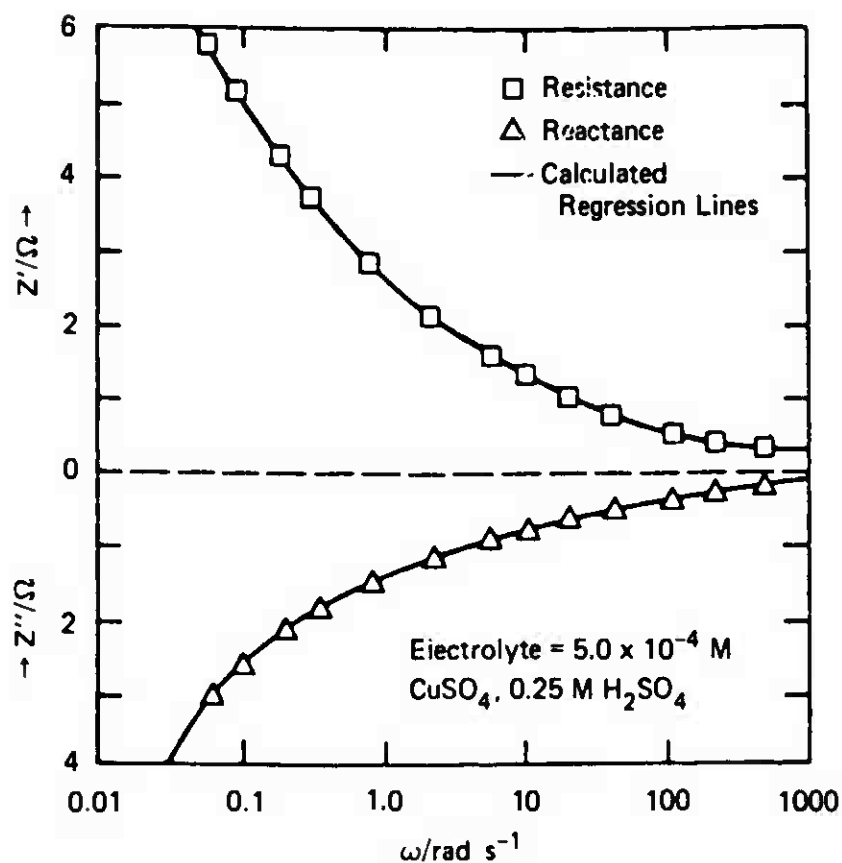
FIGURE 3 MICROSTRUCTURE OF ALLOYS TESTED

The methods used and the results obtained for each of these three experiments are discussed in the following subsections. However, before discussing these experiments, it is important first to review some of the advantages and limitations encountered when applying these electrochemical techniques.

To calculate accurately the many electrochemical parameters that can be obtained from AC measurements, it is necessary to obtain high-precision impedance measurements over a wide range of frequencies, particularly at very low frequencies. The unavailability of adequate instrumentation has been the principal limitation to the characterization of cracked or porous systems by AC techniques and is largely responsible for the only modest success of Broers and coworkers.³⁸⁻⁴⁰ More recently, Mund et al.⁴¹ analyzed the performance of hydrogen electrodes in alkaline fuel cells systems from AC impedance measurements applied to a transmission line model.

The current work of Hills and coworkers⁴²⁻⁴⁴ provides good verification for the application of the transmission line model and the extension of equilibrium AC measurements for predicting the steady-state electrochemical parameters. In one set of experiments, the interfacial impedance components were calculated from the measured impedance of a packed bed of graphite spheres using the transmission line model, and the results were compared with the interfacial impedance measured directly for a single sphere.

Figure 4 shows the impedance data obtained for a packed-bed electrode superimposed on the least-squares best fit of data to equation (4). The tabulated values of the double-layer capacitance, Warburg coefficient, and exchange current density for the packed bed were calculated from this regression fit. These values were compared with the interfacial impedance parameters measured directly for a single graphite sphere isolated from the bed. The substantial agreement between the two sets of calculated impedance parameters is strong verification for the applicability of the transmission line model to characterizing porous or cracked electrodes.



Derived Parameters	Packed Bed	Single Sphere	
C_d	154×10^{-6}	130×10^{-6}	F cm^{-2}
σ	120	120	$\Omega \text{ s}^{-1/2} \text{ cm}^{-2}$
i_o	6.3×10^{-3}	12.4×10^{-3}	cm^{-2}

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FIGURE 4 MEASURED AND CALCULATED IMPEDANCE SPECTRA
FOR A BED OF 600- μm GRAPHITE SPHERES
(From Reference 4)

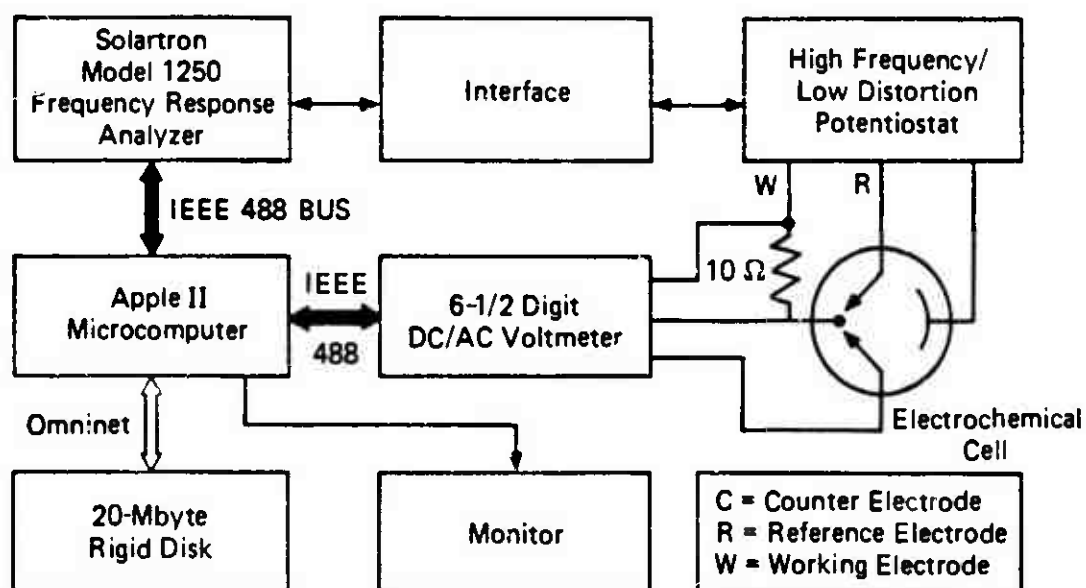
This previous research clearly shows that many important operating parameters of porous and cracked electrodes are contained within the measured impedance dispersion. However, two factors are fundamental in the application of this method to the in situ determination of electrode characteristics. First, impedance measurements must be of sufficient precision (better than 0.1% for each impedance component),²² and second, the measurements must be made over a frequency range wide enough (10^{-3} to 10^4 Hz) to adequately resolve the impedance spectrum and to allow subsequent deconvolution to obtain the electrochemical parameters.

The requirements for a high-speed, high-precision, impedance measurement system capable of operating at very low frequencies have been presented in detail by Macdonald and McKubre.²² In general, these requirements are in conflict. Maximum acquisition speed is available from noise or transform methods, but these methods are not very precise.²² High precision is best achieved with a frequency-by-frequency measurement technique such as phase-sensitive detection, but the measurements are time consuming. Fortunately, this is not a serious hindrance when such equipment is automated and the experiments are computer-controlled. We used such automated, computer-controlled equipment in the experiments described in the following subsections.

3.2.1 Planar Electrode Experiments

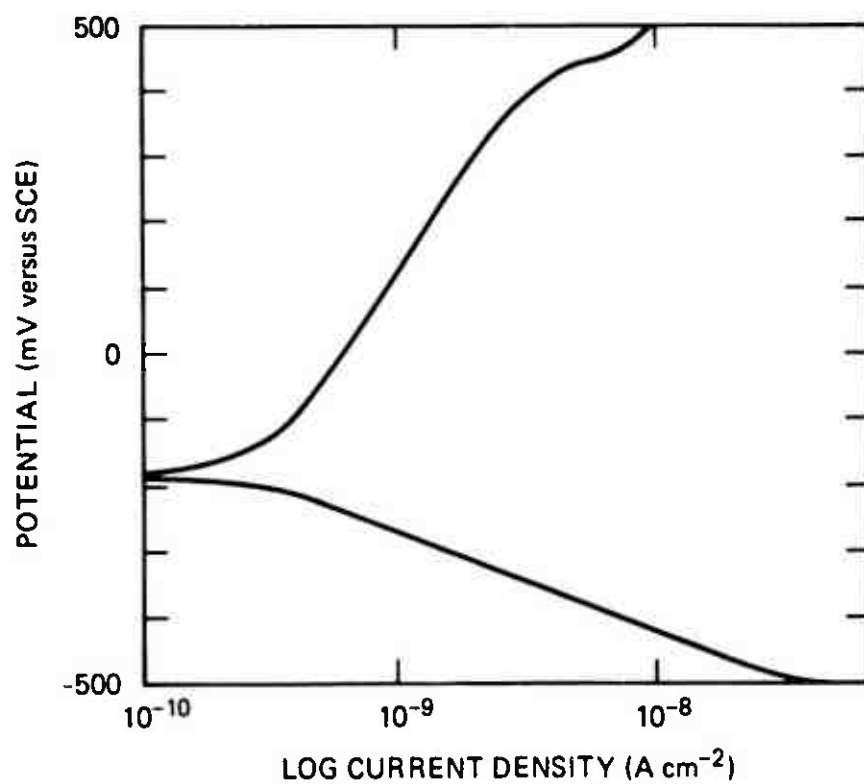
Experiments were performed on planar uncracked electrode of HY80 and Ti-6Al-4V exposed to aerated 3.5 wt% NaCl to obtain the electrochemical parameters needed for developing the DC, crack propagation model and to aid in interpreting the results of electromechanical impedance testing. The experimental setup for these tests is shown in Figure 5. Specimens were mounted with one planar surface exposed to the electrolyte.

Figure 6 presents the Tafel plot obtained for Ti-6Al-4V at very low sweep rates; the sweep was initiated at the cathodic limit of -500 mV versus the saturated calomel electrode (SCE). The apparently well-behaved Tafel law behavior evidenced by the region of linear



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FIGURE 5 EXPERIMENTAL CONFIGURATION FOR AC AND DC TEST ON PLANE PARALLEL ELECTRODES



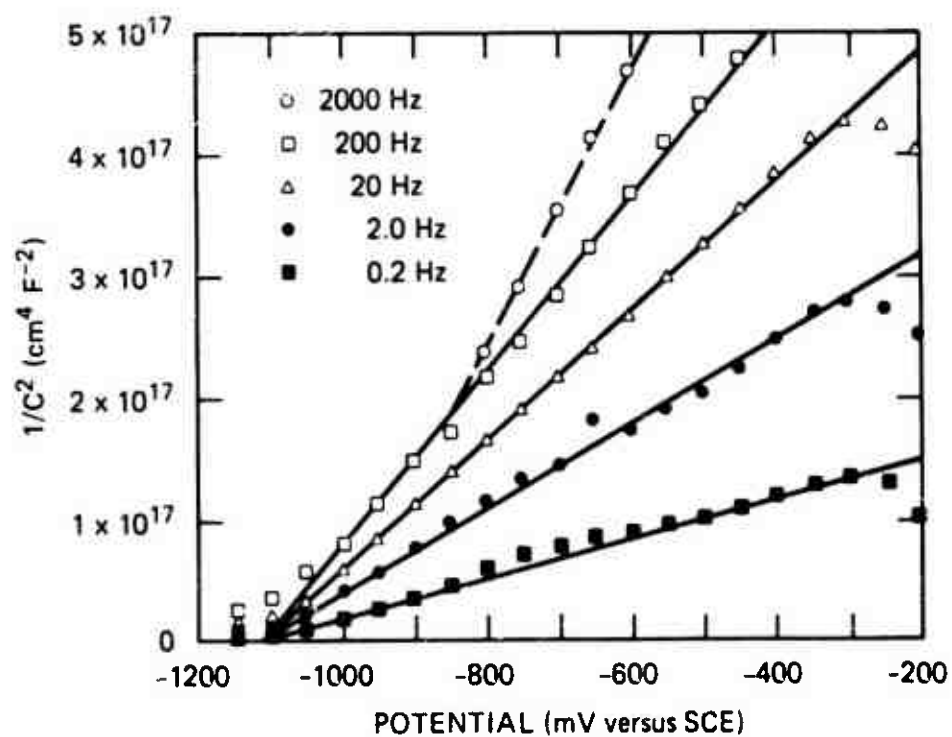
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FIGURE 6 TAFEL PLOT FOR A PLANE PARALLEL ELECTRODE OF Ti-6Al-4V EXPOSED TO 3.5 wt% NaCl AND 25°C, VOLTAGE SWEEP RATE = 0.01 mV s⁻¹

relationship between voltage and the logarithm of current suggests charge-transfer kinetic rate control in both the anodic and cathodic regions.

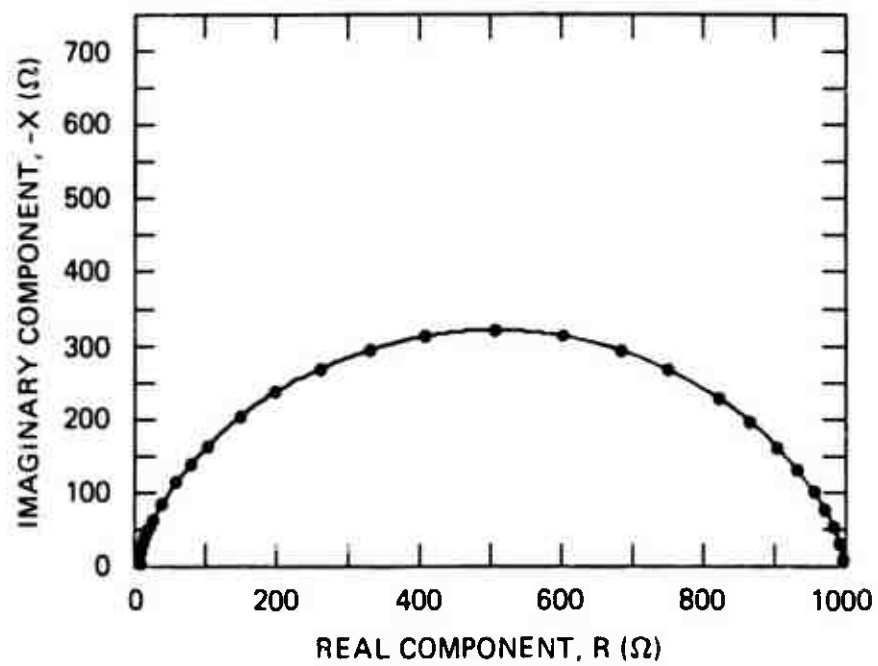
The AC impedance behavior of this electrode, however, strongly indicates that the reaction kinetics of the Ti-6Al-4V electrode surface is dominated by the presence of a semiconducting oxide film such as TiO_2 . Evidence of the dominance of semiconductor-electrochemical effects can be seen in the Mott-Schottky plot presented as Figure 7. The reciprocal of the measured capacitance squared is plotted versus potential at 25-mV steps from -200 to -1200 mV versus SCE. Regions of linearity in such a plot indicate the presence of a space-charge layer^{45,46} (band bending within the oxide film). The type of frequency dispersion shown in Figure 7 (that is, the lines at each frequency do not superimpose) is unusual and may be due to impedance effects within the electrolyte phase (the electrical double layer) or to heterogeneity within the oxide itself. The extrapolated intercept of this family of lines with the axis at $C \rightarrow \infty$ ($1/C^2 \rightarrow 0$) indicates the position of minimum band bending (the "flat-band" potential), which is a characteristic of each semiconducting oxide.^{45,46} This intercept of ~ 1100 mV SCE is within 100 mV of that expected for pure TiO_2 . This 100 mV offset is a result of the defect structure and doping of the Ti-6Al-4V film that forms in the chloride environment.

The HY80 specimens showed a more conventional bulk electrochemical response than the Ti-6Al-4V. The HY80 specimen did not show Mott-Schottky behavior, which is not surprising because the corrosion film that develops is porous and without uniform composition through its thickness; that is, the donor density varies through the film thickness. Figure 8 shows the impedance locus or Nyquist⁴⁷ response of a plane parallel electrode of HY80 exposed to aerated 3.5 wt% NaCl, at the free corrosion potential. The depressed semicircular form is that expected for a metal electrode actively corroding under mixed kinetic/mass transport control. Figure 9 presents data collected at the same electrode, covering a range of potentials more cathodic than the



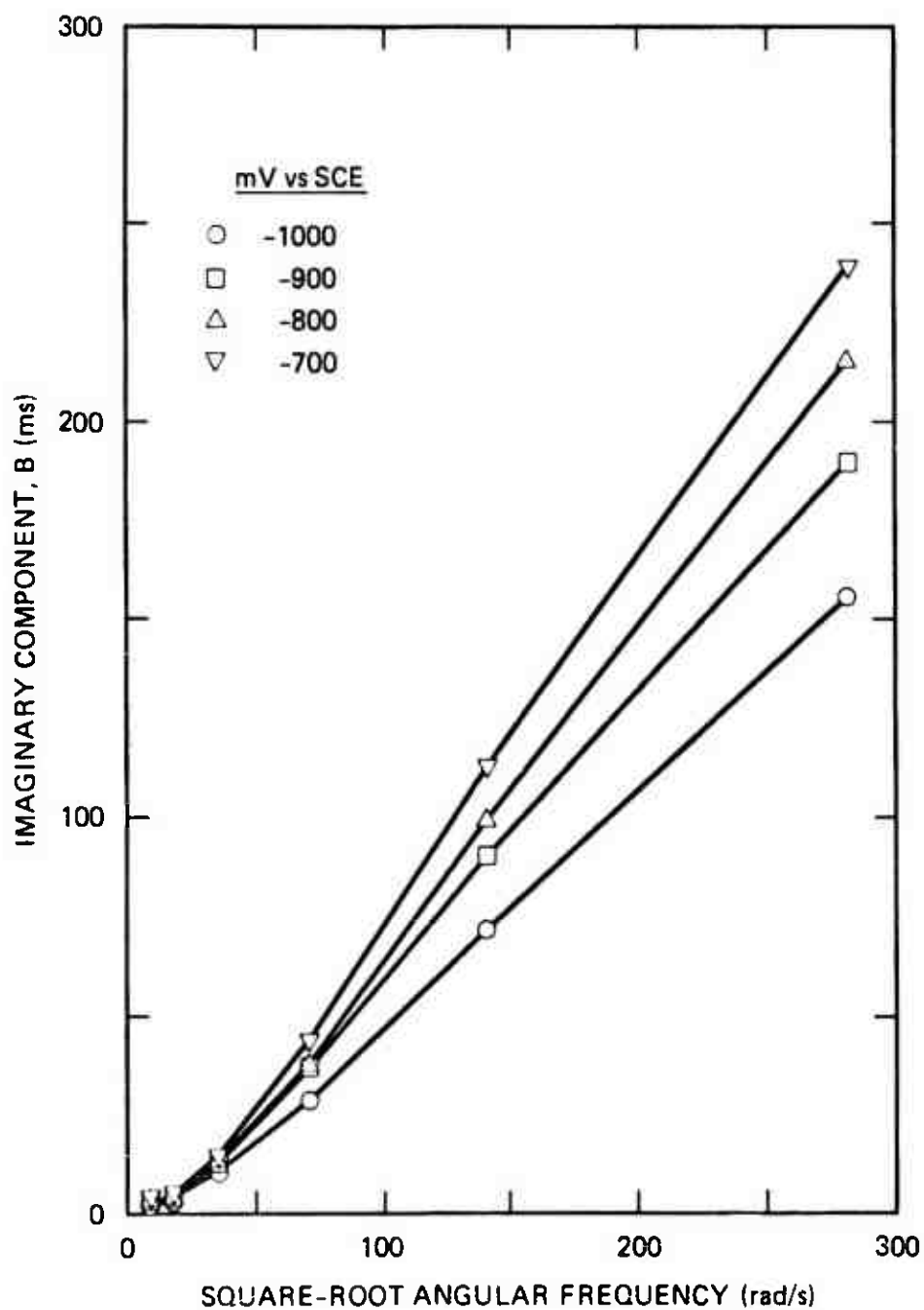
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FIGURE 7 MOTT-SCHOTTKY PLOT FOR A PLANE PARALLEL ELECTRODE OF Ti-6Al-4V EXPOSED TO 3.5 wt% NaCl AT 25°C



JA-4333-14

FIGURE 8 IMPEDANCE LOCUS PLOT FOR A PLANE PARALLEL ELECTRODE OF HY80 EXPOSED TO 3.5 wt% NaCl AT 25°C



JA-4333-15

FIGURE 9 REDUCED AOMITTANCE VERSUS $\omega^{1/2}$ FOR A PLANE PARALLEL ELECTRODE OF HY80 EXPOSED TO 3.5 wt% NaCl AT 25°C, CATHODIC POTENTIAL RANGE

free corrosion potential of HY80 (~ -600 mV versus SCE in aerated 3.5 wt% NaCl). These data are plotted as the reduced admittance, B , versus the square root of the angular frequency, $\omega^{1/2}$,

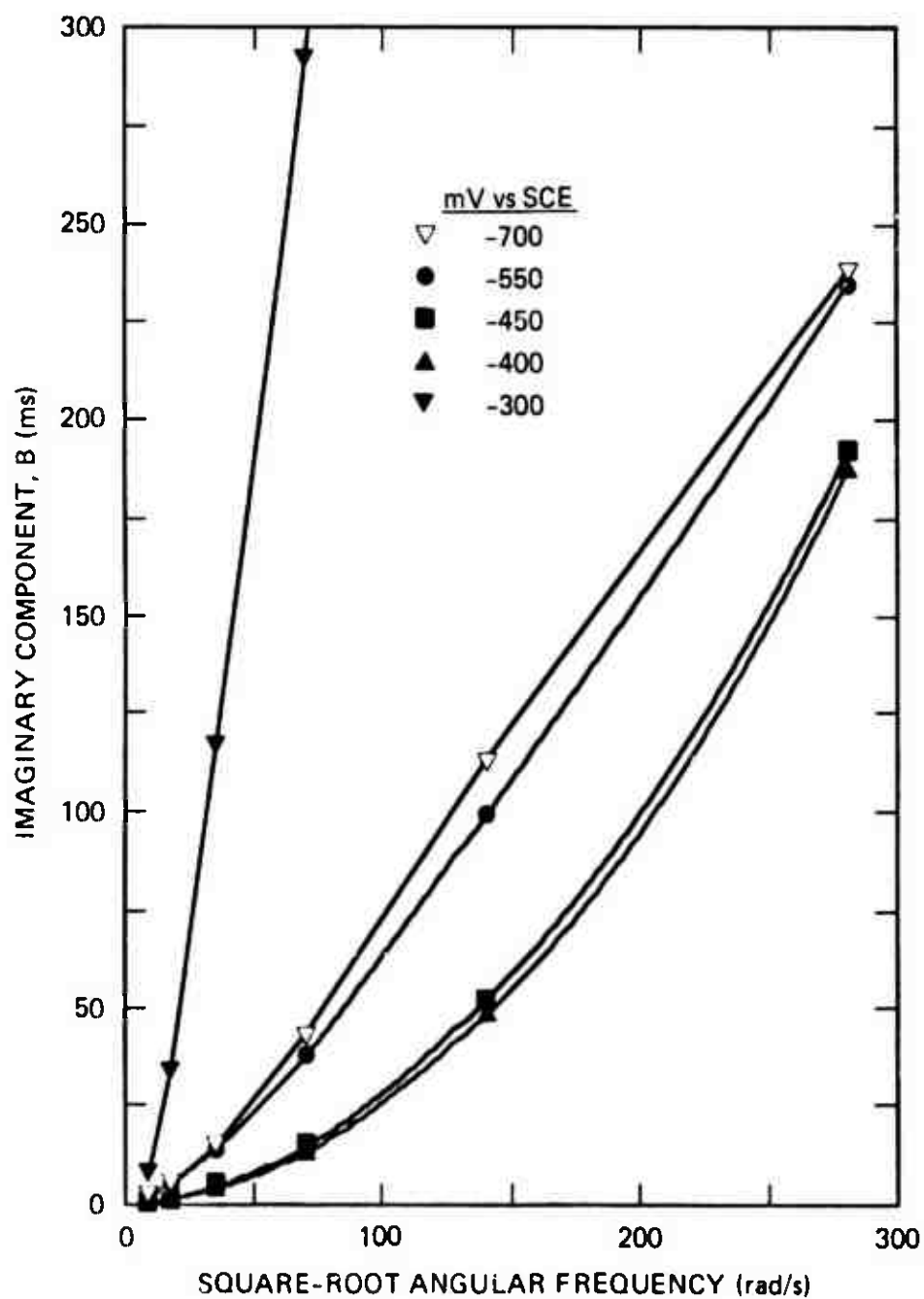
$$B = -X/[(R - R_g)^2 + X^2] \quad (12)$$

where $\omega^{1/2} = (2\pi f)^{1/2}$, X is the imaginary component of the impedance, R is the real component of the impedance, R_g is the uncompensated series electrolyte resistance, and f is the frequency of the impedance measurement in Hz.

The family of straight lines in Figure 9 indicates that, at potentials more negative than (cathodic to) the free corrosion potential, the impedance of an HY80 surface is dominated by diffusional effects within the electrolyte.⁴⁷ At potentials higher than -700 mV, however, deviation from a linear B versus $\omega^{1/2}$ dependence occurs, as shown by the data at -550, -450, and -400 mV, plotted in Figure 10. These data are replotted in Figure 11 versus ω . The straight lines shown are regression fits to the data points; this linearity indicates that the imaginary part of the admittance is dominated by a capacitance of approximately $20 \mu F cm^{-2}$.⁴⁷ The slope of $dB/d\omega$ is equal to the double-layer capacitance and can be seen in this potential range because of the absence of diffusional control effects.

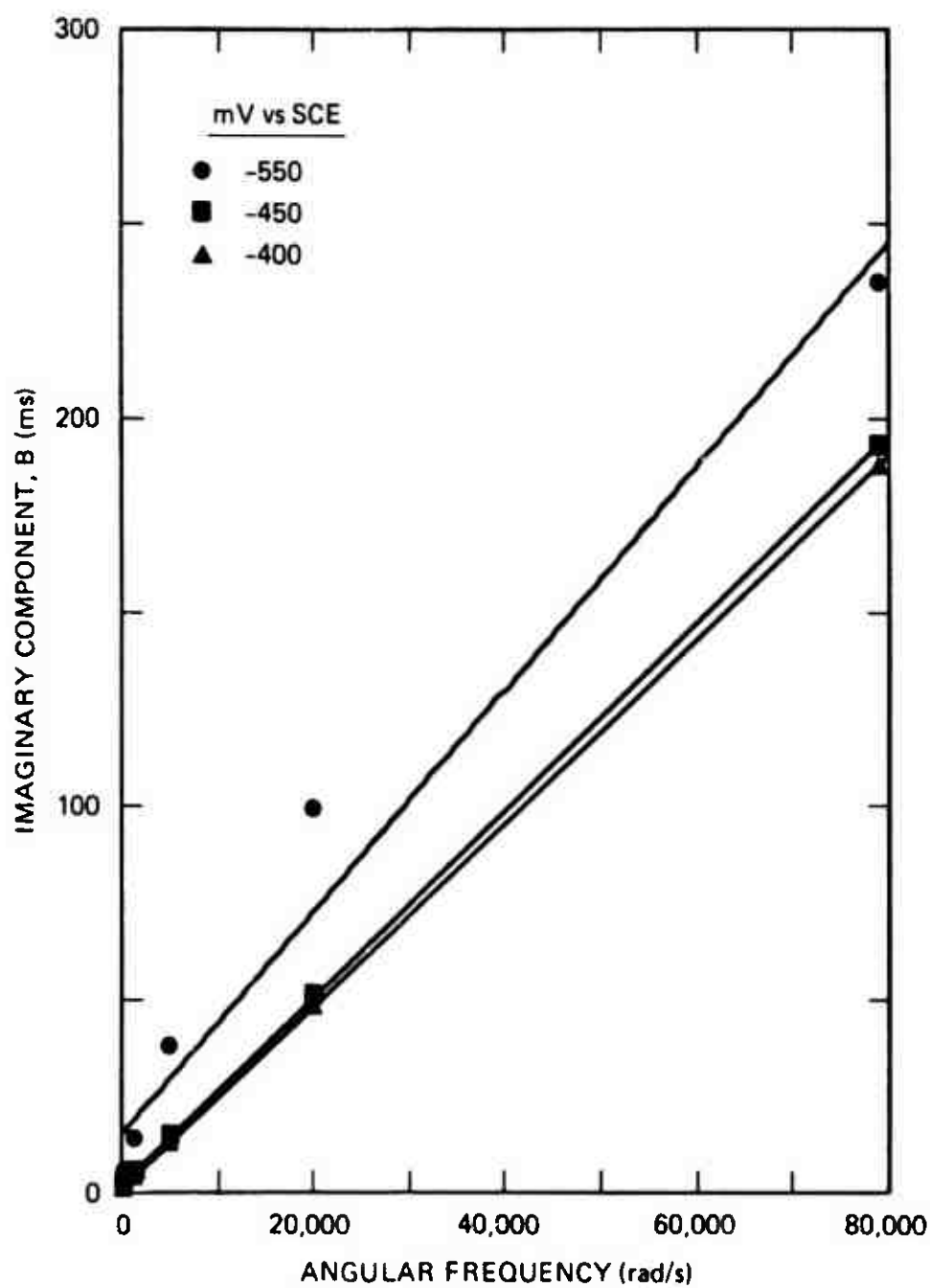
At -300 mV versus SCE, the electrode admittance increases greatly and again displays linearity versus $\omega^{1/2}$, as shown in Figure 10. This is the transpassive region for HY80, and the electrode impedance becomes dominated by the mass transport of corrosion products from the electrode surface.

In summary, the results of planar electrode experiments on bulk Ti-6Al-4V and HY80 specimens showed that, over an extended potential range, the Ti-6Al-4V specimen behaved as if it were covered by a dense semiconducting oxide layer. It exhibited the characteristic linear $1/C^2$



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FIGURE 10 REDUCED ADMITTANCE VERSUS $\omega^{1/2}$ FOR A PLANE PARALLEL ELECTRODE OF HY80 EXPOSED TO 3.5 wt% NaCl AT 25°C, ANODIC POTENTIAL RANGE



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FIGURE 11 REDUCED ADMITTANCE VERSUS ω FOR A PLANE PARALLEL ELECTRODE OF HY80 EXPOSED TO 3.5 wt% NaCl AT 25°C

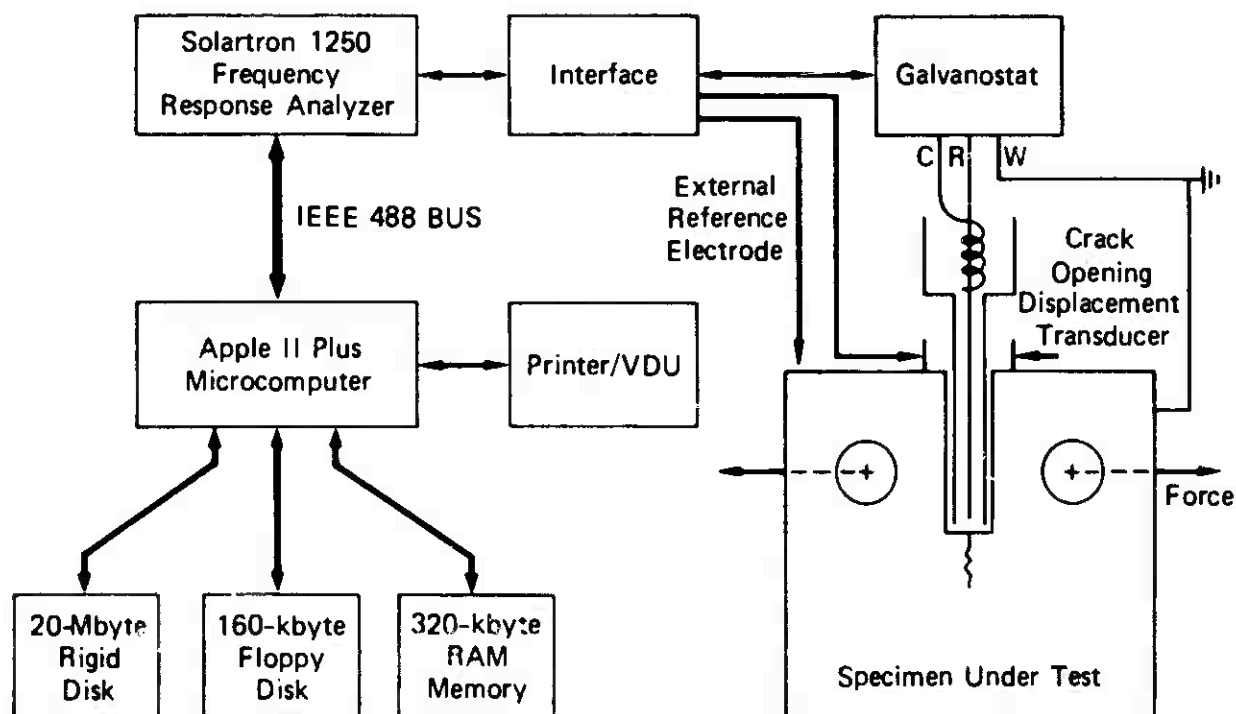
versus voltage behavior. On the other hand, the dependence of the impedance response on voltage for HY80 was more complex although more typical of a corroding electrode. At potentials less than and equal to the free corrosion potential, the electrode impedance response was dominated by diffusion, presumably of reactant (dissolved O_2) to the electrode. At potentials up to 200 mV more positive than the free corrosion potential, in the potential range where a pseudo-passive film is expected to form, the impedance appears to be dominated by an essentially voltage-independent capacitance, almost certainly due to the electrical double layer in the electrolyte. At still more positive potentials, in the transpassive range, the electrode impedance appears to be dominated by the diffusion of reaction products from the electrode surface.

3.2.2 Mechanically loaded Cracked Electrode Experiments

We developed an experimental facility designed to obtain data on crack electrochemistry during CF and SCC of various materials in aqueous solutions at room temperature and pressure. Figure 12 diagrams the experiment arranged for impedance measurement of specimens under mechanical load conditions. Photographs of the setup are shown in Figure 13 (electronics), Figure 14 (test chamber), and Figure 15 (test specimen).

As detailed in Figure 12, impedance measurements were obtained using a Solartron Model 1250 frequency response analyzer (FRA) operated under microcomputer control. The Model 1250 is an automated, digitally demodulated, stepped frequency, impedance meter capable of 0.01% precision for each impedance component in the frequency range 10^{-4} to 6×10^4 Hz. This instrument and the preceding series of frequency response analyzers (Solartron Model 1172 and 1174) have been used extensively in recent years to measure impedances in electrochemical systems.⁴⁸⁻⁵²

The FRA was operated under the control of an Apple II-Plus microcomputer equipped with 64 kbyte of internal random access memory (RAM),



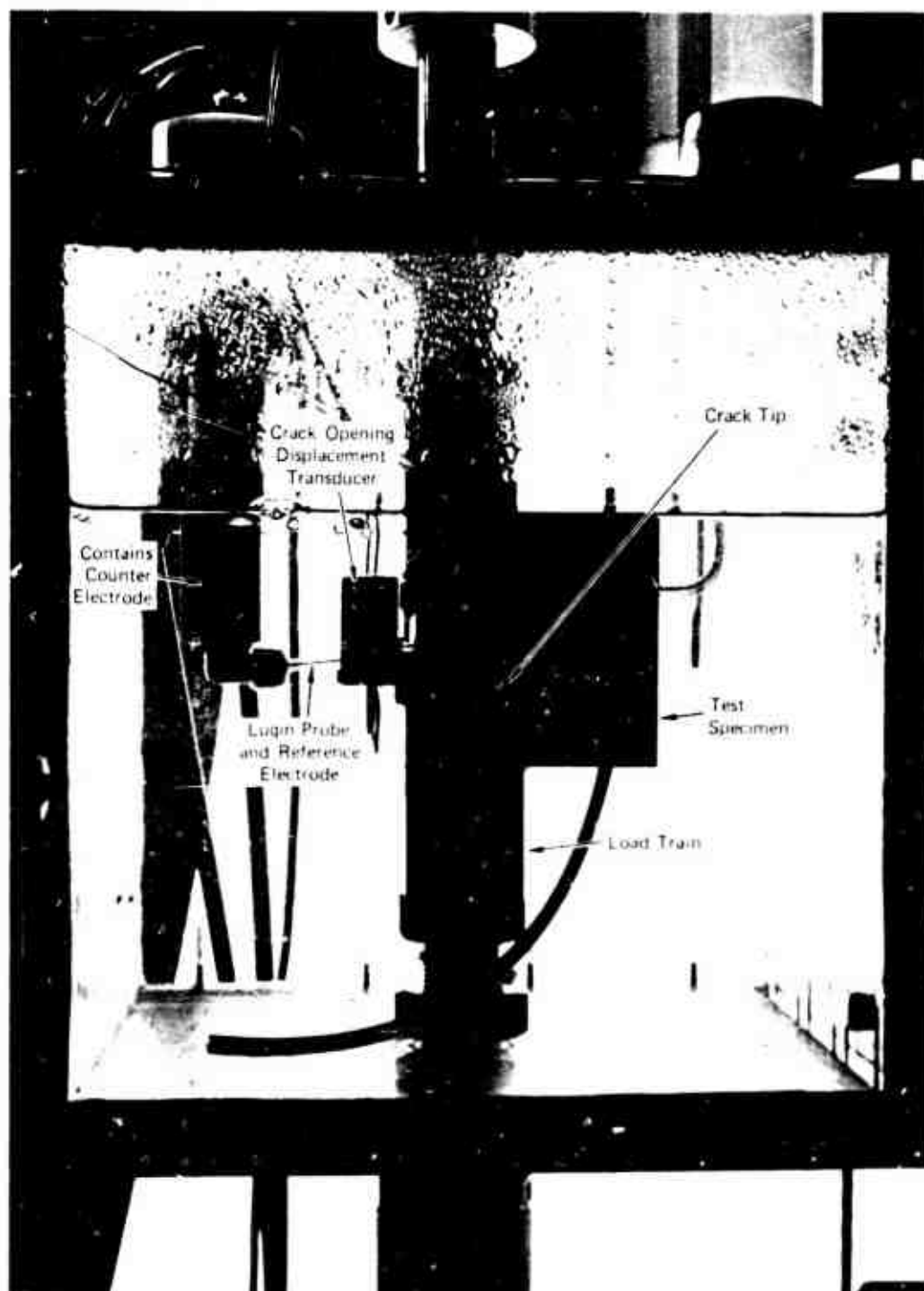
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FIGURE 12 SCHEMATIC OF IMPEDANCE MEASUREMENT SYSTEM FOR STRESS CORROSION CRACK AND CORROSION FATIGUE TESTS



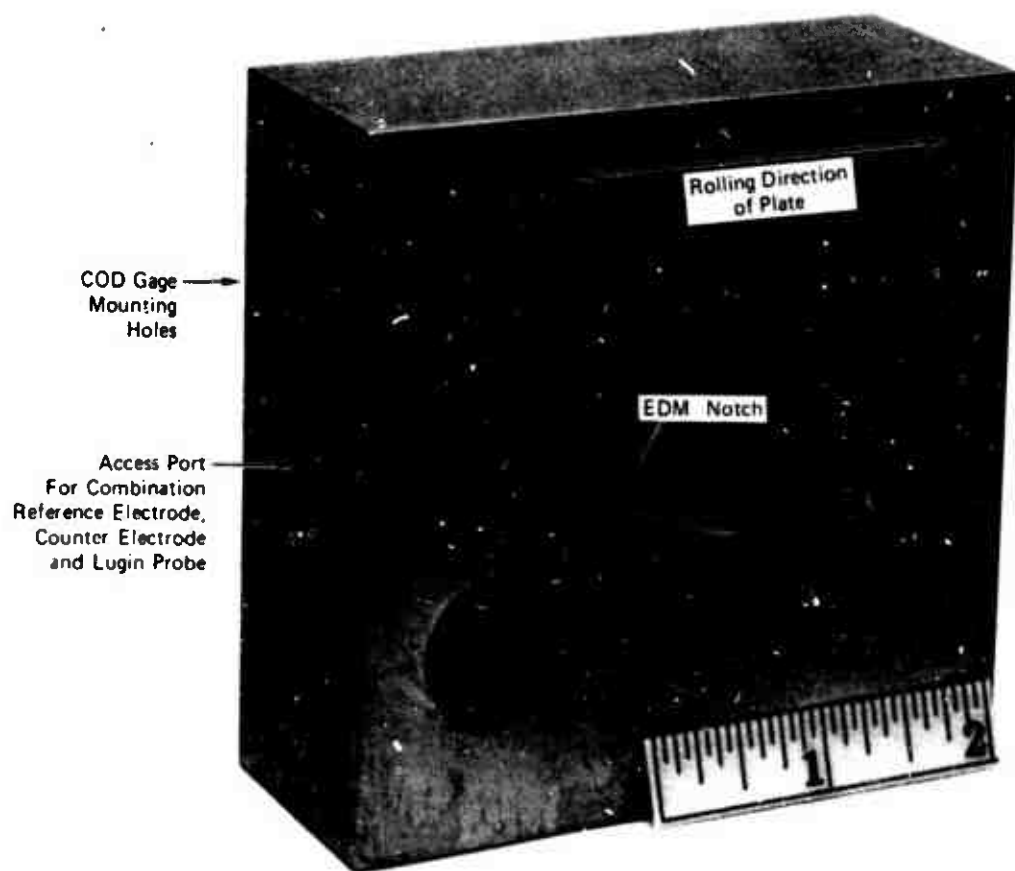
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FIGURE 13 FACILITY FOR MEASURING IMPEDANCE SPECTRA OF STRESS
CORROSION CRACKING OR CORROSION FATIGUE TEST SPECIMENS



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FIGURE 14 DETAIL OF TEST CHAMBER



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FIGURE 15 DETAIL OF TEST SPECIMEN

320 kbyte of external RAM (Axlon "Ramdisk 320"), and a 20-mbyte rigid disk (Corvus Model 20 MB/M). The control program was written at SRI in Basic and 6502 Machine languages and is included as Appendix A.

Some experiments were performed under potentiostatic control, using a Princeton Applied Research Model 173/276 potentiostat; however, most of the experiments were performed under pseudo-galvanostatic control. In the latter mode, a resistance several orders of magnitude larger than the cell impedance is placed in series with the counter electrode, and a large AC voltage is applied. To a good approximation, the current is determined by the AC voltage divided by the series resistance, independent of cell impedance.

For experiments in which the load is cycled, the periods of the mechanical and electrical cycles must be synchronized by integrating the impedance data over one complete cycle of the mechanical load. Thus, the results represent an average over a full cycle of crack-opening displacement. If these cycles are not synchronized, the data may contain a large amount of systematic error and will inevitably show considerable scatter. For example, if the impedance measurements are integrated over a time that is shorter than the mechanical load cycle, multiple determinations (at different electrical perturbation frequencies) may be made during a single mechanical cycle. These determinations will cover the range from maximum to minimum crack opening and will appear as scatter in the data set.

Because it is necessary to integrate over at least one cycle at the electrical perturbation, some error will be introduced at low frequencies when the impedance data are integrated over more than one (but not an integer number of) mechanical cycle. This error is inevitable and results in some scatter in our data at very low frequencies (< 0.01 Hz).

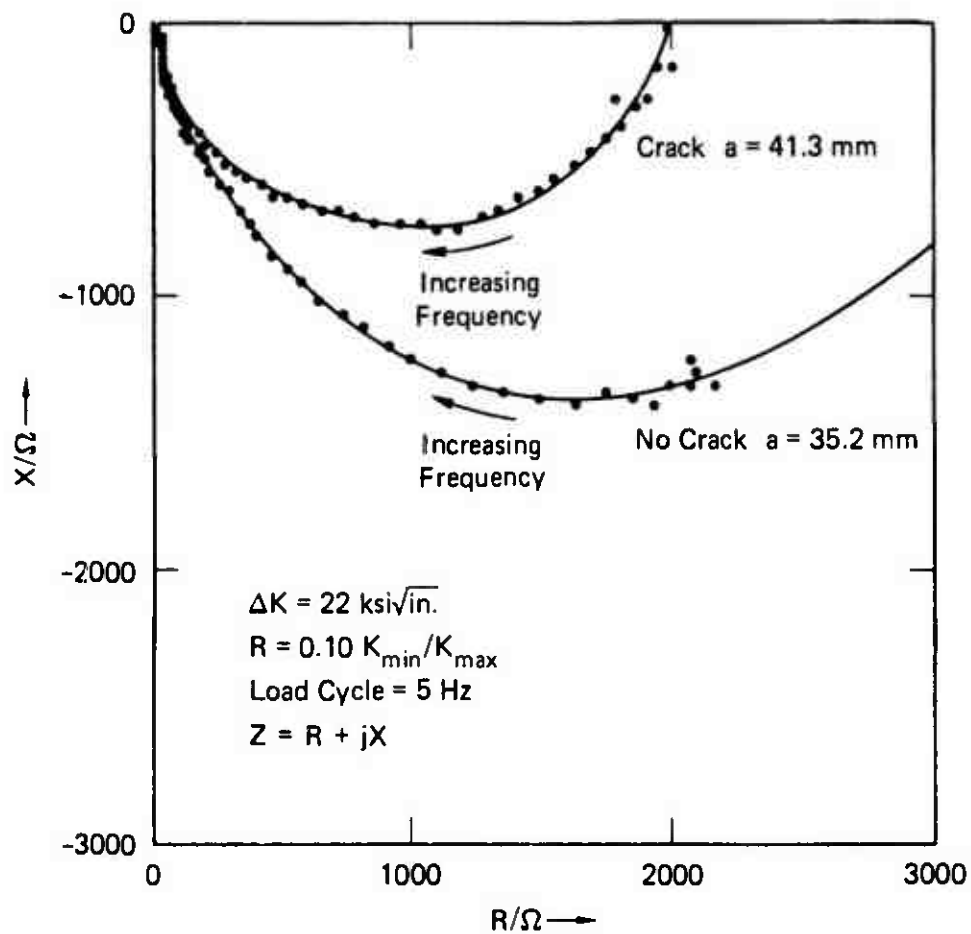
An environmental chamber was constructed that attaches to a servo-hydraulic mechanical testing machine. This chamber and the associated attachments allow us to circulate aerated or deaerated 3.5% NaCl solution (or other electrolyte) at controlled temperatures past our fatigue precracked compact tension specimens. The crack growth can be

measured by optical methods or by the compliance method, by means of a water-immersible LVDT mounted on the specimen. A special composite reference/counter electrode incorporates a silver/silver chloride electrode in a 0.25-inch-diameter Lugin probe, positioned about 0.1 inch from the start of the fatigue precrack. The fatigue precrack is at the bottom of a 2.00-inch-deep notch (1.50 inches wide by 0.010 inch thick), and the tip of the 0.25-inch-diameter Lugin probe is centered at the bottom of this notch to minimize "edge effects" on the electrochemical measurements. The counter electrode is located in a chamber to which the Lugin probe is attached. This arrangement allows us to polarize only the area at the Lugin probe tip and thus measure the response of this area.

The cracked electrochemical AC impedance measurements were obtained on Ti-6Al-4V in aerated 3.5% NaCl solutions. These tests were performed under load control with ΔK varying from 10-30 ksi $\sqrt{\text{in.}}$ with R values of 0 to 0.2. No experiments of this type were performed on HY-80.

Figures 16 and 17 show impedance data for the growth of a crack in Ti-6Al-4V. The data designated as "no crack" in Figure 16 show the impedance response in the range $10^{-3} < f < 10^4$ Hz for a specimen subjected to a 5-Hz cyclic load, but showing no superficial indication of having cracked. In the Nyquist domain this data set appears as a semicircle whose center is located above the real axis. The low-frequency intercept on the real axis is very close to 2000 Ω . The high-frequency region is shown in an amplified form in Figure 16(b). A second semicircular region is observed with a high-frequency intercept on the real axis at 52.8 Ω . The high-frequency intercept corresponds to the series resistance due to the electrolyte path between the tip of the reference electrode and the base of the notch in the specimen.

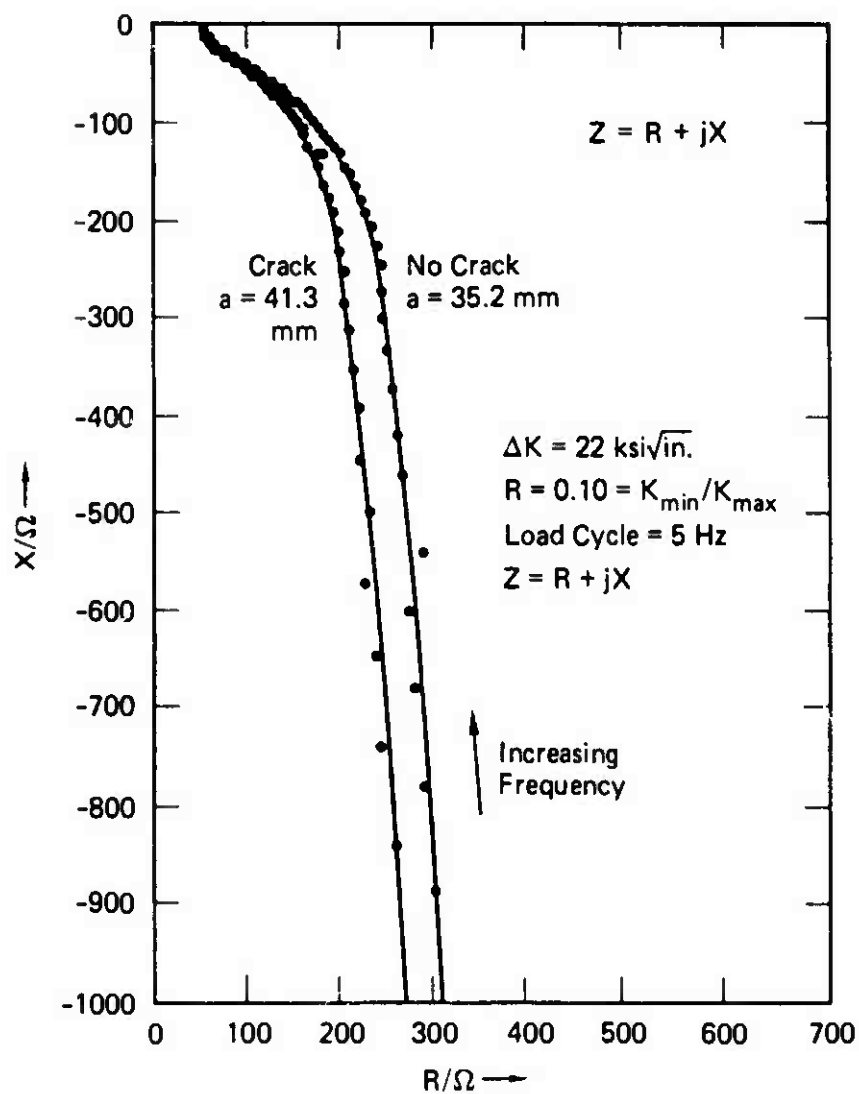
In the Bode plot [Figure 16(c)], these data exhibit a single minimum in the phase occurring at approximately 0.15 Hz. The magnitude information shows two limiting plateaus (corresponding to the intercepts with the real axis in the Nyquist plot) separated by linear regions of slope $-1/2$, -1 , and $-1/4$ with increasing frequency.



(a) Nyquist Plot

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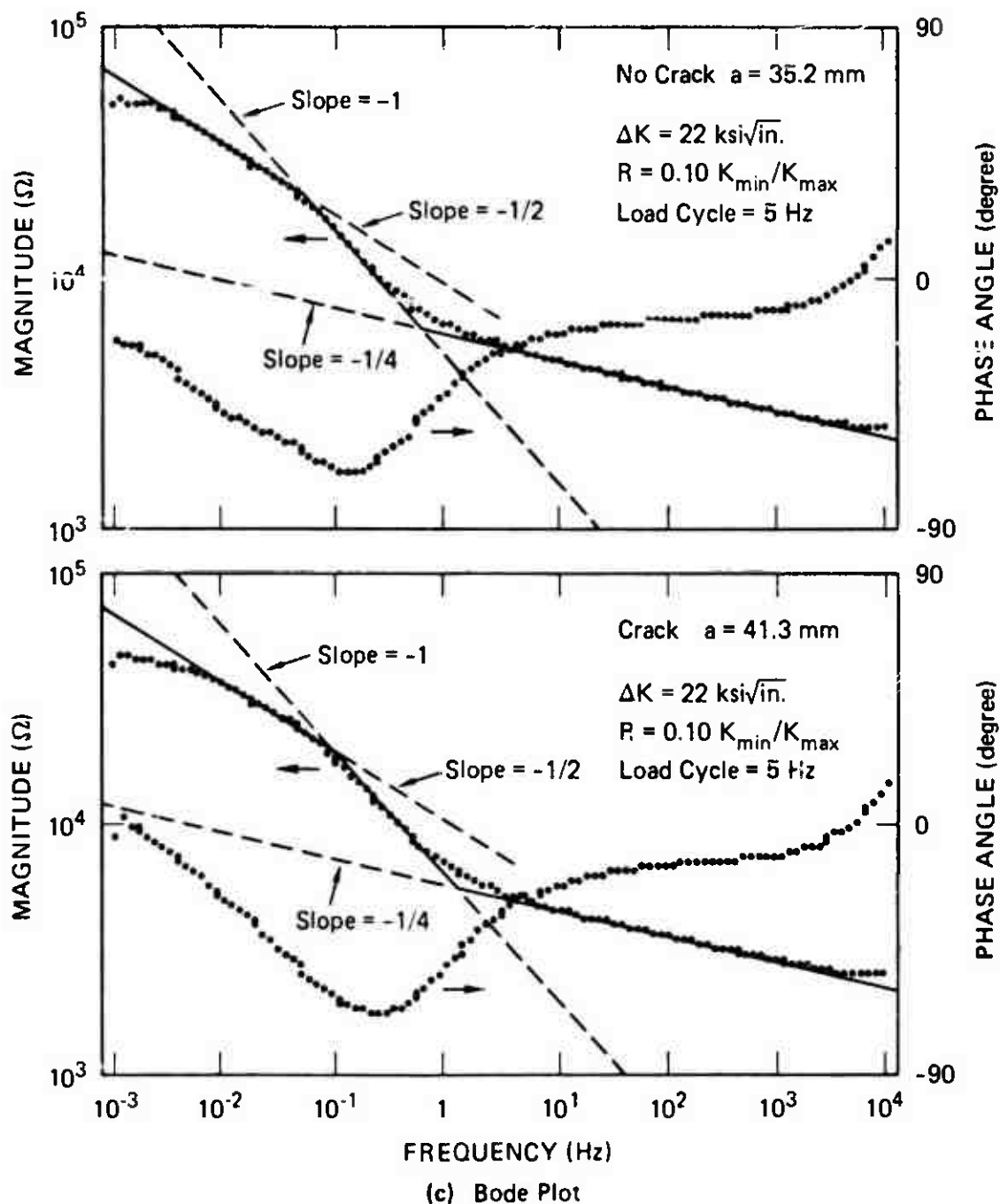
FIGURE 16 IMPEDANCE RESPONSE OF THE Ti-6Al-4V SPECIMEN BEFORE AND AFTER THE APPEARANCE OF A MACROSCOPIC CRACK IN AERATED 3.5% NaCl SOLUTION



(b) Expanded Nyquist Plot

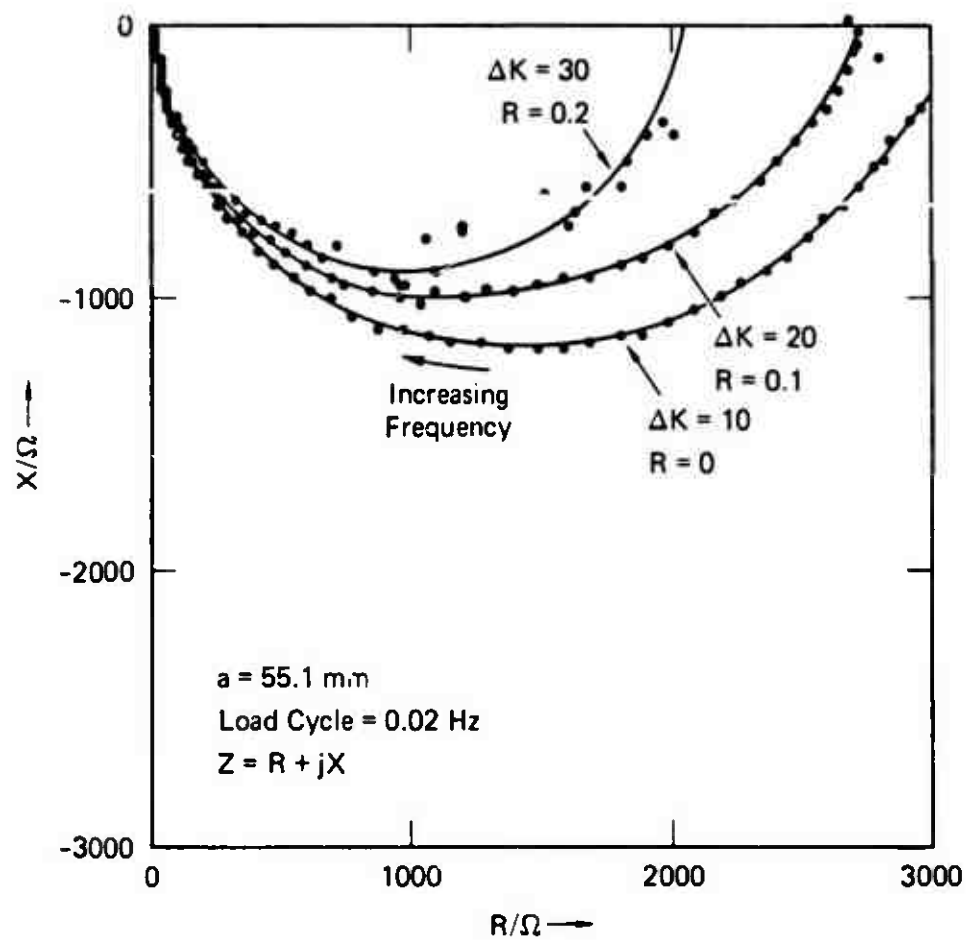
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FIGURE 16 IMPEDANCE RESPONSE OF THE Ti-6Al-4V SPECIMEN BEFORE AND AFTER THE APPEARANCE OF A MACROSCOPIC CRACK IN AERATED 3.5% NaCl SOLUTION (Continued)



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FIGURE 16 IMPEDANCE RESPONSE OF THE Ti-6Al-4V SPECIMEN BEFORE AND AFTER THE APPEARANCE OF A MACROSCOPIC CRACK IN AERATED 3.5% NaCl SOLUTION (Concluded)



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FIGURE 17 THE EFFECT OF LOAD ON THE IMPEDANCE RESPONSE OF A MATURE CRACK IN Ti-6Al-4V IN AERATED 3.5% NaCl SOLUTION

Examining these linear regions in order of decreasing frequency, we see that the region at slope $-1/4$ corresponds to the high-frequency semicircle in the Nyquist plot, shown in Figure 16(b). This region is present for unstressed specimens before cyclic loading and appears to be completely unchanged during the entire growth of the crack. We speculate that this region is associated with diffusion in the plane of the machined notch and perpendicular to the axis of the reference electrode. Although the region of slope $-1/4$ has significant extent in the Bode plot, the impedances involved are very small and have little significance in a linear (e.g., Nyquist) plot of the data. We will not consider this zone further in this report.

At intermediate frequencies, all data sets obtained show a region with a slope of -1 . This region corresponds to a f^{-1} dependence and is the form expected for the equivalent circuit in Figure 2, at intermediate and high frequencies, when diffusion of metal ions from the electrode surface are not rate limiting. A region of slope -1 in a Bode plot corresponds to a semicircle with its center located on the real axis in the Nyquist representation. The beginnings of a semicircle of great magnitude (on the scale shown) can be seen in Figure 16(b); the parameters of this semicircle are determined by the interfacial reaction resistance, R_T , and the double-layer capacitance, C (see Section 2).

Impedance data obtained from untreated specimens before the application of a cyclic load display a f^{-1} dependence (Bode slope = -1) down to limitingly low frequencies. Only under cyclic loading conditions does a region of slope $-1/2$ appear, and this region becomes increasingly significant as a crack grows. Thus, we associate the region of slope $-1/2$ in a Bode plot with the presence of a crack.

Figures 16(a), (b), and (c) each show two curves: one labeled "crack" and the other labeled "no crack" on the basis of visual inspection of the aides of the compact tension specimen. Because both show a region of $f^{-1/2}$ dependence, the curve designated as "no crack" in Figure 16(c) must have at least a vestigial rupture, associated with cyclic loading of the oxide film at the crack tip. The curve labeled

"crack" was obtained when a crack of about 3 mm was observed at the side of the specimen.

A region of apparent $f^{-1/2}$ dependence (slope $-1/2$) for the impedance within the crack is predicted by equations (4) and (5). The transmission line impedance, Z_{t1} , contains terms in $e^{\gamma l}$, which can be expanded as a Taylor series:

$$e^{\gamma l} = 1 + \gamma l + (\gamma l)^2/2! + (\gamma l)^3/3! + \dots \quad (13)$$

For $\gamma l \ll 1$, the third and subsequent terms in this series can be neglected. Substituting equation (13) into equation (4), we obtain an expression of the form

$$Z_{t1} = a + b/\gamma + \text{additional terms} \quad (14)$$

where a and b are undetermined constants and the higher order terms have decreasing significance.

Because γ is a function of $Z_1^{-1/2}$ [see equation (5)], the impedance of Z_1 placed in a transmission line will have a major component that has the square root of the frequency power dependence of the interfacial impedance itself. Thus, for Z_1 containing parallel resistance (R_p) and capacitive (C_p) elements only,

$$1/Z_1 = 1/R_p + j2\pi f C_p \quad (15)$$

and γ will be a function of $f^{1/2}$; from equation (14), Z_{t1} will be a function of $f^{-1/2}$, which is the form observed.

The preceding discussion is important because an $f^{-1/2}$ dependence is often attributed to diffusional processes at a plane-parallel electrode.²²⁻²⁴ By mathematically fitting the measured impedance data to the form predicted by equation (4), we can clearly see that the observed response is due to a capacitive element contained within a

transmission line, rather than to diffusion; the coefficients obtained do not correspond to any known diffusional process.

The capacitance under consideration is simply that of the electrical double layer on the sides of the growing crack. A resistance appears in parallel with this capacitance and is associated with faradaic processes on the crack wall. At present, we are unable to determine whether this faradaic process is anodic (metal dissolution) or cathodic (reprecipitation of metal or hydrogen evolution). To resolve this and other important issues, we constructed a discrete (finite element) transmission line model for the growing crack based on the electromechanical parameters calculated from impedance measurements, as discussed in Section 4.

The two data sets presented in Figure 16 are not greatly different in form; the major changes observed are in the characteristic frequency and the intercept with the real axis at limiting low frequencies. The characteristic frequency (f_0 = frequency of minimum phase) moves from 0.14 to 0.32 Hz between the first and second data sets, and the limiting low-frequency intercept decreases from 3915 to 1995 Ω . This decrease is believed to be an effect of crack opening. For the data set labeled "no crack," the vestigial crack, although short, is very tight and the impedance is large. Under the same load conditions, the crack-opening displacement increases as the crack grows, and the impedance becomes less. In fact, a plot of limiting resistance versus crack length shows a minimum at about 1-cm crack length, the resistance then increasing as the crack lengthens, indicating that effects of crack length become more important than the average crack-opening displacement.

The effects of crack-opening displacement were examined by varying the cyclic load conditions. Specimens were cycled at a mean load, plus and minus the cyclic load perturbation. Figure 17 shows the effects of varying both the mean and the perturbation stress levels for a mature crack (= 2 cm long) cycled at 0.02 Hz. For these data (and for all impedance data presented in this report), each impedance determination represents an average taken over one complete period of the cyclic load

and thus reflects some weighted average of crack opening displacements. Figure 17 clearly shows the effect of crack opening (proportional to load) on the limiting low-frequency resistance. From a superficial examination, it appears that the effects of the load perturbation level are more significant than those of mean load. However, we have not attempted to separate the effects of mean and perturbation stress levels quantitatively.

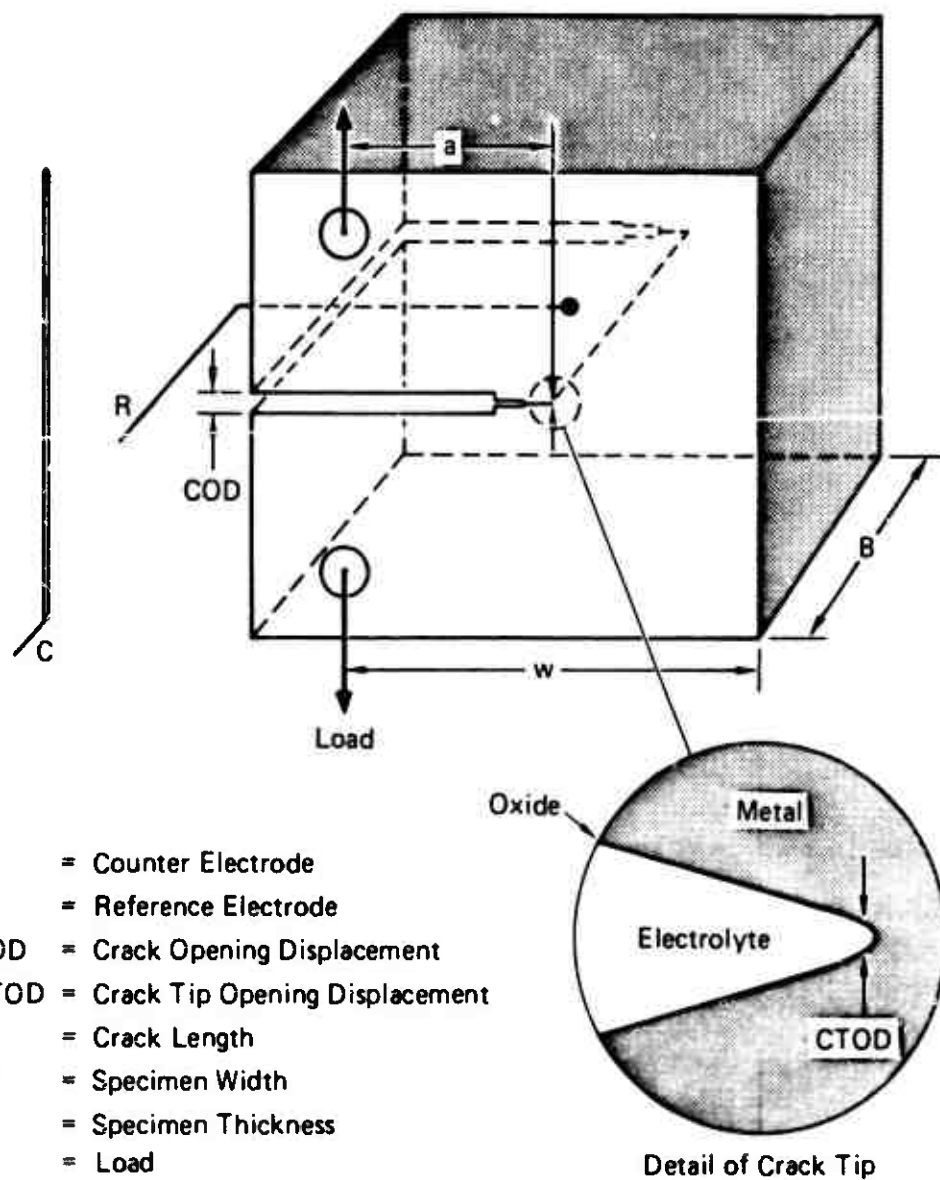
In summary, the results of electrochemical experiments on a cracked Ti-6Al-4V specimen under cyclic load conditions in 3.5% NaCl suggest that the AC impedance appears to be due to faradaic processes at the crack tip and a transmission line impedance associated with the crack walls. We also observed that, at least qualitatively, crack length and crack opening displacement appear to affect the measured impedance.

3.2.3 Electrochemical/Mechanical Impedance Experiments

It is also possible to define an impedance in terms of the electrochemical response of a fractured specimen to a mechanical input that causes crack propagation. One case in which this analysis can be applied usefully is for the electrochemically assisted (stress corrosion) cracking of metals submerged in an electrolyte and subjected to a cyclic mechanical load or stress. With some simplification, crack growth due to cyclical film rupture at the growing crack tip, followed by metal dissolution, can be considered as described below.

Figure 18 shows schematically the case of a crack growing in to a metal, under constant current control and cyclic load conditions. The loading conditions can be controlled to achieve a sinusoidal variation in the specimen load:

$$p = \bar{p} + \tilde{p} \sin(\omega t) \quad (16)$$



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FIGURE 18 CT SPECIMEN GEOMETRY FOR DETERMINING THE ELECTROCHEMICAL MECHANICAL IMPEDANCE FOR THE PROPAGATION OF A CRACK

where \bar{p} is the mean specimen load and \tilde{p} the amplitude of the superimposed sinusoidal perturbation. To a first approximation, the area exposed at the crack tip can be considered to be proportional to the crack tip opening displacement.

$$A = \gamma B (CTOD) \quad (17)$$

$$CTOD = K^2 / 2E\sigma_{ys} \quad (18)$$

$$A = \gamma B K^2 / 2E\sigma_{ys} \quad (19)$$

where

γ = a proportionally constant determined by the mechanical properties of the oxide film and metal at the crack tip

B = specimen thickness

$CTOD$ = crack tip opening displacement

E = Elastic modulus of the specimen

σ_{ys} = yield strength of the specimen

K = stress intensity factor = $p/B f(a/w)^{5/3}$

where

$$f(a/w) = w^{-1/2} (1-a/w)^{-3/2} (2 + a/w) [0.886 + 4.64 (a/w) - 13.32 (a/w)^2 + 14.72 (a/w)^3 - 5.6 (a/w)^4] \quad (20)$$

where

p = applied load

a = crack length

w = specimen width

and (a/w) is determined from⁵⁴

$$(a/w) = 1.0012 - 49.6U + 23.057U^2 - 323.91U^3 + 1789.3U^4 - 3513.2U^5 \quad (21)$$

where

$$U = [(BE[COD]/p)^{1/2} + 1]^{-1}$$

COD = crack opening displacement measured at a distance 0.345 w from the load line towards the front face of the specimen.

The value for COD is determined from

$$COD = p g(a/w) \quad (22)$$

where

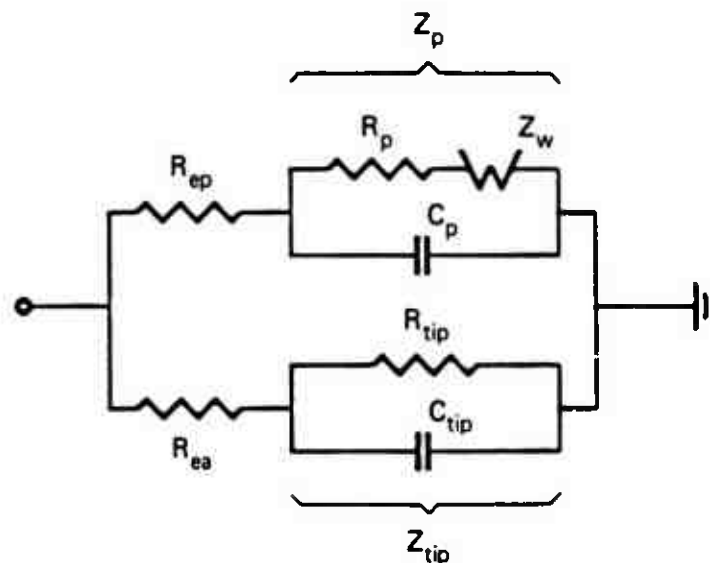
$$g(a/w) = (1/EB)(1 + \frac{0.345}{a/w}) (\frac{1 + a/w}{1 - a/w}) [1.6396 + 11.02(a/w - 6.449(a/w)^2 - 31.14(a/w)^3 + 47.251(a/w)^4 - 18.343(a/w)^5] \quad (23)$$

Combining equations (22) and (16), we obtain

$$COD = [\bar{p} + \tilde{p} \sin(\omega t)] g(a/w) \quad (24)$$

Figure 19 shows the approximate* equivalent circuit for the inside of the crack, with the impedance of the oxide-passivated walls appearing in parallel with the impedance element due to dissolution of exposed metal at the crack tip. The variation in applied load described by equation (16) results in a sinusoidal perturbation of the exposed crack tip area such that

* Because of the potential distribution along the crack, this equivalent circuit should more properly be represented as a nonuniform, finite transmission line for the oxide wall impedance, with the crack tip as a terminating impedance. Such a case is shown in Figure 1.



- R_{ep} = Electrolyte Resistance to Crack Walls
- R_p = Charge Transfer Resistance at Passive Walls
- C_p = Double Layer Capacitance at Passive Oxide
- Z_w = Diffusional Impedance at Passive Walls
- Z_p = Interfacial Impedance at Passive Walls
- R_{ea} = Electrolyte Resistance to Crack Tip
- R_{tip} = Charge Transfer Resistance at Exposed Metal
- C_{tip} = Double Layer Capacitance of Exposed Metal
- Z_{tip} = Interfacial Impedance at Crack Tip

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FIGURE 19 SIMPLIFIED EQUIVALENT CIRCUIT FOR A STRESS CORROSION CRACK

$$C_{tip} = C_{tip}^0 A \approx \frac{C_{tip}^0 \gamma}{2E\sigma_{ys} B} [\bar{p} + \tilde{p} \sin(\omega t)]^2 [f(s/w)]^2 \quad (25)$$

$$R_{tip} = R_{tip}^0 / A \approx \frac{2R_{tip}^0 E\sigma_{ys} B}{\gamma [\bar{p} + \tilde{p} \sin(\omega t)]^2 [f(a/w)]^2} \quad (26)$$

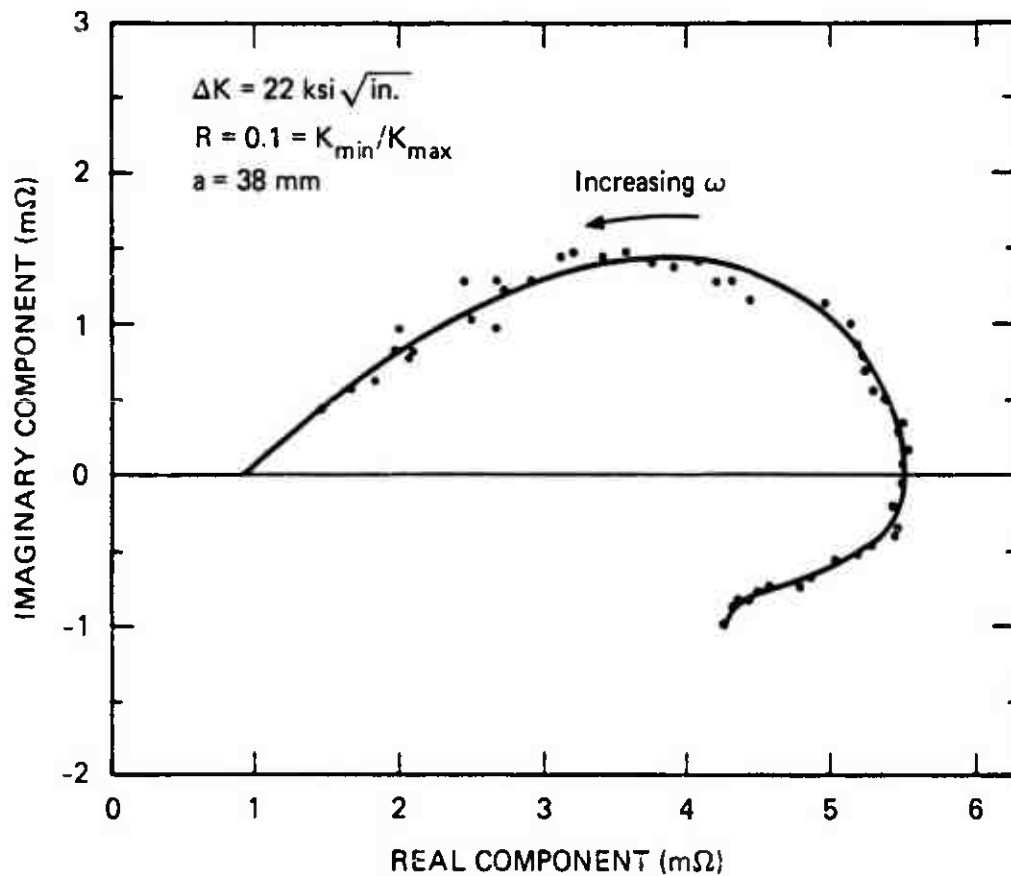
Without going through the algebra, for the equivalent circuit shown in Figure 19, we can obtain an expression for the electrochemical/mechanical impedance (Z_{em}) for this system, defined as the ratio of the AC voltage that appears at the reference electrode, to the COD due to the sinusoidal load variation under DC galvanostatic conditions:

$$Z_{em} = \frac{\tilde{V}_{Ref}}{\tilde{d}} = \bar{V}_{tip} (R_{ep} + Z_p) \left(\frac{1}{R_{tip}^0} + j\omega C_{tip}^0 \right) \frac{\gamma B}{a} \quad (27)$$

Under optimal conditions, Z_{em} , measured over a range of frequencies, can be used to deconvolve the equivalent circuit parameters in a manner analogous to that of electrochemical impedance analysis. The advantage of this method, in the example given, is that measurements can be made under dynamic load conditions and that the perturbation is imposed at the point of principal interest, near the crack tip.

In this experiment we galvanostatically imposed a 0.5 mA current between the counter electrode and the crack tip. The potential was measured with the Ag/AgCl reference electrode located at the crack tip. The mechanical frequency [ω in equation (24)] was varied from 20 mHz to 10 Hz.

Figure 20 presents the real versus imaginary components of the electrochemical/mechanical impedance response measured for an HY80 steel specimen of geometry shown in Figures 15 and 18, immersed in 3.5 wt% NaCl. Because of the form of equation (24), these plots are somewhat more complex than a conventional Nyquist plot. Nevertheless, these data are amenable to standard methods of electrical analysis. We observe that the processes at the growing crack tip dominate at low frequencies,



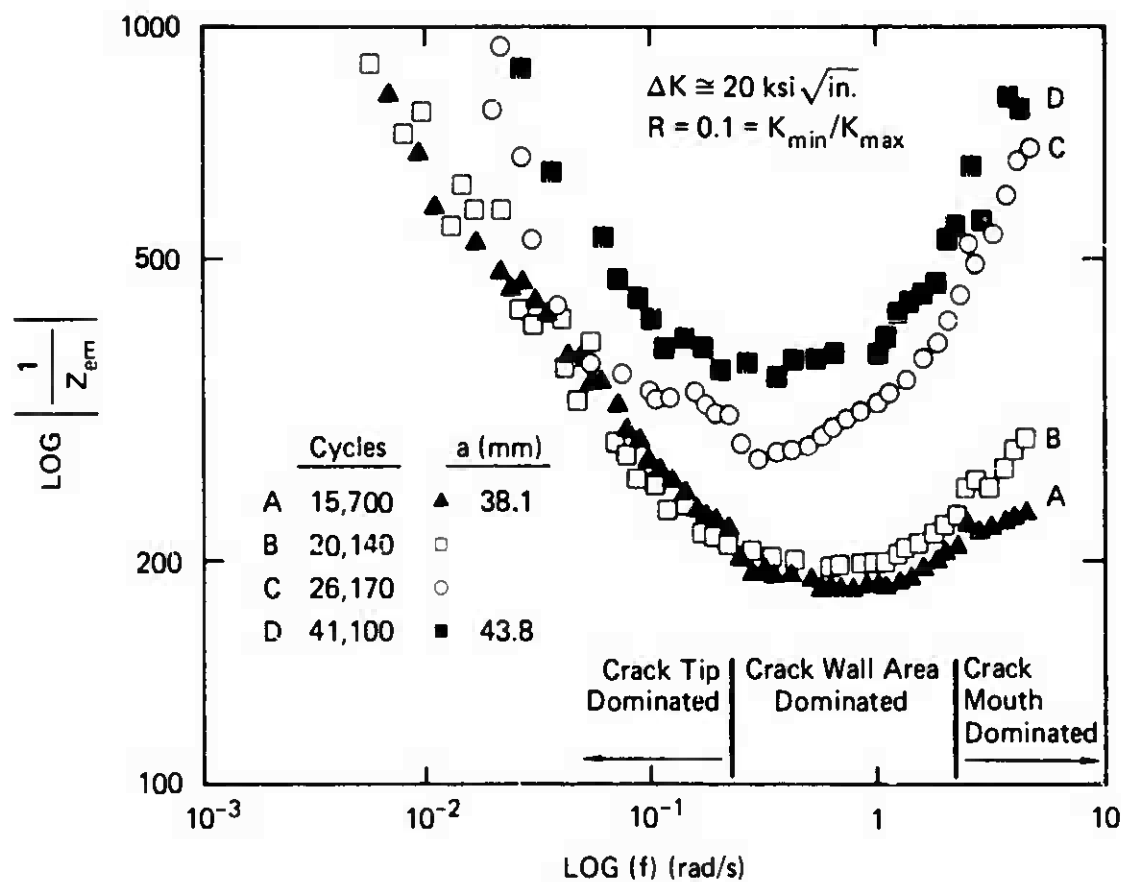
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FIGURE 20 COMPLEX PLANE PLOT OF THE ELECTROCHEMICAL/MECHANICAL IMPEDANCE FOR THE PROPAGATION OF A CRACK THROUGH HY80 STEEL IN 3.5% NaCl SOLUTION AT 25°C UNDER SINUSOIDAL LOADING CONDITIONS

and the properties of greatest interest, R_{tip} and C_{tip} , can be deconvolved at limitingly low frequencies.

Figure 21 shows the logarithm of the electrochemical/mechanical admittance ($Y_{em} = 1/Z_{em}$) plotted versus log frequency, for a typical data set, as a function of the number of mechanical load cycles experienced by the specimen during crack growth. These data show some evolution in the crack tip parameters (the low-frequency, decending portion of the curves), but considerably more changes appear in the crack wall impedance, reflecting the effect of increased crack wall area with increasing crack length. Also, note that the crack grew about 5.7 mm during this portion of the test.

To summarize the experimental results of the electrochemical/mechanical impedance data, we found that this technique was sensitive to crack wall area at frequencies above about 1 Hz and more sensitive to the crack tip at mechanical frequencies below 0.1 Hz. To understand the details of these data and the electrochemical impedance, a more detailed electrochemical/mechanical model needs to be constructed. This model together with the impedance data can then be used to measure the relevant electrochemical and mechanical parameters that occur in a growing SCC or CF crack. As described in the next section, this approach was implemented by modeling the cracking process as a discrete transmission line.



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FIGURE 21 LOG ($|1/Z_{em}|$) VERSUS LOG (FREQUENCY) FOR AN HY80 SPECIMEN EXPOSED TO 3.5 wt% NaCl AT 25°C

Section 4

APPLICATIONS OF THE DISCRETE TRANSMISSION LINE MODEL TO CRACK GROWTH PREDICTION

4.1 OVERVIEW

In developing a quantitative model intended to predict the combined effects of electrochemical corrosion and mechanical stress on crack growth, the first concern is to calculate the chemical, electrochemical, and mechanical parameters at the crack tip, from the prevailing conditions external to the specimen. The problem of computing the mechanical stress and strains in the elastic/plastic zone surrounding the crack tip, from the externally measured load and crack opening displacement, has been addressed by numerous authors^{18,19,55-59} and is not the subject of this report.

Instead, we are concerned with the manner in which the DC potential, the anodic and cathodic currents, the solution pH and conductivity, and the concentrations of metal oxide and metal ions vary with distance and time within the interpenetrating electrolyte volume of a crack growing in a metal, submerged in a bulk volume of electrolyte.

In general, two distinct types of models can be used to obtain the required distributions. A system of first- and second-order nonlinear differential equations can be used to describe the processes of diffusion and interfacial reaction and the static potential distribution. Inevitably, this system of equations cannot be solved analytically, and numerical methods and mathematical approximations must be used to obtain a solution.

An alternative approach has been developed by McKubre for studying porous stripping electrodes^{28,31,42-44} in which the transmission line equivalent circuit, described in Section 2, is considered to consist of a large, but finite number of discrete elements. This type of model

also requires a numerical solution, but offers the advantage of modeling most of the important physical and chemical processes by taken into account the full degree of nonlinearity of electrochemical systems. Of particular significance is that many of the electrochemical parameters necessary to solve the discrete transmission line can be obtained by making low-frequency AC measurements close to the potential of zero current and solving analytically for the continuous transmission line impedance.

The basic features of the discrete transmission line model, applied to a stressed crack, can be seen in Figure 1. Briefly, we consider the resistivities of the solid (metal) and electrolyte phases to be interconnected by the impedance of the metal/electrolyte interface where charge carriers change from electrons to ions. In the discrete model the electrical equivalent circuit is assumed to consist of N discrete zones, each of length a/N , associated with the crack walls, plus an additional zone representing the tip. In general, the interfacial impedance of an arbitrary section of crack wall will depend on the local potential difference between the metal and electrolyte phases, the nature and concentration of dissolved species (principally metal and hydrogen ions and oxygen), and the presence and character of an interfacial oxide film.

The selection of the tip impedance determines the nature of the electrochemically assisted cracking. We are concerned here only with mechanisms of crack growth by anodic dissolution following film rupture. With appropriate modification, the model may nevertheless be used to test mechanisms of crack growth involving de-alloying or hydrogen embrittlement.

Because of the geometry and possible concentration gradients within the crack, the electrolyte resistance at each element of the transmission line is not constant with time or distance. Generally, the metal phase resistance is much less than that of the electrolyte and can be considered to be constant.

The current that flows into the crack (or the potential at the crack surface near the crack tip) was imposed, in our experiments, by a potentiostat with respect to an external counter electrode. Under open circuit conditions this current (or potential) is imposed by the reaction of redox species on the exposed surface of the specimen.

4.2 ASSUMPTIONS

We consider electrochemical and chemical reactions occurring at the crack tip (t) on the crack walls (w), and in the crack electrolyte volume (v). The important reactions are taken to be as follows:

Site(s)	Reaction	Reaction No.
t, w	$M \rightleftharpoons M^{a+} + ae^{-}$	(5.1)
v	$M^{a+} + a/2 H_2O \rightleftharpoons MO_{a/2} + aH^{+}$	(5.2)
w, t	$a/2 H_2 \rightleftharpoons aH^{+} + ae^{-}$	(5.3)
w, t	$M + a/2 H_2O \rightleftharpoons MO_{a/2} + aH^{+} + ae^{-}$	(5.4)

All reactions are considered to be reversible. Reaction (5.1) accounts for metal dissolution, which in conjunction with the chemical reaction (5.2) accounts for oxide formation by dissolution/precipitation. Reaction (5.3) is simple electrolysis, and reaction (5.4) accounts for the direct electrochemical reaction between metal and surface metal oxide film.

The following concepts and assumptions have been applied to simplify the model.

- Only metal dissolution (reaction 5.1) and the crack tip is influenced by the crack opening displacement.
- There is no oxygen within the crack volume and thus reaction (5.3) is the only source of net cathodic current.

- The crack is considered to be a wedge and the area of metal exposed at the crack tip is determined by the tangent of the crack opening angle, θ .

$$\tan(\theta) = \text{COD}/a \quad (28)$$

where COD = crack opening displacement, a = crack length.

- In the electrochemical reactions all symmetry factors (α) are considered to be equal to 1/2.
- The chemical reaction (5.2) rapidly achieves equilibrium.
- At the steady state the activities of H_2O and H_2 are invariant.
- The activity of the metal oxide phase is equal to the monolayer surface coverage, θ , with a maximum of 1.
- At all points the crack is so thin that there exists no limitation due to diffusion perpendicular to the walls.
- The presence of an (NaCl) ensures that the electrolyte phase resistivity does not change significantly with metal or hydrogen ion concentrations.

4.3 EQUATIONS

Anodic dissolution at the crack tip is considered to proceed via the Butler-Volmer equation, with the area exposed, A_t , being proportional to D .

$$A_t = \gamma \text{COD}/a \quad (29)$$

where γ is a constant, and

$$\text{COD} = \bar{D} + |d| \sin(\omega t) \quad (30)$$

These equations (29 and 30) were used as a simplified version of Equations (19) and (24) to reduce the model run time. Equations (19) and (24) will be incorporated in the future. Equation (30) considers the effect of sinusoidal COD loading of the compact tension on the dynamics of crack growth, and a model is being developed to calculate the electromechanical impedance under dynamic conditions that also includes modeling of the γ factor in equation (29). In this section we consider only steady-state conditions, and we define an effective opening displacement, \bar{D} , which is a function of COD, d and the sinusoidal loading rate.

The current associated with metal dissolution at the crack tip, due to an applied overvoltage, under steady-state conditions can be expressed as

$$I_{M/M^{a+}} = i_{M/M}^0 a^+ (\gamma \bar{D}/a) \left\{ \exp \left[\frac{aF}{\alpha RT} (\Delta V_N - V_{M/M^{a+}}^0 - V_{cp}) \right] - \exp \left[\frac{-aF}{\alpha RT} (\Delta V_N - V_{M/M^{a+}}^0 - V_{cp}) \right] \right\} \quad (31)$$

where ΔV_N is the interfacial overvoltage in element N, F is Faraday's constant, T is temperature in Kelvin, V^0 is the equilibrium potential, i^0 is the exchange current density, subscript M/M^{a+} refers to the metal dissolution reaction (5.1), and V_{cp} is the local concentration overvoltage determined by

$$V_{cp}(N) = - (nF/RT) \ln [H^+] \quad (32)$$

The standard state for i^0 and V_{cp} is taken to be 1 molar.

Crack growth is determined at discrete, equal time steps. Within each time interval reactions (5.1), (5.3), and (5.4) are evaluated on the crack walls in each segment of the transmission line, according to the local conditions of concentration and potential.

At the end of each time interval, reaction (5.2) in each segment is considered to be at an equilibrium determined by

$$K = \frac{[MO_{a/2}][H^+]^a}{[M^{a+}][H_2O]^{a/2}} \quad (33)$$

where the activity of water, $[H_2O]$, is considered to be unity, and the activity of the oxide film, $[MO_{a/2}]$, is taken to be equal to the fractional area coverage with a maximum of 1.0 (at one monolayer coverage).

The extent of crack growth in each time interval, t , is calculated from the volume of metal dissolved at the crack tip in a rectangular parallelepiped whose width is the width (B) of the crack opening angle and γ and whose depth is the increased crack length, Δa . Thus,

$$\Delta L = \frac{(I_{M/M}^{tip a+}) (t)}{nF \overline{MW} \overline{\rho} \gamma \theta B} \quad (34)$$

where \overline{MW} and $\overline{\rho}$ are the average molecular weight and density of the dissolved metal, respectively, and the other symbols have been previously defined.

The concentrations within each segment of the transmission line are modified by the combined effects of (1) chemical and electrochemical reactions, (2) the diluting effect as the volume is increased with crack growth (in flow of bulk electrolyte from outside the crack), and (3) diffusion. The effects of diffusion along the crack length are accounted for at the same discrete time intervals as crack growth. A comprehensive model for transverse diffusion is presented in Appendix B. Briefly, we consider the propagation of concentration profiles between nearest neighbors that initially have uniform, but different concentrations. Adjacent zones have different cross-sectional areas and different volumes in the wedge-shaped crack profile. Different approximations are used for long and short times.

The final consideration is of the thickness of the "passivating" metal oxide film. This film has an important role in localizing the

metal dissolution process at the crack tip. We consider the metal oxide to conduct both electrons and ions. The electronic conductive properties are accounted for by the solid-state reaction between metal and metal oxide [reaction (5.4)]. The primary role we envisage for the metal oxide, however, is as a diffusion barrier. At greater than monolayer coverages, we consider that the direct metal dissolution reaction on the crack walls is impeded by the diffusion of metal ions across the metal oxide membrane. The passive current density, i_p , is therefore given by

$$i_p = nFD \frac{C_S - C_N}{y_N} \quad (35)$$

where D is the diffusion coefficient, C_S is the saturation solubility of metal ions in the metal oxide phase,* C_N is the concentration of metal ions at the crack electrolyte/metal oxide interface, and y_N is the oxide film thickness. We simplified the calculation by assuming that metal salt will precipitate when the activity of metal ions reaches unity within the oxide phase. We can therefore define the maximum passive current density (for $C_S = 1$ and $C_N = 0$) as

$$i_p^0 = -nFD/y_N \quad (36)$$

and the passive dissolution current in each segment is given by

$$I_N = i_p^0 (1 - C_N)/y_N \quad (37)$$

*Note that we have not specified whether or not the film is porous. In the event that it is, the values of C_S and D would change, but the principle of a diffusion barrier remains the same.

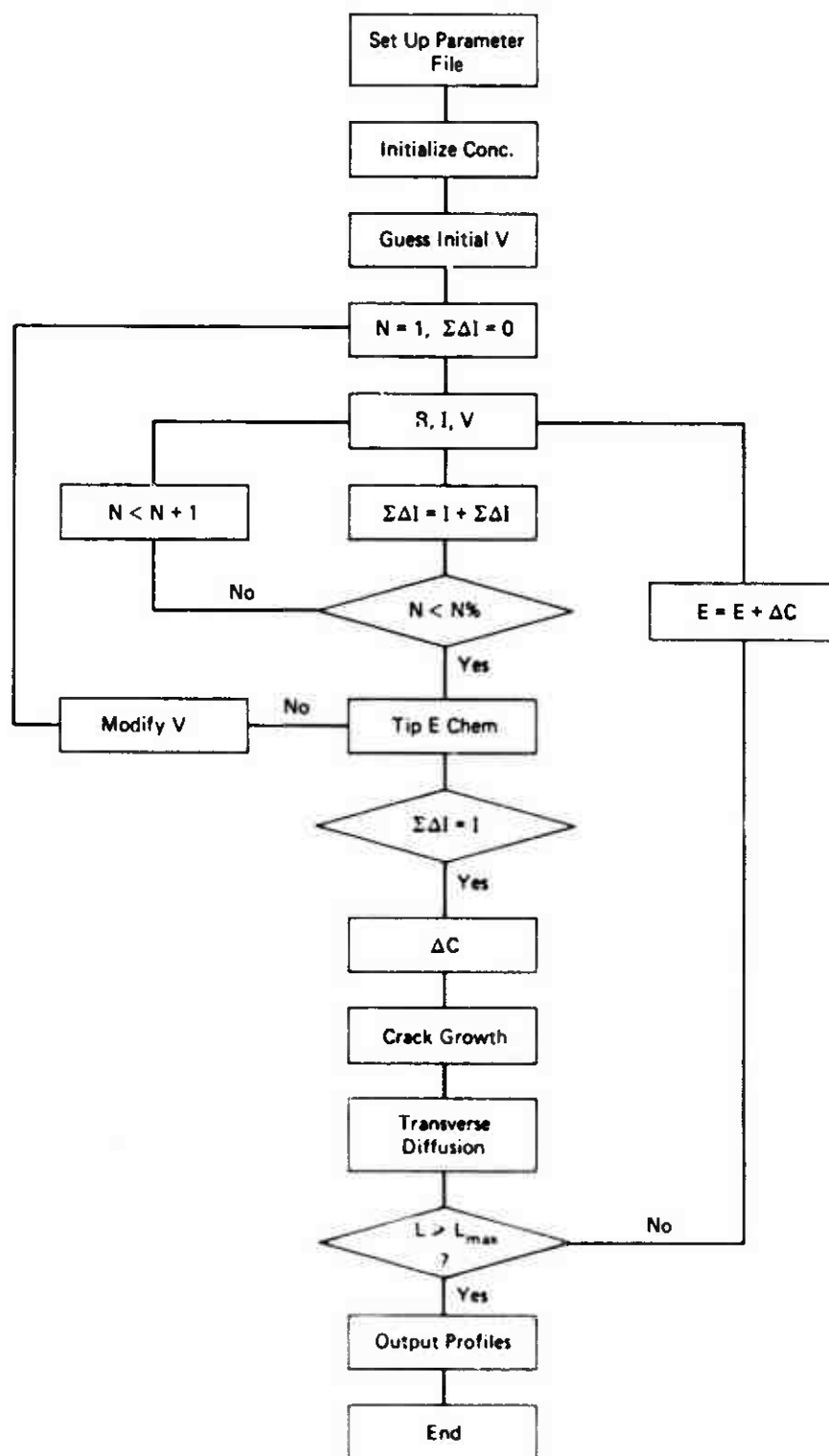
4.4 IMPLEMENTATION

The model described in this section has been implemented as a computer program written in BASIC for the Apple II microcomputer. A listing is provided as Appendix C, and a schematic flow chart is given in Figure 22. Briefly, the program allows for the initialization of the physical and electrochemical parameters used to define crack-growth conditions. These parameters are stored in the array ZM(26) and have the meanings shown in Table 3.

The transmission line is considered to consist of N segments, where $N < 200$. Data are saved in the array ZN(9,200) for the metal and electrolyte phase voltages and resistances, the interfacial currents for the electrochemical reactions $M \rightleftharpoons M^{a+}$, $H_2 \rightleftharpoons 2 H^+$, and $M \rightleftharpoons MO_{a/2}$, and for the hydrogen and metal ion concentrations in the crack electrolyte, and the oxide monolayer thickness, in each segment. The allocation of these variables is shown in Table 4.

Before the application of stress or potential, a vestigial crack is considered to exist, filled with electrolyte at the bulk pH, with the walls covered in a monolayer of oxide, and the metal ion concentration in chemical equilibrium. The data array is initialized with these concentrations at the outset of computation. The program then guesses an initial value of the applied potential that will result in the net DC current. The resistances, potentials, and currents are then calculated in each mesh of the transmission line, progressively, from the reference electrode to the crack tip. If the sum of the calculated interfacial currents is not equal to the net DC current that enters the crack (within the specified tolerance), then the initial value of applied potential is adjusted and the computation loop reiterated.

Following a successful solution of the current and potential profiles, the changes in concentration resulting from chemical and electrochemical reactions, the crack advancement, and effects of diffusion are evaluated, and the resultant profiles are output to printer and/or disk.



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FIGURE 22 CRACK GROWTH FLOW CHART

Table 3

PARAMETER ARRAY

Array Element ZM(x)	Parameter	Units
x = 1	DC current	A
2	Specimen width	cm
3	Specimen height	cm
4	Specimen length	cm
5	Crack opening angle	radians
6	Bulk electrolyte pH	---
7	Electrolyte resistivity	Ω cm
8	Metal resistivity	Ω cm
9	Mechanical stress factor, γ	cm
10	Number of electrons/ion	--
11	Computation interval	s
12	Number of elements	--
13	Computation tolerance	mV
14	Maximum number of iterations	--
15	Exchange current density, M/M^{a+}	$A\ cm^{-2}$
16	Equilibrium potential, M/M^{a+}	V
17	Exchange current density, $M/MO_{a/2}$	$A\ cm^{-2}$
18	Equilibrium potential, $M/MO_{a/2}$	V
19	Exchange current density, H/H^+	$A\ cm^{-2}$
20	Equilibrium potential, H/H^+	V
21	Chemical equilibrium constant	--
22	Charge per monolayer of oxide	$C\ cm^{-2}$
23	Charge per volume of oxide	$C\ cm^{-3}$
24	Metal ion diffusion coefficient	$cm^2\ s^{-1}$
25	Passive current density	$A\ cm^{-2}$
26	Mechanical loading frequency	Hz

Table 4

DATA ARRAY

Array Element ZM(x)	Parameter	Units
M = 0	Solid phase voltage, $V_{s,N}$	V
1	Electrolyte phase voltage, $V_{e,N}$	V
2	Solid phase resistance, $R_{s,N}$	$\Omega \text{ cm}^{-1}$
3	Electrolyte phase resistance, $R_{e,N}$	$\Omega \text{ cm}^{-1}$
4	Interfacial current, M/M^{a+}	A
5	Interfacial current, H/H^+	A
6	Interfacial current, $M/MO_{a/2}$	A
7	Hydrogen ion concentration, $[H^+]$	mole dm^{-3}
8	Metal ion concentration, $[M^{a+}]$	mole dm^{-3}
9	Metal oxide thickness, X_N	monolayers

This procedure is repeated at the interval specified until the crack achieves its desired length.

4.5 RESULTS

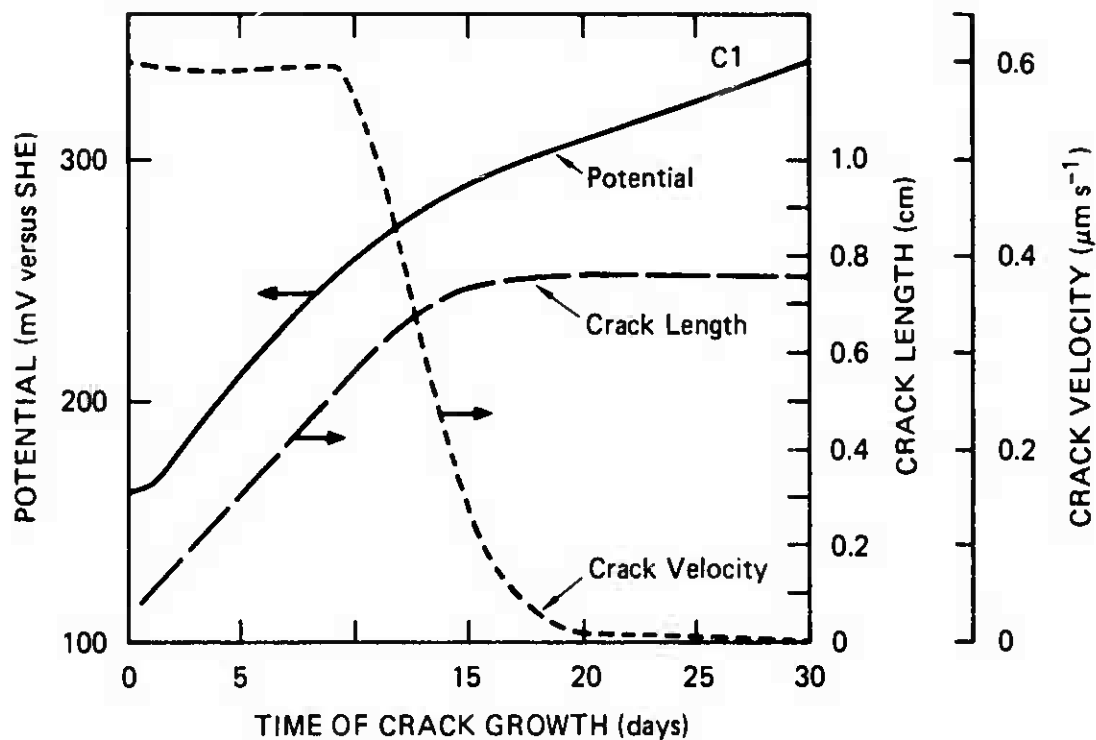
A series of computations was performed in a preliminary attempt to verify the model predictions, using estimated physical and electrochemical parameters for HY80 steel in 3.5 wt% NaCl. The parameters used are summarized in Table 5. Figures 23 through 26 show the results of computations that conform closely to the initial crack velocities measured experimentally for the compact tension specimens. We measured the crack velocity to be about $2.3 \times 10^{-7} \text{ m s}^{-1}$ and the model predicts an initial velocity of $6 \times 10^{-7} \text{ m s}^{-1}$ (see Figure 21).

For the first computation (parameters C1 in Table 5), a crack was grown from $a = a^0 + 0.05 \text{ cm}$ to $a = a^0 + 0.76 \text{ cm}$ where $a^0 = 3.6 \text{ cm}$ at a constant crack current of +1 mA. This computation used a COD cycling at 1 Hz, which corresponds to a ΔK of $\sim 20 \text{ ksi } \sqrt{\text{in.}}$; this ΔK value did not change appreciably as the crack grew over this small distance. Figure 23 shows the time dependence of the crack velocity, crack length, and potential at the orifice. The crack propagates initially at an essentially constant rate of $0.6 \mu\text{m s}^{-1}$, but after about 10 days, the crack decelerates rapidly; at 30 days the crack velocity is essentially zero. Under constant current conditions the potential at the orifice increases monotonically with time, as the active zone at the crack tip becomes further removed. Because the crack velocity decreases rapidly after the crack has grown approximately 0.5 cm, one is inclined to attribute this decrease to a decreasing ΔK or correspondingly a significantly lower crack tip ruptured area that decreases as the crack length increases. This is not the case because the stress intensity and area exposed at the tip have changed very gradually and only by a small amount over the total range of crack lengths calculated. It nevertheless appears that the model is predicting a ΔK threshold value near $20 \text{ ksi } \sqrt{\text{in.}}$. This decrease in crack growth rate seems to be due to precipitation of oxide along the crack length.

Table 5

PHYSICAL AND ELECTROCHEMICAL PARAMETERS
USED FOR MODEL COMPUTATIONS

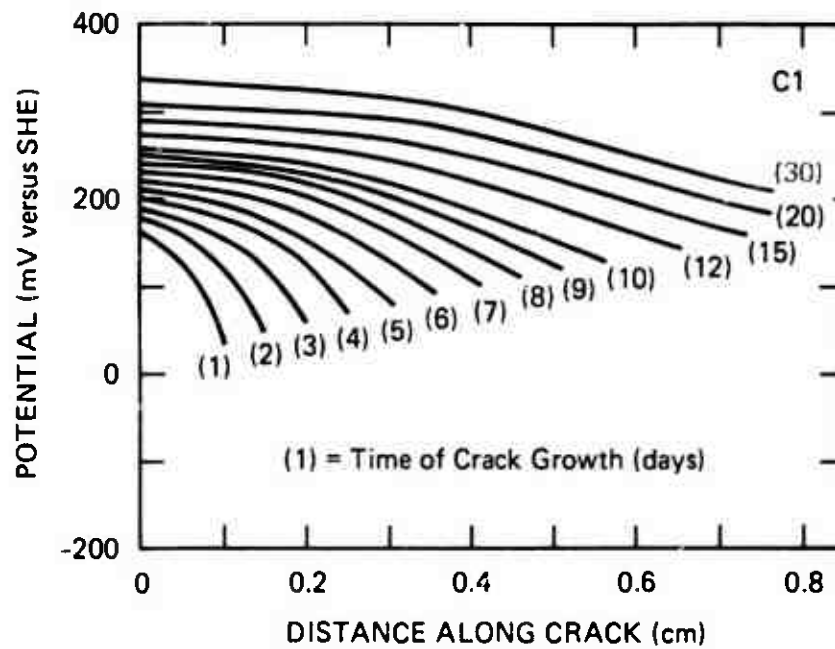
Parameter Number	Description	Computation Number		Units
		C1	C2	
1	Applied DC current	10^{-3}	$0 \rightarrow 10^{-2}$	A
5	Crack opening angle	0.003	0.003	rad
6	Bulk electrolyte pH	6.0	6.0	—
7	Electrolyte resistivity	20.0	20.0	Ω cm
8	Metal resistivity	10^{-5}	10^{-5}	Ω cm
9	Mechanical stress factor	7×10^{-4}	7×10^{-4}	cm
15	Exchange current, M/M^{a+}	10^{-2}	10^{-2}	$A\ cm^{-2}$
16	Equilibrium potential, M/M^{a+}	-200	-200	mV
17	Exchange current, $M/MO_{a/2}$	10^{-4}	10^{-4}	$A\ cm^{-2}$
18	Equilibrium potential, $M/MO_{a/2}$	-100	-100	mV
19	Exchange current, M/M^+	10^{-4}	10^{-4}	$A\ cm^{-2}$
20	Equilibrium potential, M/M^+	0	0	mV
21	Chemical equilibrium constant	10^{-6}	$10^{-6}, 10^{-3}$	—
24	Diffusion coefficient, M^{a+}	2×10^{-5}	2×10^{-5}	$cm^2\ s^{-1}$
25	Passive current density	10^{-6}	10^{-6}	$A\ cm^{-2}$
26	Mechanical loading frequency	1	1	Hz



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FIGURE 23 DC TRANSMISSION LINE MODEL CALCULATION OF THE POTENTIAL, CRACK LENGTH, AND CRACK VELOCITY AS A FUNCTION OF TIME FOR A CRACK GROWN AT CONSTANT CURRENT IN HY80 STEEL

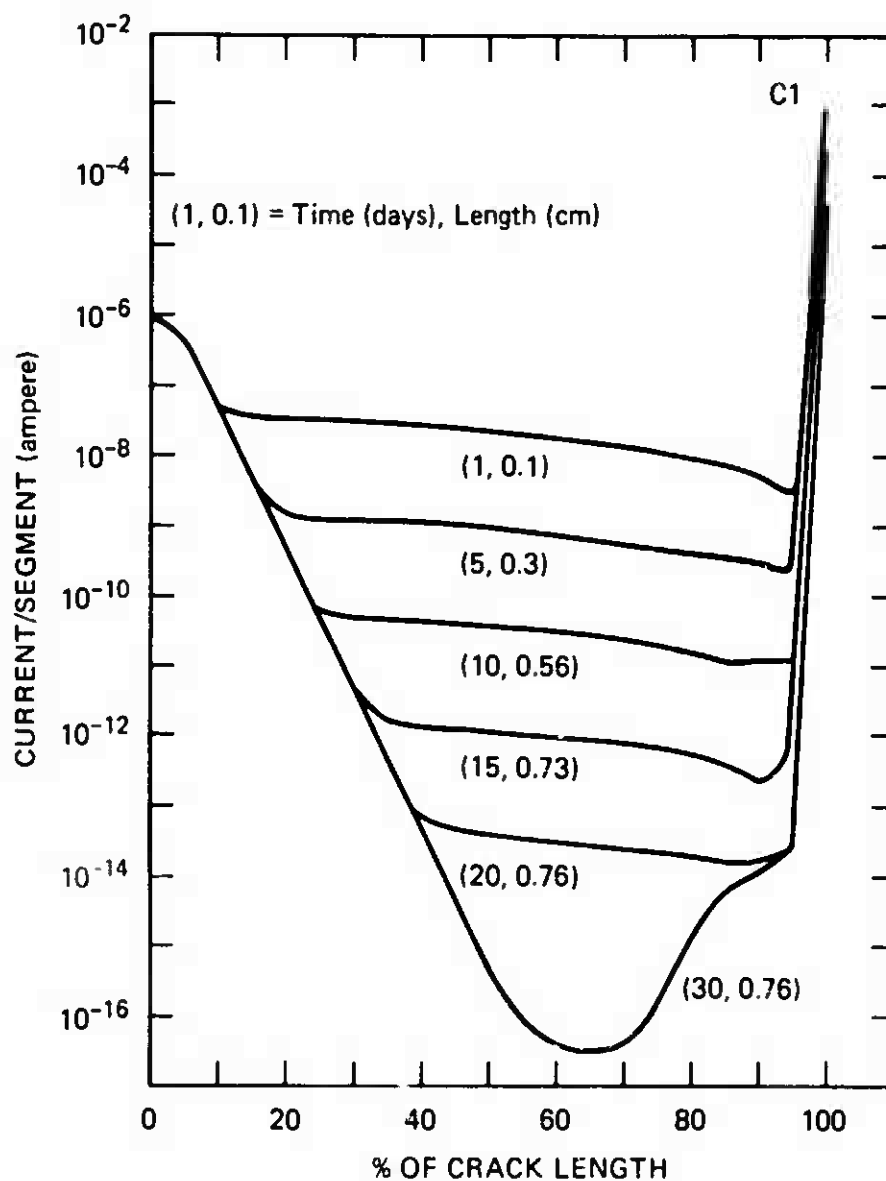
Initial conditions C1 in Table 5.



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FIGURE 24 DC TRANSMISSION LINE MODEL CALCULATION OF THE POTENTIAL VERSUS DISTANCE INTO THE CRACK AS A FUNCTION OF TIME FOR HY80 IN 3.5% NaCl

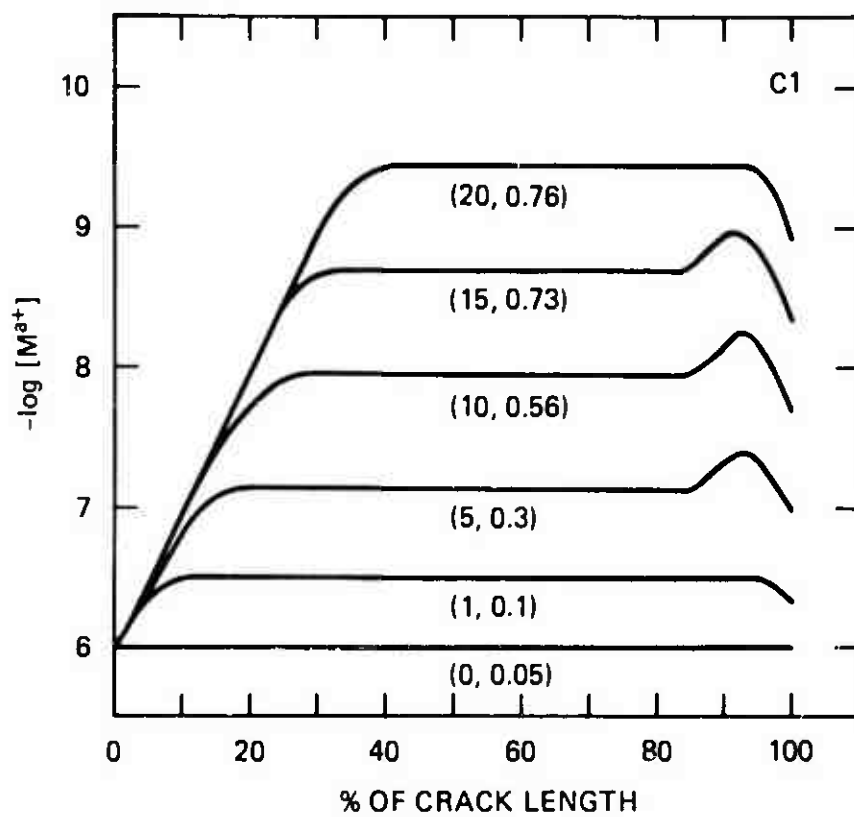
Initial conditions C1 in Table 5.



(a) Interfacial Current : $1 \rightarrow M^{a+}$

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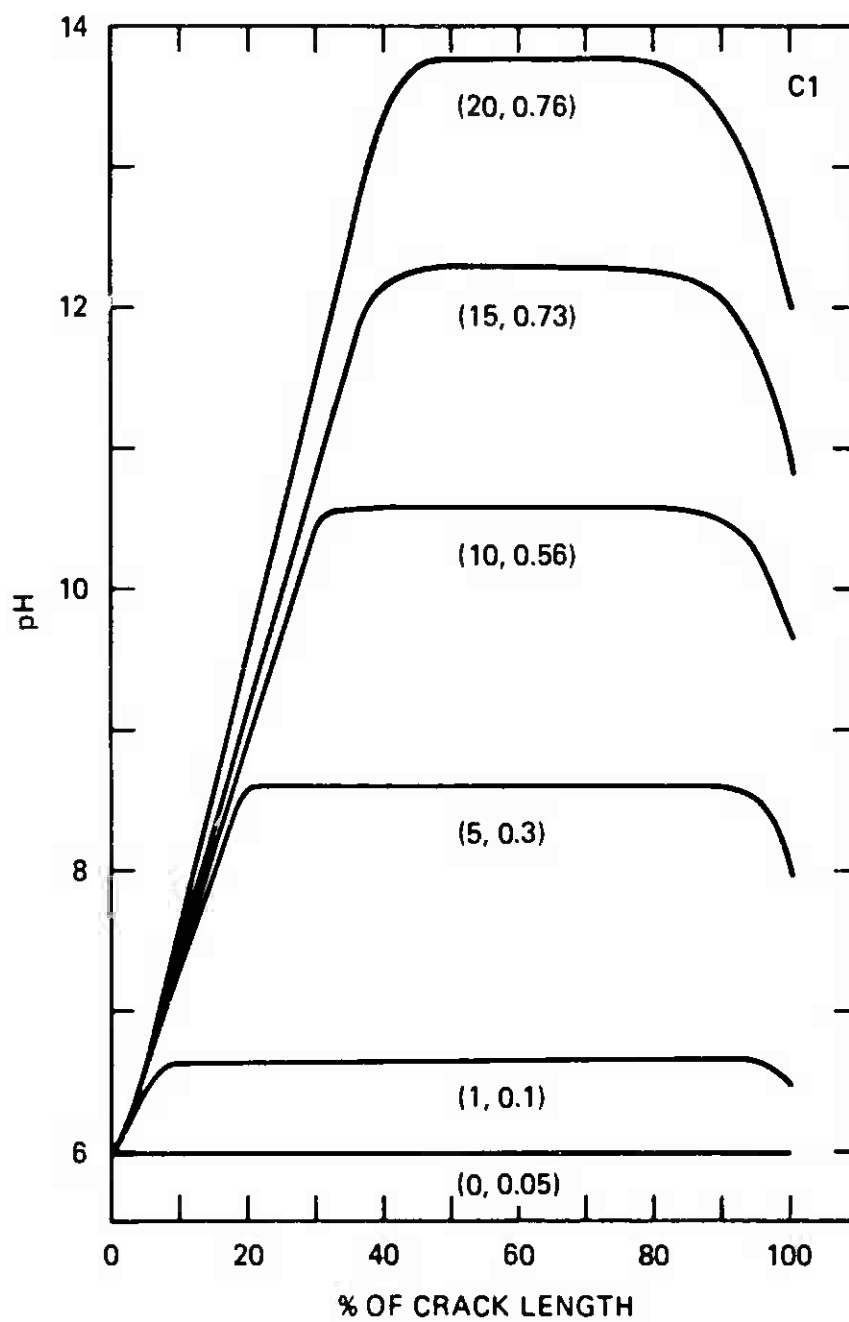
FIGURE 25 OC TRANSMISSION LINE MODEL CALCULATIONS OF INTERFACIAL CURRENT, METAL ION CONCENTRATION, AND CRACK ELECTROLYTE pH AS A FUNCTION OF DISTANCE INTO CRACK



(b) Metal Ion Concentration

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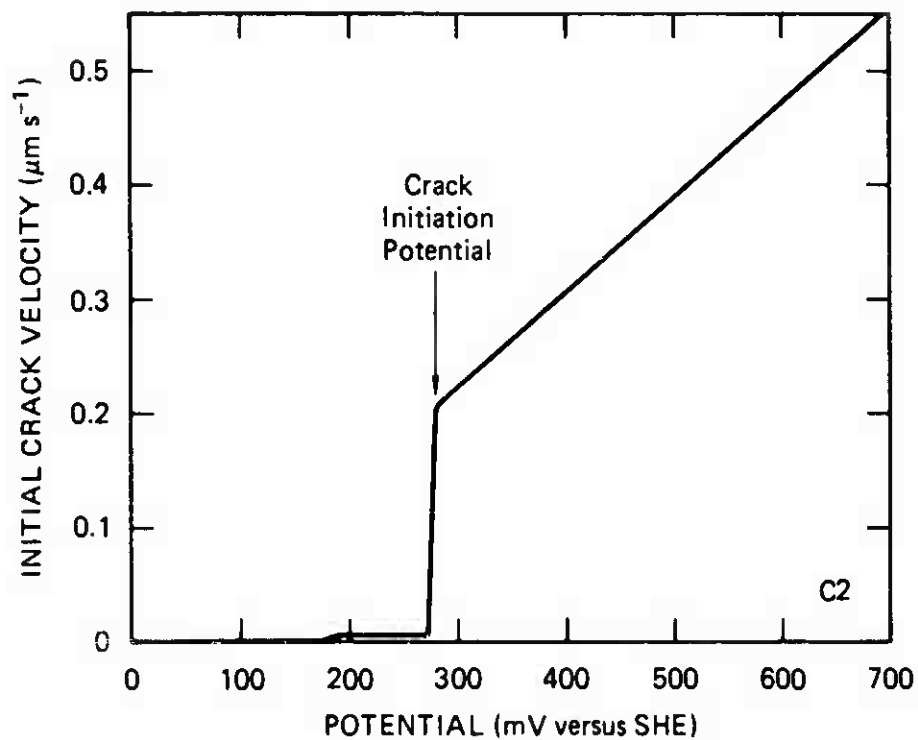
FIGURE 25 DC TRANSMISSION LINE MODEL CALCULATIONS OF INTERFACIAL CURRENT, METAL ION CONCENTRATION, AND CRACK ELECTROLYTE pH AS A FUNCTION OF DISTANCE INTO CRACK (Continued)



(c) Crack Electrolyte pH

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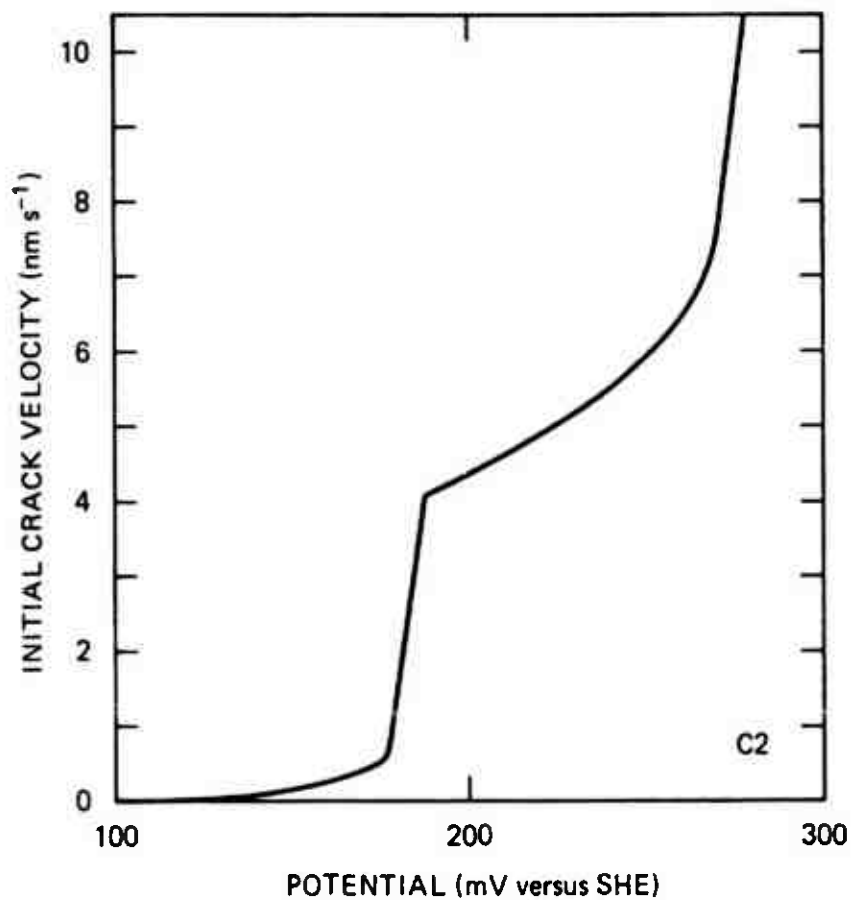
FIGURE 25 DC TRANSMISSION LINE MODEL CALCULATIONS OF INTERFACIAL CURRENT, METAL ION CONCENTRATION, AND CRACK ELECTROLYTE pH AS A FUNCTION OF DISTANCE INTO CRACK (Concluded)



(a) Velocity Versus Potential

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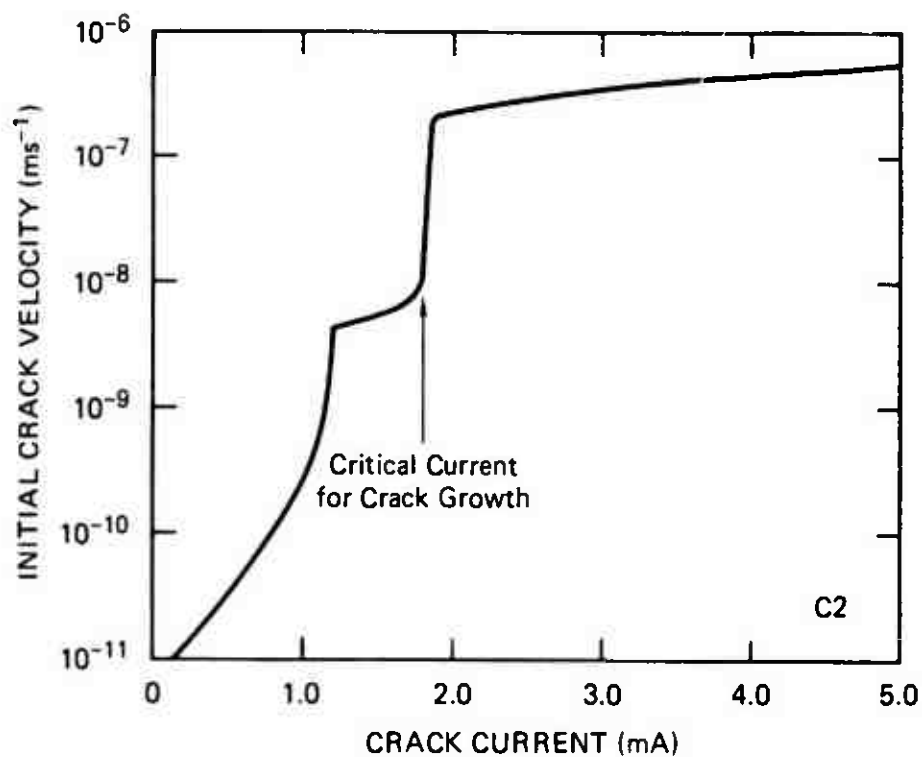
FIGURE 26 DC TRANSMISSION LINE MODEL CALCULATIONS OF VELOCITY VERSUS APPLIED POTENTIAL, VELOCITY VERSUS POTENTIAL (EXPANDED), AND LOG (VELOCITY) VERSUS APPLIED CURRENT



(b) Velocity Versus Potential (Expanded Scale)

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FIGURE 26 DC TRANSMISSION LINE MODEL CALCULATIONS OF VELOCITY VERSUS APPLIED POTENTIAL, VELOCITY VERSUS POTENTIAL (EXPANDED), AND LOG (VELOCITY) VERSUS APPLIED CURRENT (Continued)



(c) Log (Velocity) Versus Current

JA-4333-30

FIGURE 26 DC TRANSMISSION LINE MODEL CALCULATIONS OF VELOCITY VERSUS APPLIED POTENTIAL, VELOCITY VERSUS POTENTIAL (EXPANDED), AND LOG (VELOCITY) VERSUS APPLIED CURRENT (Concluded)

Figure 24 presents profiles of the potential difference between the solid and electrolyte phases (the potential driving force for electrochemical reaction) as a function of distance and time. For this example the equilibrium potential for metal dissolution is taken to be -200 mV versus the standard hydrogen electrode (SHE); thus, the baseline of this plot represents the approximate potential of zero dissolution current. As expected, the potential decreases between the crack orifice and the crack tip due to the finite conductivity of the electrolyte, the existence of electrochemical reactions at the crack walls, and the presence of reaction products in the crack electrolyte volume. Somewhat unexpectedly, for the conditions chosen, this potential drop is not a large fraction of the total overvoltage driving metal dissolution, and the potential drop decreases (as a percentage) with increasing crack length.

This observation is surprising in view of the results of previous calculations.^{8,9} Nevertheless, it is necessary that a significant fraction of the externally imposed potential be reflected at the growing crack tip to account for the observation of a critical potential for crack growth.⁶⁰

The origins of the deceleration in crack growth rate observed after 10 days for computation C1 can be seen clearly in Figures 25(a) through (c). These figures show a normalized crack length, with the time of growth and actual length given in parentheses. Figure 25(a) presents the component of the total interfacial current due to metal dissolution via reaction (5.1), as a function of time and length. The ordinate is plotted logarithmically to accommodate the large range of interfacial currents. Independent of time and length, the majority of the dissolution current flows from the region of film rupture at the crack tip. Despite the presence of a passivating oxide film, some metal dissolution also occurs on the walls of the crack. To a first approximation, however, the crack can be considered as active at the tip, partially active at the orifice, and passive (with respect to metal dissolution) in the central segments.

Figure 25(b) shows the concentration of metal ions (plotted as $-\log[\text{metal ion}]$) within the crack volume. For the example calculated the concentration is constant before the imposition of an external current, at a value determined by the chemical equilibrium between metal ions, hydrogen ions, and the surface metal oxide. As the crack grows, metal ions become depleted in the central segments due to the formation of metal oxide. Metal ions are produced by dissolution at the crack tip, but the effect of this concentration does not propagate deeply along the crack length.

Because reaction (5.2) is assumed to be at equilibrium, the depletion of metal ions in the central segments requires that the hydrogen ion concentration also be low. Thus, Figure 25(c) shows a trend toward alkalinity in the crack volume, with local acidification at the crack tip.

A second series of calculations was performed to determine the effect of crack current (or external potential) on the initial crack velocity. The parameters used are listed as "C2" in Table 5, and the results are summarized in Figures 26(a) through (c). Figure 26(a) shows the steady state crack velocity for a vestigial crack 0.1 cm long, plotted versus the potential of the electrolyte at the crack orifice for $K = 10^{-6}$. This plot exhibits a discontinuity at about 275 mV versus SHE. Below this potential the crack grows very slowly, whereas at higher potentials crack velocity increases roughly linearly with potential. One can interpret this discontinuity as a crack initiation potential although a closer inspection of the velocity versus potential profile near 200 mV [see Figure 26(b)] reveals two abrupt steps in velocity, one at 180 mV and the other at 275 mV. Figure 26(c) shows the same data plotted as the logarithm of crack velocity versus the current that flows into the crack, which allows us to determine the critical current for crack growth of ~ 18 mA for the conditions selected.

The results obtained for a chemical rate constant of 10^{-3} are not plotted but show that, with larger values of the chemical rate constant, the discontinuities in velocity, shown in Figure 26, disappear, and the

crack growth rate becomes a simple monotonic function of potential (or current). A second major effect of the chemical rate constant is that large values of the chemical rate constant result in general acidification of the crack electrolyte.

Section 5

CONCLUSIONS

From the results of this program, we draw the following conclusions regarding the use of AC impedance techniques and transmission line modeling to obtain electrochemical/mechanical properties states distributed within actively growing environmentally assisted cracks:

- The AC impedance response of the uncracked Ti-6Al-4V was found to behave as if the titanium alloy were covered with a dense TiO_2 semiconducting oxide layer. The HY80 exhibited more complex behavior although more typical of a corroding electrode. At transpassive and cathodic potentials the electrode impedance behavior was dominated by diffusional behavior, whereas in the potential range where a pseudo-passive film is expected to form, the impedance response was dominated by the double-layer capacitance in the electrolyte.
- The AC impedance response measured on cracked Ti-6Al-4V specimens under corrosion-fatigue conditions was found to depend on environmentally induced crack growth, total crack length, and change in stress intensity (ΔK). The electromechanical impedance of HY80 steel undergoing corrosion fatigue was modeled as a simplified equivalent circuit. The electromechanical impedance HY80 was also measured. This electromechanical impedance technique was sensitive to crack wall area at frequencies above 1 Hz and more sensitive to the crack tip at mechanical frequencies below 0.1 Hz.
- A DC transmission line model of growing corrosion-fatigue cracks constructed from HY80 undergoing corrosion fatigue was used to predict crack growth rates and potential and chemistry distributions within the crack. The predicted crack growth rates were in reasonable agreement with the experimentally measured values. The model also predicted a reasonable ΔK threshold for crack growth. At present, the model treats the crack tip region rather simply, but several models exist that could be incorporated rather easily in the future.

The results of this program have shown that a technique combining AC impedance, electrochemical/mechanical impedance, and transmission line

modeling offers the potential to determine both the mechanical and electrochemical processes that occur within stress corrosion and corrosion-fatigue cracks. At present, it is one of the few techniques with this capability. The results did not conclusively show that the combination of AC impedance, electromechanical impedance, and transmission line modeling can be used quantitatively to predict crack growth rates because the transmission line model was not used to reproduce the electromechanical impedance. We recommend additional effort to use the transmission line model in conjunction with the electromechanical/electrochemical impedance to obtain the critical mechanical and chemical parameters at the crack tip. It is clear that, with more modeling and experimental work on a wider variety of materials, load cycles, and aqueous environments, the electrochemical/mechanical technique developed in this program can become an important research tool.

REFERENCES

1. A. J. Forty and D. Van Rooyen, Eds., Proceedings of Conference on Fundamental Aspects of Stress Corrosion Cracking (NACE, Houston, Texas, 1969).
2. O. F. Devery, A. J. McEvily, and R. W. Staehle, Eds., Corrosion Fatigue: Chemistry, Mechanics and Microstructure (NACE, Houston, Texas, 1979).
3. Z. A. Foroulis, Ed., Proceedings of Conference on Environment-Sensitive Fracture of Engineering Materials (The Metallurgical Society of AIME, Warrendale, Pennsylvania, 1979).
4. J. C. Scully, Ed., The Theory of Stress Corrosion Cracking in Alloys, (NATO, Brussels, 1971).
5. A. J. McEvily and A. P. Bond, J. Electrochem Soc., 112, 131 (1965).
6. F. P. Ford, Metal Science, 326 (July 1978).
7. H. L. Logan, J. Res. Nat. Bur. Stand., 48, 99 (1952).
8. P. Doig and P.E.J. Flewitt, Proc. Roy. Soc., 357, 439 (1977).
9. P. Doig and P.E.J. Flewitt, Met. Trans., 124, 923 (1981).
10. R. P. Wei and J. D. Landes, Mater. Res. Stand., 9, 25 (1969).
11. P. B. Dawson and R. M. Pelloux, Met. Trans., 54, 723 (1974).
12. D. Schlain, "Corrosion Properties of Titanium and Its Alloys," Bureau of Mines Bulletin No. 619, U.S. Department of the Interior (1964).
13. J. D. Jackson and W. K. Boyd, "Corrosion of Titanium," DMIC Memorandum 218 (Battelle Memorial Institute, Columbus, Ohio, 1966).
14. Werkst. Korros., 30, 846 (1979).
15. J. F. Newman, Corrosion Science, 21, 487 (1981).
16. R. D. Caligiuri, L. E. Eiselstein, and M. J. Fox, "Low Temperature Sensitization of Weld Heat-Affected Zones in Type 304 Stainless Steel," lecture presented at Proceedings of International Atomic Energy Agency Specialists Meeting on Subcritical Crack Growth, held at Freiburg, Germany (May 1981).

17. F. P. Ford, "A Mechanism of Environmentally Controlled Crack Growth of Structural Steels in High Temperature in High Temperature Water," lecture presented at Proceedings of International Atomic Energy Agency Specialists Meeting on Subcritical Crack Growth," held at Freiburg, Germany (May 1981).
18. H. Riedel and J. R. Rice, Fracture Mechanics, P. C. Paris, Ed. (ASTM STP 700 1980), p. 112.
19. H. Riedel, J. Mech. Phys. Solids, 29, 35 (1981).
20. T. P. Hoar and F. P. Ford, Corrosion Science, 13, 729 (1973).
21. F. P. Ford, "Understanding Micromechanisms of Fracture," lecture presented at Gordon Conference, New Hampshire (1981).
22. D. D. Macdonald and M.C.H. McKubre, "Impedance Measurement in Electrochemical Systems," Chapter 2 in Modern Aspects of Electrochemistry, J. O'M Bockris, Ed., Vol. 16 (Plenum, New York, 1982).
23. D. D. Macdonald and M.C.H. McKubre, "Electrochemical Impedance Techniques in Corrosion Science," in Electrochemical Corrosion Testing, ASTM STP 727, Florian Mansfeld and Ugo Bertocci, Eds. (ASTM, 1981), pp. 110-169.
24. M. Sluyters-Rehback and J. H. Sluytera, in Electroanalytical Chemistry, Vol. 4, A. J. Bard, Ed. (Marcel Dekker, New York, 1970), pp. 1-128.
25. L. E. Elselstein, R. D. Caligiuri, S. S. Wing, and B. C. Syrett, "Accelerated Corrosion of Copper-Nickel Alloys in Sulfide-Polluted Seawater: Mechanism No. 2," lecture presented at Corrosion 82, Houston, Texas (1982).
26. M.C.H. McKubre and D. D. Macdonald, "The Rotating Cylinder-Collector Electrode (RCCE)," J. Electrochem. Soc., 127, 632 (1980).
27. O. S. Ksenzheck and V. V. Stender, Dokl. Akad. Nauk SSR, 106, 487 (1956); 107, 280 (1956).
28. M.C.H. McKubre, "Equilibrium and Steady State Studies of Continuous Flow-Through Electrode Systems," report to The University, Southampton University, Southampton, England (1978).
29. J. McHardy, J. M. Baris, and P. Stonehart, J. Appl. Electrochem, 6, 371 (1976).
30. J. O'M Bockris and A.J.N. Reddy, Modern Electrochemistry (Plenum Press, New York, 1973).

31. M.C.H. McKubre, Ph.D. thesis, Victoria Univeraity, Wellington, New Zealand (1976).
32. J. H. Sluyters, thesis, Utrecht, The Netherlands (1959).
33. A. B. Yzermans, thesis, Utrecht, The Nederlanda (1965).
34. P. Drosaback and J. Schultz, *Electrochim. Acta*, 9, 1391 (1969); 11, 669 (1966).
35. J. R. Macdonald, *J. Electroanal. Chem.*, 32, 317 (1971).
36. D. D. Macdonald, Transient Techniques in Electrochemiatry (Plenum Press, New York, 1977).
37. M. Stern and A. L. Geary, *J. Electrochem. Soc.*, 104 (1), (1957).
38. G.H.J. Broers and M. Schenke, in International Symposium Brennstoffelmente, K. Schwabe and E. Winkler, Eds. (Akademic-Verlag, Berlin, 1968), p. 299.
39. G.H.J. Broers and M. Schenke, in Hydrocarbon Fuel Cell Technology, B. S. Baker, Ed. (Academic Presa, New York, 1965), p. 225.
40. G.H.J. Broera, in Fuel Cella (American Institute of Chemical Engineers, New York, 1963), p. 90.
41. K. Mund, G. Richter, and F. von Sturm, *J. Electrochem. Soc.*, 124, 1 (1977).
42. M.C.H. McKubre and G. J. Hills, "The Use of AC Impedance Meaaurements to Characterize the Steady-State Propertiea of Continuous Flow-Through Electrodes" (to be published).
43. G. J. Hills and M.C.H. McKubre, SRI International (unpublished work).
44. M.C.H. McKubre and G. J. Hills, FORTAN IV programs written at The University, Southampton University, Southampton, England.
45. M. J. Madou and M.C.H. McKubre, *J. Electrochem. Soc.* 130, 5 (1983).
46. M. J. Madou, "A Semiconductor Electrochemiatry Approach to the Study of Oxide Films on Nickels, Iron and Cadmium Electrodes," SRI Annual Report on Project 5703 (1984).
47. D. D. Macdonald and M.C.H. McKubre, Chapter 2 in Modern Aspects of Electrochemistry, No. 14, O.M. Bockris, B. E. Conway, and R. E. White, Eds. (Plenum Press, New York, 1962).
48. G. Gabrielli and M. Keddam, *Electrochim. Acta*, 19, 355 (1974).

49. R. D. Armstrong, M. P. Bell, and A. A. Metcalfe, J. Electroanal. Chem., 84, 6 (1977); K. L. Bladen, J. Appl. Electrochem., 7, 345 (1977); A. A. Metcalfe, J. Electroanal. Chem., 88, 187 (1978).
50. D. Lelevre and V. Plichon, Electrochim. Acta, 23, 725 (1978).
51. P. Casson, N. A. Hampson, and M. J. Willars, J. Electroanal. Chem., 97, 21 (1979).
52. R. D. Armstrong, M. F. Bell, and A. A. Metcalfe, J. Electroanal. Chem., 77, 287 (1977).
53. E399, Volume 10, "1982 Annual Book of ASTM Standards," ASTM, p. 611.
54. A. Saxena and S. J. Hudak, Int. J. Fract., 14, p. 453 (1978).
55. M. L. Williams, J. Appl. Mech., 24, 109-114 (1957).
56. J. R. Rice and M. A. Johnson, in Elastic Behavior of Solids, M. F. Kanninen et al.
57. J. W. Hutchinson, J. Mech. Phys. Solids, 16, 13-31 (1968).
58. J. R. Rice and G. F. Rosengren, J. Mech. Phys. Solids, 16, 1-12 (1968).
59. R. M. McMeeking, J. Mech. Phys. Solids, 25, 357-381 (1977).
60. Private communication, D. D. Macdonald, SRI International (January 1986).

Appendix A

IMPEDANCE DATA MANAGEMENT AND CONTROL PROGRAM

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1  REM "OMSS.MAIN 15/JUN/1983
3  REM BY M.C.H.MCKUBRE
10 HINEM: 36300: LOMEN: 24577
90 ZNZ = 120: IF WPZ < > 0 THEN 1000
100 DIM ZM(128),ZM(5,ZNZ),ZZ(9),ZT(32),ZOB(8)
110 PRINT CHR$(4);"BLOAD B.FRA"
140 ZM(1) = 1:ZM(2) = 1:ZM(11) = 100:ZM(12) = 1:ZM(13) = 1:ZM(21) = 1:ZM(22) = 1:ZM(23) = 1:ZM(24) = 1:
    ZM(25) = 1:ZM(34) = 65535:ZM(35) = 1:ZM(38) = ZNZ:ZM(39) = 1.1:ZM(44) = 1:ZM(45) = 0201:ZM(49) = 2
    00
150 ZM(51) = 1:ZM(53) = 1:ZM(55) = 1:ZM(56) = ZNZ:ZM(57) = 1:ZM(84) = 2:ZM(85) = 2:ZM(86) = 2:ZM(121) =
    2:ZM(122) = 1:ZM(123) = 1
160 X = FRE(0):SBZ = 6:OBZ = 1:VBZ = 23
170 IF SZ < 4 OR SZ > 6 THEN SZ = 5:OZ = 1:VZ = 0
200 GOSUB 20000
300 DATA "FR","AM","BI","MF","MO","ZSY","LE","SR","SL","AC","AS","AV","AE","AP","QA","QB","QM","SQ","S
    G","RG"
320 DATA "IS","IC","NS","MC","HA","AU","RA","OE","OC","IP","SA","SI","RE","NA","NI","GO","GO","GS","GR
    ","NH","NS","SS","HS","SC","SO","CO"
340 DATA "VE","AA","PO","XI","XH","XL","XO","YI","YH","YL","YO","SP","PL","SM","ST","PG","VA","UP","O
    N","FD","FO","FC","LL"
360 DATA "BK","BL","BE","BC","BF","BB","BO","BI","BQ","BP","EP","JP","CP","TH","TT","OP","FN"
380 DATA "AF","BF","RF","TF","UA","UB","UR","UT","UG","LA","LB","LR","LT","LG","SV","PP","PS","OS","OT
    ","RR","RH"
400 DATA "NR","NA","PN","ER","AI","AR","TS"
1000 TEXT: POKE 34,0: HOME: PRINT
1100 PRINT: PRINT "PROGRAM OPTIONS ARE:"
1120 PRINT: PRINT " 1...SET UP SOLARTRON"
1140 PRINT: PRINT " 2...HELP"
1160 PRINT: PRINT " 3...TAKE MEASUREMENTS"
1180 PRINT: PRINT " 4...CHAIN BOOE PLOT"
1200 PRINT: PRINT " 5...CHAIN NYQUIST PLOT"
1220 PRINT: PRINT " 6...SAVE DATA ON DISK"
1230 PRINT: PRINT " 7...RETRIEVE DATA FROM DISK"
1240 PRINT: PRINT " 8...SET TIME"
1245 PRINT: PRINT " 9...CHAIN ANALYSIS PROGRAM"
1250 PRINT: PRINT " 0...EXIT PROGRAM"
1260 ZZ(3) = 0: VTAB(23):ZZ(4) = 0:ZZ(5) = 9: GOSUB 10100
1280 IF ZEZ(0) = 1 THEN 1000
1300 ON ZZ(3) GO 1500,2500,3000,4000,5000,6000,7000,8000,9700
1320 HOME: VTAB 9: PRINT "EXIT PROGRAM": PRINT: PRINT "TYPE GOTO 1000 TO RESUME": END
1500 GOSUB 15000: GOTO 1000
1900 ZM(128) = 1:M# = "TIF2": GOSUB 29000:ZZ(4) = ZZ(3):M# = "TIF0": GOSUB 29000: PRINT: PRINT "RS = "

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      ZZ(4): PRINT : INPUT "USE THIS VALUE (Y/N) ? ";M$: IF M$ < > "Y" THEN 15000
1920 ZM(51) = ZZ(4): GOTO 1500: REM RP
2000 NOME : PRINT "INITIALISE"
2020 GOSUB 20000:M$ = ":'TT2'": GOSUB 21000
2040 GOSUB 29000: REM KEITNLEY
2060 GOTO 15000
2500 NOME : VTAB 5: PRINT " HELP:": PRINT " ----": VTAB 10: PRINT " THERE IS NO HELP AVAILABLE HER
E.": PRINT "LIFE IS LIKE THAT. IT CAN SOMETIMES BE": PRINT "NARO AND CRUEL.": PRINT " IF YOU DON
'T KNOW WHAT YOU ARE DOING"
2510 PRINT "IT IS POSSIBLE THAT YOU SHOULDN'T": PRINT "BE DOING IT.": PRINT " PLEASE DO NOT HESITAT
E TO NOT": PRINT "CALL ME,": VTAB 19: NTAB 9: PRINT "MIKE"
2520 VTAB 23: GET Z0$(0): PRINT Z0$(0): GOTO 1000
3000 NOME : VTAB 3: PRINT "NAME AND LOCATION OF SAVE DATA FILE"
3010 GOSUB 11500: PRINT : PRINT "FILE NAME WILL BE PRECEDED BY OMSS(0)-": PRINT : INPUT "ENTER FILE NA
ME = OMSS(0)-":Z0$(0)
3015 X = FRE (0):ZF$ = Z0$(0):ZZ(8) = 77:Z0$(0) = "OMSS(P)-" + ZF$: GOSUB 11400:ZF$ = "OMSS(0)-" + ZF$
+ "$":ZZ(8) = 78
3020 PRINT : PRINT "STARTING FILE $ ":ZZ(3) = ZFX:ZZ(4) = 0:ZZ(5) = 100:ZZ(6) = 1: GOSUB 10100: IF ZE
X(0) = 1 THEN 3020
3030 ZFX = ZZ(3):ZM(3) = ZM(118)
3040 X = FRE (0): POKE 34,0: NOME : POKE 34,3: VTAB 1: PRINT "MEASUREMENT MODE # ":ZM(127): VTAB 2: PRINT
ZF$:ZF$: VTAB 3: PRINT "SCALE FACTOR ":ZM(53)
3050 ZM(47) = 0: NOME : VTAB 5: PRINT "STATUS PAGE": PRINT "----- ----": VTAB 8: PRINT "TOTAL # OF POI
NTS ":ZMX: VTAB 10: PRINT "TIMED SWEEP": HTAB 19: PRINT "ON": IF ZM(125) = 0 THEN VTAB 10: NTAB
19: PRINT "OFF"
3060 VTAB 12: PRINT "DC VOLTAGE SWEEP": HTAB 19: PRINT "ON": IF ZM(120) = 0 THEN VTAB 12: NTAB 19: PRINT
"OFF"
3070 VTAB 14: PRINT "FREQUENCY SWEEP": HTAB 19: PRINT "ON": IF ZM(34) = ZM(35) THEN VTAB 14: NTAB 19
: PRINT "OFF"
3080 VTAB 16: PRINT "HARMONIC SWEEP": NTAB 19: PRINT "ON": IF ZM(122) = ZM(123) THEN VTAB 16: NTAB 1
9: PRINT "UFF"
3090 VTAB 18: PRINT "INPUT FRONT/REAR": HTAB 19: PRINT "FRONT": IF ZM(50) > 0 THEN VTAB 18: HTAB 19:
PRINT "REAR ": IF ZM(50) > 1 THEN VTAB 18: HTAB 19: PRINT "BOTH"
3100 VTAB 2: HTAB 28: PRINT "START @ ":ZM(124): VTAB 3: NTAB 29: PRINT "STOP @ ":ZM(125)
3110 IF ZM(126) > 0 THEN GOSUB 18200: IF ZZ(3) + ZZ(4) / 60 < ZM(124) THEN FOR I1 = 1 TO 4444: NEXT
I1: GOSUB 18000: GOTO 3110
3120 FPZ = 1: IF ZM(50) = 2 THEN FRZ = 2
3130 ZM(56) = INT (ZMX / (FRZ * ZM(55) * ZM(57)))
3140 ZM(39) = (ZM(34) / ZM(35)) ^ (1 / ZM(56))
3145 ZM(0,0) = ZMX: GOSUB 18200:ZM(1,0) = ZZ(3) + ZZ(4) / 60:ZM(2,0) = ZM(127):ZM(3,0) = ZM(53):ZM(4,0)
= 1250
3150 VTAB 23: PRINT ZM(39),ZM(57),ZM(56)
3160 VTAB 5: CALL - 958: PRINT
3170 J = 0: IF ZM(121) = 1 THEN ZM(3) = ZM(118): REM INITIAL DC
3175 GOSUB 3900: REM SET DISPLAY
3180 I1 = 3: GOSUB 17000
3190 FOR J2M = 1 TO 441 * ZM(117): NEXT J2M
3200 ZM(1) = ZM(35): REM F MIN.
3210 I1 = 1: GOSUB 17000
3220 ZM(29) = 0: IF ZM(11) > = ZM(49) THEN ZM(29) = 1: REM COUPLING
3230 I1 = 29: GOSUB 17100
3240 ZM(25) = ZM(122): REM INITIAL HARMONIC

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3250 I1 = 25: GOSUB 17000
3260 FRZ = 0: ZM(30) = 0: IF ZM(50) = 1 THEN ZM(30) = 1: FRZ = 1: REM REAR
3270 I1 = 30: GOSUB 17100: ZM(45) = 0100: IF ZM(127) = 2 THEN ZM(45) = 0200
3280 IF ZM(127) = 0 THEN ZM(45) = 0201
3290 J = J + 1: IF J = ZMZ AND ZM(128) = 1 THEN 3620
3295 IF J > ZMZ THEN 3580: REM FULL
3300 I1 = 45: GOSUB 17000: GOSUB 18000: I1 = 32: GOSUB 16900: REM MEASURE
3310 M# = ":OP2,I": I1 = 4: GOSUB 24000: IF ZZ(4) < > 0 THEN 3300
3320 FOR ZS = 1 TO 3: ZM(ZS - 1, J) = ZZ(ZS): NEXT ZS
3330 IF ZM(127) > 3 THEN I1 = 45: ZM(45) = 0200: GOSUB 17000: GOSUB 18000: M# = ":OP2,I": I1 = 4: GOSUB
24000: REM CH#2
3340 IF ZM(127) < 3 THEN ZM(3, J) = 1: ZM(4, J) = 0
3350 IF ZM(127) = 3 THEN ZM(3, J) = ZM(1, J): ZM(4, J) = ZM(2, J): ZM(1, J) = ZZ(2): ZM(2, J) = ZZ(3)
3360 IF ZM(127) = 4 THEN ZM(3, J) = ZZ(2) - ZM(1, J): ZM(4, J) = ZZ(3) - ZM(2, J)
3370 IF ZM(127) = 3 THEN ZM(3, J) = ZM(1, J): ZM(4, J) = ZM(2, J): ZM(1, J) = ZZ(2): ZM(2, J) = ZZ(3)
3380 IF ZM(127) = 5 THEN GOSUB 3800: GOTO 3420
3390 GOSUB 9500: ZM(3, J) = 1 / ZM(51): ZM(4, J) = 6.2B232 * ZM(0, J) * ZM(52): GOSUB 9500: ZM(1, J) = ZM(1, J)
/ ZM(53): ZM(2, J) = ZM(2, J) / ZM(53): REM SCALE
3400 GOSUB 9980: ZM(3, J) = ZM(3): REM MAG. & PHASE
3420 I1 = 1: M# = ":?ER": GOSUB 24000: VTAB 21: HTAB 12: PRINT ZZ(I1)
3430 ZZ(3) = 7: ZZ(4) = ZM(122): ZZ(5) = ZM(118): ZZ(6) = ZM(35): GOSUB 3990
3432 ZZ(3) = 8: ZZ(4) = ZM(123): ZZ(5) = ZM(119): ZZ(6) = ZM(34): GOSUB 3990
3434 ZZ(3) = 9: ZZ(4) = 1: ZZ(5) = ZM(120): ZZ(6) = ZM(39): GOSUB 3990
3436 ZZ(3) = 10: ZZ(4) = ZM(25): ZZ(5) = ZM(3): ZZ(6) = ZM(1): GOSUB 3990
3440 VTAB 12: HTAB 9: PRINT J - 1; "/"; ZMZ; TAB( 25); J; "/"; ZMZ
3450 FOR I1 = 0 TO 5: VTAB (13 + I1): HTAB 6: CALL - B6B: PRINT ZM(I1, J - 1); TAB( 24); ZM(I1, J): NEXT
I1
3460 INVERSE : VTAB 20: HTAB 12: Z0$(0) = "FRONT": IF ZM(30) = 1 THEN Z0$(0) = " REAR"
3462 PRINT Z0$(0); HTAB 28: Z0$(0) = "OC": IF ZM(29) = 1 THEN Z0$(0) = "AC"
3464 PRINT Z0$(0); HTAB 36: Z0$(0) = "OFF": IF ZM(14) = 1 THEN Z0$(0) = "OM "
3466 PRINT Z0$(0): NORMAL
3480 VTAB 4: CALL - B6B: IF ZM(47) = 999 THEN PRINT "TERMINATE"
3490 IF ZM(50) = 2 AND FRZ = 0 THEN ZM(30) = 1: FRZ = 1: GOTO 3270: REM REAR
3500 IF ZM(25) < ZM(123) THEN ZM(25) = ZM(25) + 1: GOTO 3250: REM LOOP H
3510 IF ZM(1) > = ZM(34) THEN 3540
3520 ZM(1) = ZM(1) * ZM(39): IF ZM(1) > ZM(34) THEN ZM(1) = ZM(34)
3530 GOTO 3210
3540 IF SGN (ZM(120)) * SGN (ZM(119) - ZM(3)) THEN ZM(3) = ZM(3) + ZM(120): GOTO 3180
3550 REM OC LIMIT REACHED
3560 IF ZM(121) = 1 THEN 3180
3570 GOTO 3210
3580 REM FULL
3590 GOSUB 18000
3600 ZM(124) = ZM(124) + ZM(126): REM INC.TIME
3610 X = FRE (0): ZFX = ZFX + 1: Z0$(0) = ZFX + STR$ (ZFX): ZZ(8) = 7B: GOSUB 11400: REM SAVE DATA
3612 IF (ZZ(3) + ZZ(4) / 100) > ZM(125) OR ZM(47) = 999 THEN 1000: REM TERMINATE
3616 IF ZM(121) = 2 THEN ZM(3) = ZM(3) + ZM(120): IF SGN (ZM(12)) = SGN (ZM(119) - ZM(3)) THEN 1000:
REM DC LIMIT
3618 GOTO 3040: REM CLOSE LOOP
3620 ZM(1) = 60: I1 = 1: GOSUB 17000: ZM(0, ZMZ) = 60: FOR A = 1 TO 441: NEXT A: M# = "T1F1": GOSUB 29200: Z
M(2, ZMZ) = ZZ(3): M# = "T1F0": GOSUB 29200: ZM(3, ZMZ) = ZZ(3)

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3630 ZM(18) = 0:II = 18: GOSUB 17000: FOR II = 1 TO 441: NEXT II:M# = "TIF1": GOSUB 29200:ZM(4,ZM#) = Z
  Z(3):M# = "T(F0)": GOSUB 29200:ZM(5,ZM#) = Z(3)
3640 II = 20: GOSUB 16900: GOTO 3420
3800 REM CHI=I,CM2=V
3820 ZM(3,J) = ZM(25):ZM(4,J) = Z(2):ZM(5,J) = Z(3)
3840 Z(2) = 1 / ZM(51):Z(3) = 6.28232 * ZM(0,J) * ZM(52):Z(4) = ZM(1,J) * Z(2) - ZM(2,J) * Z(3):ZM
  (2,J) = ZM(1,J) * Z(3) + ZM(2,J) * Z(2):ZM(1,J) = Z(4): REM I=E/R
3860 ZM(1,J) = ZM(1,J) * ZM(53):ZM(2,J) = ZM(2,J) * ZM(53):ZM(4,J) = ZM(4,J) * ZM(53):ZM(5,J) = ZM(5,J)
  * ZM(53): REM SCALE MULTIPLIER
3880 RETURN
3900 REM DISPLAY
3920 REM
3930 VTAB 6: CALL - 958: HTAB 8: PRINT "H   DCV   FREQUENCY": PRINT "INIT.": PRINT "FINAL": PRINT "
  STEP": PRINT "CURR.": FOR II = 0 TO 5: VTAB (13 + II): PRINT "#":II: NEXT II
3940 VTAB 20: PRINT "INPUT FROM      : COUPLING   :COMP "
3960 VTAB 21: PRINT "LAST ERROR: ": RETURN
3990 VTAB Z(3): HTAB 7: CALL - 868: PRINT Z(4): TAB( 11):Z(5): TAB( 18):Z(5): RETURN
4000 ZD$(0) = "BODE": GOSUB 19900
4020 NP% = 1: CALL 520"DMSS.BODE"
5000 ZD$(0) = "NYQUIST": GOSUB 19900
5020 NP% = 1: CALL 520"DMSS.NYQUIST"
6000 REM SAVE DATA TO DISK
6010 GOSUB 11500: PRINT : PRINT "FILE NAME WILL BE PRECEDED BY DMSS(D)-": PRINT : INPUT "ENTER FILE NA
  ME = DMSS(D)-":ZD$(0):ZD$(0) = "DMSS(D)-" + ZD$(0)
6020 Z(18) = 78: GOSUB 11420: GOTO 1000
6500 ZD$(0) = ZD$(0) + STR$ ( INT (Z(3) + 0.5)): RETURN
7000 REM RETRIEVE DATA FROM DISK
7040 X = FRE (0): GOSUB 11500: PRINT : PRINT "CURRENT FILE NAME = ":ZF%:"%":ZF%: PRINT : INPUT "  NEW
  FILE NAME = DMSS(D)-":ZD$(0):ZD$(0) = "DMSS(D)-" + ZD$(0): IF ZD$(0) < > "DMSS(D)-" THEN ZF% = Z
  D$(0)
7060 X = FRE (0): INPUT "  NEW FILE %   = ":ZF%:ZD$(0) = ZF% + "%" + STR$ (ZF%)
7080 Z(18) = 78: GOSUB 11300: GOTO 1000
8000 HOME : REM SET TIME
8020 GOSUB 18200: VTAB 8: PRINT "NEW TIME:": HTAB 9: INPUT "HOURS ":JZN: IF JZN > 99 OR JZN < 0 THEN 8
  020
8040 VTAB 11: HTAB 7: INPUT "MINUTES ":ZM(83): IF ZM(83) > 59 OR ZM(83) < 0 THEN 8040
8060 II = 83: GOSUB 17200: GOTO 1000
9000 REM DISPLAY COUNTER ROUTINE
9010 HTAB 30: PRINT "% ":JZN:" ": RETURN
9240 PR% 3: PRINT "@(:": PRINT "":ZD$(0):"X": PRINT "@?:@H:": PR% 0: INPUT ZD$(0): IN% 0: RETURN
9500 REM COMPLEXDIVISION
9520 Z(5) = ZM(3,J) * ZM(3,J) + ZM(4,J) * ZM(4,J)
9540 Z(6) = (ZM(1,J) * ZM(3,J) + ZM(2,J) * ZM(4,J)) / Z(5)
9560 Z(4) = (ZM(2,J) * ZM(3,J) - ZM(1,J) * ZM(4,J)) / Z(5)
9580 ZM(1,J) = Z(6):ZM(2,J) = Z(4): RETURN
9700 ZD$(0) = "ANALYSIS": GOSUB 19900
9720 CALL 520"DMSS.ANALYSIS"
9970 REM MAG. & PHASE
9980 ZM(3,J) = SQR (ZM(1,J) * ZM(1,J) + ZM(2,J) * ZM(2,J))
9985 ZM(4,J) = ATM (ZM(2,J) / ZM(1,J)) * 180 / 3.141592654)
9990 ZM(5,J) = LOG (ZM(3,J)) / LOG (10): RETURN
9999 PRINT CHR$( 13): CHR$( 4):"SAVEDMSS.MAIN": END

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10000 REM Y/N SUBR
10010 ZEZ(0) = 0: PRINT "YES ": GET ZD$(0):ZZ(3) = PEEK (36) - 4: IF ZD$(0) = "Y" OR ZD$(0) = CHR$ (
13) THEN ZZ(3) = 2: PRINT "": RETURN
10020 IF ZD$(0) = "N" THEN POKE 36,ZZ(3): PRINT "NO ":ZZ(3) = 1: RETURN
10030 ZEZ(0) = 1: GOSUB 10050: RETURN
10050 REM ERROR SUBR
10060 PRINT CHR$ (7):ZEZ(0) = 1: RETURN
10100 REM I/P SUBR
10110 CALL - B6B
10120 ZEZ(0) = 0: PRINT ZZ(3): INPUT " ";ZD$(0): IF ZD$(0) = "" THEN ZZ(7) = ZZ(3): GOTO 10170
10130 FOR I = 1 TO LEN (ZD$(0)):ZQ$ = MID$ (ZD$(0),I,1)
10140 IF ZQ$ = "+" OR ZQ$ = "-" OR ZQ$ = " " OR ZQ$ = "." OR ZQ$ = "E" THEN 10160
10150 IF ZQ$ < "0" OR ZQ$ > "9" THEN 10050
10160 NEXT I:ZZ(7) = VAL (ZD$(0))
10170 IF ZZ(7) < ZZ(4) OR ZZ(7) > ZZ(5) THEN 10050
10180 ZZ(3) = ZZ(7): IF ZZ(6) = 1 THEN ZZ(3) = INT (ZZ(7))
10190 FOR I = 0 TO 200: NEXT I: RETURN
11300 REM : LOAD ARRAY
11320 POKE 98,90: POKE 99,ZZ(8): CALL 38152
11330 PRINT CHR$ (4);"BLOAD"ZD$(0);",A": PEEK (38394) + PEEK (38395) * 256
11340 RETURN
11400 REM : SAVE ARRAY
11420 POKE 98,90: POKE 99,ZZ(8): CALL 38104
11430 PRINT CHR$ (4);"BSAVE"ZD$(0);",A" PEEK (38394) + PEEK (38395) * 256",L" PEEK (38396) + PEEK (3
8397) * 256"
11440 RETURN
11500 REM ASK SLOT,DRIVE AND VOLUME
11510 VTAB 6: CALL - 95B: PRINT "POINTERS CURRENTLY SET AT ": VTAB 8: PRINT " SLOT #";SZ: PRINT "
DRIVE #";DZ: PRINT " VOLUME #";VZ
11520 VTAB 12: PRINT "CHANGE POINTERS (Y/N) ? ": GET ZD$(0): IF ZD$(0) = "N" THEN 11550
11530 PRINT : PRINT :ZZ(3) = SZ:ZZ(4) = 4:ZZ(5) = 6:ZZ(6) = 0: PRINT " SLOT ": GOSUB 10120: IF ZEZ
(0) = 1 THEN 11530
11532 SZ = INT (ZZ(3) + 0.5)
11535 PRINT :ZZ(3) = DZ:ZZ(4) = 1:ZZ(5) = 2:ZZ(6) = 0: PRINT " DRIVE ": GOSUB 10120: IF ZEZ(0) = 1 THEN
11535
11537 DZ = INT (ZZ(3) + 0.5): IF SZ < > 6 THEN VZ = 0: GOTO 11550: REM FLOPPY
11540 PRINT :ZZ(3) = VZ:ZZ(4) = 1:ZZ(5) = 6:ZZ(6) = 0: PRINT " VOLUME ": GOSUB 10120: IF ZEZ(0) = 1
THEN 11540
11542 VZ = INT (ZZ(3) + 0.5)
11550 PRINT : PRINT "PRESS ANY KEY TO CATALOG ": GET ZD$(0): PRINT : PRINT CHR$ (4);"CATALOG,S"SZ",D"
DZ",V"VZ
11560 PRINT : PRINT "ANOTHER CATALOG Y/N ? ": GOSUB 10000: IF ZEZ(0) = 1 THEN 11560
11570 IF ZZ(3) = 2 THEN 11500
11580 RETURN
15000 TEXT : POKE 34,0: HOME : VTAB 5: PRINT "SET-UP OPTIONS ARE:"
15020 PRINT : PRINT " 1...RETURN TO MAIN MENU"
15040 PRINT : PRINT " 2...CREATE/MODIFY SET-UP FILE"
15060 PRINT : PRINT " 3...RETRIEVE SET-UP FILE FROM DISK"
15080 PRINT : PRINT " 4...SAVE SET-UP FILE TO DISK"
15100 PRINT : PRINT " 5...EXECUTE SET-UP FILE"
15120 PRINT : PRINT " 6...RESET (INITIALIZE) SOLARTRON"
15140 PRINT : PRINT " 7...RESET (INITIALIZE) KEITHLEY"

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15200 ZZ(3) = 1: VTAB (23):ZZ(4) = 1:ZZ(5) = 7: GOSUB 10100: IF ZEX(0) = 1 THEN 15000
15220 ON ZZ(3) GOTO 1000,15300,16600,16640,16700,2000,1900
15300 HOME : VTAB 5: PRINT "SET-UP WHICH SUBSYSTEM:"
15320 PRINT : PRINT " 1...GENERATOR"
15340 PRINT : PRINT " 2...ANALYSER"
15360 PRINT : PRINT " 3...SWEET(S)"
15380 PRINT : PRINT " 4...IMPEADANCE STANDARD"
15400 PRINT : PRINT " 5...MEASUREMENT CONFIGURATION"
15460 PRINT : PRINT " 0...RETURN TO SET-UP OPTIONS"
15480 ZZ(3) = 0: VTAB (23):ZZ(4) = 0:ZZ(5) = 5: GOSUB 10100: IF ZEX(0) = 1 THEN 15300
15500 ON ZZ(3) GOTO 15600,15800,16000,16300,16500
15520 GOTO 15000
15600 HOME : VTAB 3: PRINT "GENERATOR"
15610 VTAB 6: PRINT "FREQUENCY ":ZZ(3) = ZM(1):ZZ(4) = 1E - 5:ZZ(5) = 655.35:ZZ(6) = 0: GOSUB 10100: IF
ZEX(0) = 1 THEN 15610
15620 ZM(1) = ZZ(3)
15630 VTAB 9: PRINT "AMPLITUDE ":ZZ(3) = ZM(2):ZZ(4) = 0:ZZ(5) = 10.23:ZZ(6) = 0: GOSUB 10100: IF ZEX
(0) = 1 THEN 15630
15640 ZM(2) = ZZ(3)
15650 VTAB 12: PRINT "D.C. BIAS ":ZZ(3) = ZM(3):ZZ(4) = - 10.23:ZZ(5) = 10.23:ZZ(6) = 0: GOSUB 10100
: IF ZEX(0) = 1 THEN 15650
15660 ZM(3) = ZZ(3)
15666 IF ZM(2) + ABS (ZM(3)) > 14 THEN VTAB 8: PRINT "COMBINED VOLTAGE TOO LARGE": GOTO 15630
15670 VTAB 15: PRINT "WAVEFORM (SIN=0,SQR=1) ":ZZ(3) = ZM(4):ZZ(4) = 0:ZZ(5) = 1:ZZ(6) = 1: GOSUB 101
00: IF ZEX(0) = 1 THEN 15670
15680 ZM(5) = ZZ(3)
15690 VTAB 18: PRINT "AMPLITUDE COMP. (OFF=0,ON=1) ":ZZ(3) = ZM(14):ZZ(4) = 0:ZZ(5) = 1:ZZ(6) = 1: GOSUB
10100: IF ZEX(0) = 1 THEN 15690
15700 ZM(14) = ZZ(3)
15710 IF ZM(14) = 0 THEN 15300
15720 HOME : VTAB 5: PRINT "AMPLITUDE COMPRESSION ON"
15730 VTAB 8: PRINT "SOURCE CHANNEL ":ZZ(3) = ZM(11):ZZ(4) = 1:ZZ(5) = 2:ZZ(6) = 1: GOSUB 10100: IF Z
EX(0) = 1 THEN 15730
15740 ZM(11) = INT (100 * ZZ(3) + 0.5)
15750 VTAB 12: PRINT "VOLTAGE LEVEL ":ZZ(3) = ZM(12):ZZ(4) = 1E - 4:ZZ(5) = 300:ZZ(6) = 0: GOSUB 1010
0: IF ZEX(0) = 1 THEN 15750
15760 ZM(12) = ZZ(3)
15770 VTAB 16: PRINT "ERROR PERCENT ":ZZ(3) = ZM(13):ZZ(4) = 1:ZZ(5) = 50:ZZ(6) = 0: GOSUB 10100: IF
ZEX(0) = 1 THEN 15770
15780 ZM(13) = ZZ(3)
15790 GOTO 15300
15800 HOME : VTAB 3: PRINT "ANALYSER"
15810 VTAB 6: PRINT "INTEGRATION TIME (SECONDS) ":ZZ(3) = ZM(21):ZZ(4) = .01:ZZ(5) = 1E-4:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 15810
15820 ZM(21) = ZZ(3)
15830 VTAB 9: PRINT "MEASUREMENT DELAY ": GOSUB 15995:ZZ(3) = ZM(11):ZZ(4) = 0:ZZ(5) = 1E5:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 15830
15840 ZM(11) = ZZ(3)
15850 VTAB 14: PRINT "INITIAL HARMONIC ":ZZ(3) = ZM(25):ZZ(4) = 1:ZZ(5) = 16:ZZ(6) = 1: GOSUB 10100: IF
ZEX(0) = 1 THEN 15850
15860 ZM(25) = ZZ(3)

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15870 VTAB 18: PRINT "AUTO INTEGRATE OFF=0": PRINT "CH1(L)=2,CH2(L)=2,CH3(S)=3,CH2(S)=4": ZZ(3) = ZM(2
6):ZZ(4) = 0:ZZ(5) = 4:ZZ(6) = 1: GOSUB 10100: IF ZEX(0) = 1 THEN 15870
15880 ZM(26) = ZZ(3)
15900 VTAB 6: CALL - 95B: VTAB 8: PRINT "INPUT VOLTAGE RANGE AUTO=0": PRINT "30MV=1,300MV=2,3V=3,30V
=4,300V=5":ZZ(3) = ZM(27):ZZ(4) = 0:ZZ(5) = 5:ZZ(6) = 1: GOSUB 10100: IF ZEX(0) = 1 THEN 15900
15910 ZM(27) = ZZ(3)
15920 VTAB 13: PRINT "INPUT COUPLING ": PRINT "OC=0,AC=1,FREQUENCY TO CHANGE=XX":ZZ(3) = ZXX(1):ZZ(4)
= 0:ZZ(5) = 999:ZZ(6) = 0: GOSUB 10100: IF ZEX(0) = 1 THEN 15920
15930 ZM(49) = ZZ(3):ZM(29) = ZM(49): IF ZM(49) > 1 THEN ZM(29) = 0
15950 VTAB 28: PRINT "INPUT (FRONT=0,REAR=1,BOTH=2) ":ZZ(3) = ZM(50):ZZ(4) = 0:ZZ(5) = 2:ZZ(6) = 1: GOSUB
10100: IF ZEX(0) = 1 THEN 15950
15960 ZM(50) = ZZ(3):ZM(30) = ZM(50): IF ZM(50) > 1 THEN ZM(30) = 0
15990 GOTO 15300
15995 PRINT "(S=SECONDS,C=CYCLES) ":;11 = 24: PRINT "CYCLES ";: GET ZD(0): IF ZD(0) = "S" THEN HTAB
22: VTAB 10: PRINT "SECONDS":;11 = 23
15996 RETURN
16000 HOME : VTAB 3: PRINT "SWEEP(S)...# OF MEASUREMENTS = ":ZNX
16010 VTAB 6: CALL - 95B: PRINT "DC VOLTAGE SWEEP (V/M) ? ": GOSUB 10000:ZM(57) = 1: IF ZEX(0) = 1 THEN
16010
16020 IF ZZ(3) = 1 THEN ZM(118) = ZM(3):ZM(119) = ZM(3):ZM(120) = 0: GOTO 16100
16030 VTAB 9: PRINT "INITIAL DC VOLTAGE ":;ZZ(3) = ZM(3):ZZ(4) = - 10.23:ZZ(5) = 10.23:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16030
16040 ZM(118) = ZZ(3)
16050 VTAB 12: PRINT "FINAL DC VOLTAGE ":;ZZ(3) = ZM(119):ZZ(4) = - 10.23:ZZ(5) = 10.23:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16050
16060 ZM(119) = ZZ(3)
16070 VTAB 15: PRINT "DC VOLTAGE STEP ":;ZZ(3) = ZM(120):ZZ(4) = - 10.23:ZZ(5) = 10.23:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16070
16080 ZM(120) = ZZ(3)
16085 IF SGN (ZM(119) - ZM(118)) < > SGN (ZM(120)) THEN VTAB 8: PRINT "ARE YOU GOING TO CIRCLE INF
INITY ?": GOTO 16030
16088 IF ZM(120) = 0 THEN ZM(121) = 2:ZM(57) = 1:ZM(117) = 0: GOTO 16100
16090 VTAB 18: PRINT "FILL ARRAY BETWEEN DC STEPS (V/M)": GOSUB 10000:ZM(121) = ZZ(3): IF ZM(121) = 2
THEN 16100
16093 ZM(57) = INT (1.5 + (ZM(119) - ZM(118)) / ZM(120))
16095 VTAB 20: PRINT "DELAY BETWEEN DCV (/S) ":;ZZ(3) = ZM(117):ZZ(4) = 0:ZZ(5) = 1000:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16095
16097 ZM(117) = ZZ(3)
16100 VTAB 6: CALL - 95B: PRINT "FREQUENCY SWEEP (V/M) ? ": GOSUB 10000:ZM(56) = 1: IF ZEX(0) = 1 THEN
16100
16105 IF ZZ(3) = 1 THEN ZM(34) = ZM(11):11 = 34: GOSUB 21000:ZM(35) = ZM(11):11 = 35: GOSUB 21000: GOTO
16150
16110 VTAB 9: PRINT "FREQUENCY MINIMUM ":;ZZ(3) = ZM(35):ZZ(4) = 1E - 5:ZZ(5) = 65535:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16110
16120 ZM(35) = ZZ(3):11 = 35: GOSUB 17000
16130 VTAB 12: PRINT "FREQUENCY MAXIMUM ":;ZZ(3) = ZM(34):ZZ(4) = ZM(35):ZZ(5) = 65535:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16130
16140 ZM(34) = ZZ(3):11 = 34: GOSUB 17000
16150 ZM(55) = 1: IF ZM(34) > 32767 THEN ZM(25) = 1: GOTO 16200: REM NO HARMONIC POSSIBLE
16155 VTAB 6: CALL - 95B: PRINT "HARMONIC SWEEP (V/M) ? ": GOSUB 10000: IF ZEX(0) = 1 THEN 16150
16160 IF ZZ(3) = 1 THEN ZM(122) = ZM(25):ZM(123) = ZM(25): GOTO 16200

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16170 VTAB 9: PRINT "INITIAL HARMONIC # ";ZZ(3) = ZM(122):ZZ(4) = 1:ZZ(5) = INT (65535 / ZM(34)):ZZ(
6) = 1: GOSUB 10100: IF ZEX(0) = 1 THEN 16170
16180 ZM(122) = ZZ(3)
16190 VTAB 12: PRINT "FINAL HARMONIC # ";ZZ(3) = ZM(123):ZZ(4) = ZM(122):ZZ(5) = INT (65535 / ZM(34)
):ZZ(6) = 1: GOSUB 10100: IF ZEX(0) = 1 THEN 16190
16195 ZM(123) = ZZ(3):ZM(55) = ZM(123) - ZM(122) + 1
16200 VTAB 6: CALL - 95B: PRINT "TIMED SWEEP (Y/M) ? "; GOSUB 10000: IF ZEX(0) = 1 THEN 16200
16210 IF ZZ(3) = 1 THEN ZM(124) = 0:ZM(125) = ZM(124):ZM(126) = ZM(125): GOTO 16290
16220 GOSUB 18000: VTAB 9: PRINT ZD(0): REM CLOCK
16230 VTAB 12: PRINT "START MEASUREMENTS @ HH.MM ";ZZ(3) = ZM(124):ZZ(4) = 0:ZZ(5) = 24:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16230
16240 ZM(124) = ZZ(3)
16250 VTAB 15: PRINT "STOP MEASUREMENTS @ HH.MM ";ZZ(3) = ZM(125):ZZ(4) = ZM(124):ZZ(5) = 99.59:ZZ(6)
= 0: GOSUB 10100: IF ZEX(0) = 1 THEN 16250
16260 ZM(125) = ZZ(3)
16270 VTAB 18: PRINT "MEASUREMENT INTERVAL HH.MM ";ZZ(3) = ZM(126):ZZ(4) = 0:ZZ(5) = 24:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16270
16280 ZM(126) = ZZ(3)
16290 ZM(56) = INT (ZM(55) / (ZM(55) * ZM(57))): GOTO 15300
16300 HOME : VTAB 3: PRINT "SCALE FACTORS:"
16310 VTAB 6: PRINT "// RESISTANCE STANDARO ";ZZ(3) = ZM(51):ZZ(4) = .1:ZZ(5) = 1E9:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16310
16320 ZM(51) = ZZ(3)
16330 VTAB 10: PRINT "// CAPACITANCE STANDARO ";ZZ(3) = ZM(52):ZZ(4) = 0:ZZ(5) = 1E3:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16330
16340 ZM(52) = ZZ(3)
16350 VTAB 14: PRINT "IMPEOANCE SCALE FACTOR ";ZZ(3) = ZM(53):ZZ(4) = 1:ZZ(5) = 1E9:ZZ(6) = 0: GOSUB
10100: IF ZEX(0) = 1 THEN 16350
16360 ZM(53) = ZZ(3)
16490 GOTO 15300
16500 HOME : VTAB 3: PRINT "MEASUREMENT MODE:"
16510 VTAB 5: CALL - 95B: PRINT "INPUT(S): 0=2/1": HTAB 14: PRINT "1=1": HTAB 14: PRINT "2=2": HTAB
14: PRINT "3=(2-1)/1": HTAB 14: PRINT "4=1/(2-1)": HTAB 14: PRINT "5=1/2"
16520 VTAB 11:ZZ(3) = ZM(127):ZZ(4) = 0:ZZ(5) = 5:ZZ(6) = 1: GOSUB 10100: IF ZEX(0) = 1 THEN 16520
16525 ZM(127) = ZZ(3)
16530 VTAB 13: PRINT "OPERATOR: 0=UNITY": HTAB 14: PRINT "1=JW": HTAB 14: PRINT "2=1/JW": HTAB 14: PRINT
"3=JW^2": HTAB 14: PRINT "4=1/JW^2"
16540 VTAB 19:ZZ(3) = ZM(116):ZZ(4) = 0:ZZ(5) = 4:ZZ(6) = 0: GOSUB 10100: IF ZEX(0) = 1 THEN 16540
16545 ZM(116) = ZZ(3)
16550 VTAB 20: PRINT "COORDINATES 0=A/B": HTAB 14: PRINT "1=R/THETA": HTAB 14: PRINT "2=LOG.R/THETA"
16560 VTAB 23:ZZ(3) = ZM(146):ZZ(4) = 0:ZZ(5) = 2:ZZ(6) = 0: GOSUB 10100: IF ZEX(0) = 1 THEN 16560
16565 ZM(146) = ZZ(3)
16570 GOTO 15300
16600 HOME : VTAB 3: PRINT "RETRIEVE SET-UP FILE"
16620 GOSUB 166B0:ZZ(B) = 77: GOSUB 11300: GOTO 15000
16640 HOME : VTAB 3: PRINT "SAVE SET-UP FILE TO DISK"
16660 GOSUB 166B0:ZZ(B) = 77: GOSUB 11400: GOTO 15000
16680 X = FRE (0): GOSUB 11500: PRINT : PRINT "FILE NAME WILL BE PRECEDED BY OMSS(P)-": PRINT : INPUT
"ENTER FILE NAME = OMSS(P)-":Z0(0):ZF0 = "OMSS(P)-" + Z0(0):Z0(0) = ZF0: RETURN
16700 HOME : VTAB 3: PRINT "EXECUTE SET-UP FILE"
16710 FOR I = 1 TO 6: GOSUB 17000: NEXT I

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16720 II = 14: GOSUB 17000: IF ZN(14) = 1 THEN FOR II = 11 TO 13: GOSUB 17000: NEXT II
16730 II = 20: GOSUB 16900
16740 II = 21: GOSUB 17000: II = 24: IF ZN(23) > 0 THEN II = 23
16750 GOSUB 17000: II = 25: GOSUB 17000: II = 26: GOSUB 17000
16760 FOR II = 27 TO 30: FOR JZN = 1 TO 2: GOSUB 17100: NEXT JZN: NEXT II
16770 II = 34: GOSUB 17000: II = 35: GOSUB 17000: II = 46: GOSUB 17000
16780 ZN(45) = 0201: IF ZN(127) > 0 THEN ZN(45) = 0100: IF ZN(127) > 1 THEN ZN(45) = 0200: IF ZN(127) >
    2 THEN ZN(45) = 0100
16790 II = 45: GOSUB 17000: II = 68: GOSUB 16900
16800 JZN = 0: II = 85: ZN(85) = 1: GOSUB 17200: REN DISPLAY
16802 JZN = 1: ZN(85) = 0: GOSUB 17200
16804 JZN = 2: ZN(85) = 1: GOSUB 17200
16806 JZN = 3: ZN(85) = 1: GOSUB 17200
16810 JZN = 1: II = 86: ZN(86) = 0: GOSUB 17200: REN DISPLAY
16811 JZN = 2: ZN(86) = 0: GOSUB 17200
16812 JZN = 3: ZN(86) = ZN(116): GOSUB 17200
16813 JZN = 4: ZN(86) = 0: GOSUB 17200
16814 JZN = 5: ZN(86) = 0: GOSUB 17200
16816 II = 108: GOSUB 17000: II = 109: GOSUB 17000
16820 GOTO 1000
16900 RESTORE : FOR I = 1 TO II: READ M$: NEXT I: M$ = ":" + M$ + ":" : GOSUB 21000: RETURN
17000 RESTORE : FOR I = 1 TO II: READ N$: NEXT I: N$ = ":" + N$ + STR$ (ZN(II)) + ":" : GOSUB 21000: RETURN

17100 FOR JZN = 1 TO 2: RESTORE : FOR I = 1 TO II: READ M$: NEXT I: M$ = ":" + M$ + STR$ (JZN) + "," +
    STR$ (ZN(II)) + ":" : GOSUB 21000: NEXT JZN: RETURN
17200 RESTORE : FOR I = 1 TO II: READ N$: NEXT I: N$ = ":" + M$ + STR$ (JZN) + "," + STR$ (ZN(II)) +
    ":" : GOSUB 21000: RETURN
18000 REN CLOCK
18010 ZZ(3) = PEEK ( - 16384) - 128: REN KEY PUSH
19020 IF ZZ(3) = 1 THEN GOTO 1000: REN ABORT
18080 IF ZZ(3) = 19 THEN 18220: REN STATUS
18090 IF ZZ(3) = 20 THEN ZN(47) = 999: REN TERMINATE
18100 IF ZZ(3) = 21 THEN ZN(47) = 0
18190 RETURN
18200 REN TIME
18220 II = 1: M$ = ":" ? TM0": GOSUB 24000: ZZ(3) = ZZ(II): N$ = ":" ? TN1": GOSUB 24000: ZZ(4) = ZZ(II): ZD(
    0) = "TIME IS " + STR$ (ZZ(3)) + ":" : N$ = STR$ (ZZ(4)): IF ZZ(4) < 9 THEN N$ = "0" + N$
18240 ZD(0) = ZD(0) + M$: VTAB 1: HTAB 28: PRINT ZD(0): RETURN : REN READ CLOCK
19900 REN CHAIN SUBROUTINE
19920 HOME : VTAB 9: NPX = 1: PRINT "LOADING DNSS." ZD(0)
19940 PRINT CHR$ (4); "BLOAD CHAIN,A520,5"SBX;" ,D1,V"VBX
19960 RETURN
20000 ZZ = 12
20010 ZD(4) = "0" + CHR$ (95) + CHR$ (ZZ + 64): ZD(5) = "0" + CHR$ (95) + "?" + CHR$ (ZZ + 32) +
    ":"
20020 ZD(6) = CHR$ (4) + "IN0": ZD(7) = CHR$ (4) + "PR00"
20030 ZD(8) = CHR$ (4) + "PR03": AA0 = "0" + CHR$ (95) + "(": "": BB0 = "X"0?:0H:"
20900 RETURN
21000 REN SEND DATA TO FRA
21030 PRINT ZD(8): PRINT ZD(5)
21040 PRINT N$
21050 PRINT ZD(6)

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21470 PRINT ZD$(7)
21500 RETURN
24000 REM DATA RETRIEVE
24030 PRINT ZD$(8): PRINT ZD$(5)
24040 PRINT CHR$(13): PRINT M$: GOTO 28500: PRINT ZD$(7): PRINT ZD$(6): RETURN
28500 PRINT CHR$(13): ZD$(4): ": PRINT ZD$(7): VTAB 23
28501 ON I1 - 1 GOTO 28504,28506,28508
28502 INPUT ZZ(1): PRINT ZD$(8): RETURN
28504 INPUT ZZ(1),ZZ(2): PRINT ZD$(8): RETURN
28506 INPUT ZZ(1),ZZ(2),ZZ(3): PRINT ZD$(8): RETURN
28508 INPUT ZZ(1),ZZ(2),ZZ(3),ZZ(4): PRINT ZD$(8): RETURN
29000 REM KEITHLEY MODEL 192 SET-UP
29200 ZD$(0) = M$ + "ROK00053H0Z0N1"
29220 VTAB 23
29240 PRINT ZD$(8): PRINT AA$: ZD$(0): BD$: PRINT ZD$(7): INPUT ZD$(0): PRINT ZD$(6): VTAB 23: PRINT "0"
29260 ZZ(3) = VAL ( MID$( ZD$(0),5)): RETURN

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Appendix B

DIFFUSION IN AN ANGULAR CRACK

This appendix gives the solution concentration as a function of time and position in an angular crack. The mathematical representation of the crack is shown in Figure B.1. A crack tip rupture and dissolution provides the concentration $C = 1$ up to the $r = a$ cell element of the angular crack. In this case, r_m is the distance from the crack origin to the m^{th} cell segment and Δ is the distance between cell segments. Thus,

$$r_m = m\Delta \quad (\text{B-1})$$

We need to solve for $c_m(t)$ where $c_m(t)$ = average concentration in $r_{m-1} < r < r_m$ at time t and

$$m = 1, 2, 3, \dots$$

Let $c = c(a, r, t)$ be the solution of the standard diffusion equation

$$\frac{\partial c}{\partial t} = D \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial c}{\partial r} \right) \quad (\text{B-2})$$

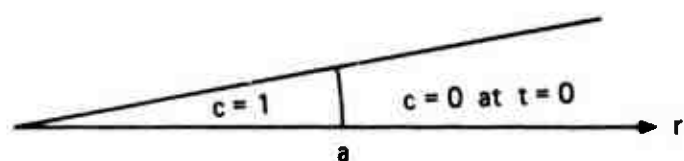
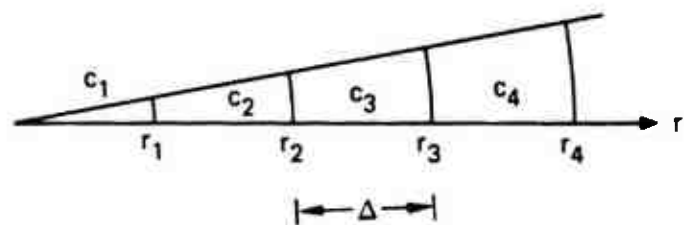
where D = diffusion coefficient with

$$c = \begin{cases} 1 & \text{for } r < a \\ 0 & \text{for } a < r \end{cases} \quad \text{at } t = 0$$

Assuming only nearest neighbors interact over short time t give

$$c_1(t) = c_2(0) + [c_1(0) - c_2(0)] J_-(1) \quad (\text{B-3})$$

and for $m = 2, 3, 4, \dots$; the solution for the concentration as a function of time and position along the crack is given by



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FIGURE B.1 MATHEMATICAL REPRESENTATION OF DIFFUSION
IN AN ANGULAR CRACK

$$c_m(t) = c_{m+1}(0) + [c_m(0) - c_{m+1}(0)] J_-(m) + [c_{m-1}(0) - c_m(0)] J_+(m-1)$$

(B-4)

where $J_-(m)$, a function of t as well as m , is the average concentration in cell m just to the left of a unit jump in concentration at $r = r_m$ and $J_+(m)$ is the average concentration in cell $(m+1)$ just to the right of the unit jump at $r = r_m$. That is,

$$J_-(m) = \frac{\int_{(m-1)\Delta}^{m\Delta} c(m\Delta, r, t) r dr}{\int_{(m-1)\Delta}^{m\Delta} r dr} \quad (B-5)$$

$$J_+(m) = \frac{\int_{(m+1)\Delta}^{m\Delta} c(m\Delta, r, t) r dr}{\int_{m\Delta}^{(m+1)\Delta} r dr} \quad (B-6)$$

Approximate values valid for $\sqrt{Dt}/\Delta \ll 1$ are

$$J_-(m) = 1 - \frac{\sqrt{Dt}}{\Delta} \frac{2m}{(2m-1)\sqrt{\pi}} \quad (B-7)$$

$$J_+(m) = \frac{\sqrt{Dt}}{\Delta} \frac{2m}{(2m+1)\sqrt{\pi}} \quad (B-8)$$

The derivation of solution (B-4) is given as follows.

Let \bar{c} = Laplace transform of c ; therefore,

$$\bar{c} = \int_0^{\infty} e^{-pt} c dt \quad (B-9)$$

Then the transform of the basic problem is

$$D \left(\frac{d^2 \bar{c}}{dr^2} \right) + \left(\frac{1}{r} \frac{d \bar{c}}{dr} \right) - p \bar{c} = -c_{oo} \quad (B-10)$$

where c_{oo} , a function of r , is the initial value of c :

$$c_{oo} = \begin{cases} 1 & r < a \\ 0 & a < r \end{cases}$$

Solving for $r < a$ yields

$$\bar{c} = AI_0(qr) + BK_0(qr) + 1/p \quad (B-11)$$

where I_0 and K_0 are the modified Bessel functions; $q = \sqrt{p/D}$; and A and B are constants of integration. Now $B = 0$ because $K_0 \rightarrow \infty$ as $r \rightarrow 0$.

Solving for $a < r$ gives

$$\bar{c} = HI_0(qr) + GK_0(qr) \quad (B-12)$$

where H and G are constants of integration and $H = 0$ because $I_0 \rightarrow \infty$ as $r \rightarrow \infty$.

Both \bar{c} and $d\bar{c}/dr$ are continuous at $r = a$. Therefore,

$$AI_0(qa) + 1/p = GK_0(qa) \quad (B-13)$$

$$AI_0'(qa) = GK_0'(qa) \quad (B-14)$$

Then

$$A = \frac{qa \dot{K}_0(qa)}{p} \quad (B-15)$$

$$G = \frac{qa \dot{I}_0(qa)}{p} \quad (B-16)$$

by use of $K_0(x)\dot{I}_0(x) - I_0(x)\dot{K}_0(x) = 1/x$. Therefore,

$$\bar{c} = \begin{cases} \frac{1}{p} - \frac{qa K_1(qa) I_0(qr)}{p} & r < a \\ \frac{qa I_1(qa) K_0(qa)}{p} & a < r \end{cases} \quad (B-17)$$

$$(B-18)$$

Early time approximation is as follows:

$$\frac{\sqrt{Dt}}{\Delta} \ll 1 \sim \frac{1}{q\Delta} \ll 1 \sim \frac{1}{qa} \ll 1$$

Then

$$K_0(qa) \doteq K_1(qa) \doteq \sqrt{\frac{\pi}{2qa}} e^{-qa} \quad (B-19)$$

$$I_0(qa) \doteq I_1(qa) \doteq \frac{e^{qa}}{\sqrt{2\pi qa}} \quad (B-20)$$

$$\bar{c} \doteq \begin{cases} \frac{1}{p} - \frac{1}{2p} \sqrt{\frac{a}{r}} e^{-q(a-r)} & r < a \\ \frac{1}{2p} \sqrt{\frac{a}{r}} e^{-q(r-a)} & a < r \end{cases} \quad (B-21)$$

$$(B-22)$$

Inversion of the transforms gives

$$c = \begin{cases} 1 - \frac{1}{2} \sqrt{\frac{a}{r}} \operatorname{erfc} \frac{a-r}{2\sqrt{Dt}} & r < a \\ \frac{1}{2} \sqrt{\frac{a}{r}} \operatorname{erfc} \frac{r-a}{2\sqrt{Dt}} & a < r \end{cases} \quad \begin{matrix} \text{(B-23)} \\ \text{(B-24)} \end{matrix}$$

With $J_+(m)$ and $J_-(m)$ defined after equation (B-4) and with $I_+(m)$ and $I_-(m)$ being the integrals of the concentration in those definitions, one finds

$$J_+(m) = \frac{I_+(m)}{\int_{m\Delta}^{(m+1)\Delta} r dr} = \frac{2}{(2m+1)\Delta^2} I_+(m)$$

$$I_+(m) = \int_{m\Delta}^{(m+1)\Delta} \frac{1}{2} \sqrt{\frac{a}{r}} \operatorname{erfc} \frac{r-a}{2\sqrt{Dt}} r dr \quad \text{(B-25)}$$

where $a = m\Delta$. The order of accuracy is $1/Q$. Approximations correct to this order can be found as follows:

$$J_-(m) = 1 - \frac{2}{(2m-1)\Delta^2} I_-(m)$$

$$I_-(m) = \int_{(m-1)\Delta}^{m\Delta} \frac{1}{2} \sqrt{\frac{a}{r}} \operatorname{erfc} \frac{a-r}{2\sqrt{Dt}} r dr \quad \text{(B-26)}$$

Let $Q = \Delta/2\sqrt{Dt}$. Then $Q \gg 1$ by assumption. Integrations are needed to order of accuracy $1/Q$.

Function $\operatorname{ierfc}(x)$ is defined by

$$\int_x^\infty \operatorname{erfc}(x) dx = \frac{1}{\sqrt{\pi}} e^{-x^2} - x \operatorname{erfc}(x) \quad (\text{B-27})$$

$$I_+(m) = \int_a^{a+\Delta} \frac{1}{2} \sqrt{ar} \operatorname{erfc} \frac{r-a}{2\sqrt{Dt}} dr \quad a = m\Delta \quad (\text{B-28})$$

Let $x = (r - a)/2\sqrt{Dt}$. Then $r = a(1 + x/mQ)$ and

$$\begin{aligned} I_+(m) &= \int_0^Q \frac{1}{2} a \sqrt{1 + x/mQ} \operatorname{erfc}(x) \frac{a}{mQ} dx \\ &= \frac{a^2}{2mQ} \int_0^Q \sqrt{1 + x/mQ} \operatorname{erfc}(x) dx \\ &= \frac{m\Delta^2}{2Q} [H_+(m) + K_+(m)] \end{aligned}$$

where

$$\begin{aligned} H_+ &= \int_0^1 \sqrt{1 + x/mQ} \operatorname{erfc}(x) dx \\ K_+ &= \int_0^Q \sqrt{1 + x/mQ} \operatorname{erfc}(x) dx \end{aligned}$$

H_+ can be approximated by

$$\begin{aligned} H_+ &= \int_0^1 \left[1 + \frac{1}{2} \frac{x}{mQ} + \dots \right] \operatorname{erfc}(x) dx \\ &\approx \int_0^1 \operatorname{erfc}(x) dx \end{aligned}$$

and to lowest (Q^0) order

$$\begin{aligned} H_+ &= -\text{ierfc}(x) \Big|_0^1 \\ &= \frac{1}{\sqrt{\pi}} - \text{ierfc}(1) \end{aligned} \quad (\text{B-30})$$

For H_- we get

$$\begin{aligned} H_- &= \int_1^Q \sqrt{1 + x/mQ} \text{erfc}(x) dx \\ &= \sqrt{1 + x/mQ} (-\text{ierfc}(x)) \Big|_1^Q - \int_1^Q (-\text{ierf}(x)) \frac{1}{2mQ} \left(1 + \frac{x}{mQ}\right)^{-1/2} dx \end{aligned}$$

Then

$$H_- = \text{ierfc}(1) \quad (\text{B-31})$$

to lowest order. Therefore,

$$\begin{aligned} I_+(m) &= \frac{m \Delta^2}{2 Q \sqrt{\pi}} \\ J_+(m) &= \frac{m}{(2m+1)Q\sqrt{\pi}} \end{aligned}$$

For $I_-(m)$ we get

$$I_-(m) = \int_{a-\Delta}^a \frac{1}{2} \sqrt{ar} \text{erfc} \frac{a-r}{2\sqrt{Dt}} dr$$

where

$$a = m\Delta$$

$$Q = \Delta/2\sqrt{Dt}$$

Then, with $z = (a - r)/2\sqrt{Dr}$, $r = a(1 - x/mQ)$. Thus,

$$I_-(m) = \frac{a^2}{2mQ} \int_0^Q \sqrt{1 - x/mQ} \operatorname{erfc}(x) dx$$

$$I_-(m) = \frac{a^2}{2mQ} \frac{1}{\sqrt{\pi}} \quad (B-32)$$

to lowest order, as before.

$$J_-(m) = \frac{m}{(2m - 1)Q\sqrt{\pi}} \quad (B-33)$$

Appendix C

DC TRANSMISSION LINE MODEL

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1      REM "SCC TL DC 16/April/1985
2      REM "Transmission Line Model for Stress Corrosion Cracking
3      REM "BY M.C.H.McKubre
10     PRINT CHR$(13); CHR$(4); "SAVE SCC TL DC#60"
500    DIM Zn(9,200),Zm(26)
520    F = 96478
600    DATA 14,.IDC,AMPS,0,.WIDTH,CM,10,.HEIGHT,CM,5,.LENGTH,CM,.1,
      .ANGLE,RAD,.02,.BULK,pH,--,6,.RHO-E,OHM-CM,20,.RHO-S,OHM-CM,1E-5,
      .GAMMA,CM,1E-4,#.E-/ATOM,2,INTERVAL,SEC.,3600,NUMBER,SEGMENTS,20,
      TOLERANCE,MV,.1,MAX.ITER.,LOOPS,99
620    DATA 26,IO.M/M^A+,A.CM-2,1E-3,V..M/M^A+,VOLT,0,IO.M/MO,A
      .CM-2,1E-5,V..M/MO,VOLT,.1,IO.H/H2,A.CM-2,1E-5,V..H/H2,VOLT,.2,
      K,---,1E-6,MONOLAYER,COUL/CM2,1E-4,N*F*MW*RHO,COUL/CM^3,8.4E7,D,
      CM2.S-1,2E-5,PASSIVE,1,A.CM-2,1E-6,?,?,0
700    RESTORE : READ II: FOR I = 1 TO II: READ ZQ$,ZT$,Zm(I): NEXT I:
      READ IJ: FOR I = 1 + II TO IJ: READ ZQ$,ZT$,Zm(I): NEXT I:N% = Zm(12)

1000   TEXT : HOME : VTAB 3: PRINT "PROGRAM OPTIONS ARE:: PRINT
1010   PRINT : PRINT "1....SET UP NEW CONSTANTS"
1020   PRINT : PRINT "2....CALCULATE STEADY STATE"
1030   PRINT : PRINT "3....INITIALGUESS OF V"
1040   PRINT : PRINT "4....SAVE ARRAY TO DISK"
1050   PRINT : PRINT "5....SEND ARAY TO PIPELINE"
1090   PRINT : PRINT : PRINT "WELL ? " : GET ZQ$: IF ZQ$ = "0" THEN HOME :
      VTAB 15: PRINT "PROGRAM EXITED - GOTO 1000 TO RESUME": END
1100   IF VAL (ZQ$) > 5 THEN 1000
1120   ON VAL (ZQ$) GOTO 1500,2000,3000,4000,5000
1140   GOTO 1000
1500   GOSUB 1510: GOTO 1000
1510   HOME : VTAB 2: PRINT "SET-UP CONSTANTS - PAGE#1"
1520   RESTORE : READ II: FOR I = 1 TO II: READ ZQ$,ZT$,J: VTAB (3 + I): HTAB 4:
      PRINT I; " ";ZQ$;: HTAB 20: PRINT Zm(I);: HTAB 12: PRINT ZT$: NEXT I
1540   VTAB 23: INPUT "HIT # TO MODIFY ";ZQ$:
      IF VAL (ZQ$) < 1 OR VAL (ZQ$) > II THEN 1600
1560   II = VAL (ZQ$): FLASH : VTAB (II + 3): HTAB (1): PRINT "=" : VTAB 22: RESTORE :
      READ N: FOR I = 1 TO II: READ ZQ$,ZT$,N: NEXT I: NORMAL : PRINT
      "CHANGE ";ZQ$;: INPUT " TO ";ZQ$: IF ZQ$ < > "" THEN Zm(II) = VAL (ZQ$)
1580   VTAB 22: HTAB 32: PRINT ZT$: GOTO 1500
1600   HOME : VTAB 2: PRINT "SET-UP CONSTANTS -- PAGE#2"
1620   RESTORE : READ II: FOR I = 1 TO II: READ ZQ$,ZT$,J: NEXT I: READ IJ:
      FOR I = II + 1 TO IJ: READ ZQ$,ZT$,N: VTAB (3 + I - II): HTAB 4: PRINT I;
      ";ZQ$;: HTAB 20: PRINT Zm(I);: HTAB 32: PRINT ZT$: NEXT I
1640   VTAB 23: INPUT "HIT # TO MODIFY ";ZQ$: IF VAL (ZQ$) = 0 THEN RETURN
1650   IF VAL (ZQ$) < II OR VAL (ZQ$) > IJ THEN 1510
1660   IJ = VAL (ZQ$): VTAB 22: RESTORE : READ N: FOR I = 1 TO II: READ ZQ$,ZT$,N: NEXT I:
      READ N: FOR I = II + 1 TO IJ: READ ZQ$,ZT$,N: NEXT I: NORMAL : PRINT "CHANGE
      ";ZQ$;: INPUT " TO ";ZQ$: IF ZQ$ < > "" THEN Zm(IJ) = VAL (ZQ$)
1680   VTAB 22: HTAB 32: PRINT ZT$: GOTO 1600

2000   HOME : VTAB 2: PRINT "CALCULATING STEADY STATE CONDITIONS"
2010   PRINT CHR$(13); CHR$(4); "PR#1": PRINT CHR$(15):
      PRINT CHR$(9); "132N": PRINT CHR$(12)
2012   RESTORE : READ II: FOR I = 1 TO II: READ ZQ$,ZT$,J: PRINT I; " ";ZQ$; " = ";Zm(I); " ";ZT$:
      NEXT I: READ IJ: FOR I = II + 1 TO IJ: READ ZQ$,ZT$,J: PRINT I; " ";ZQ$; " = ";Zm(I); " ";ZT$:
      NEXT I: PRINT : PRINT "VERSION: ";: LIST 10
2014   ZQ$ = " / ": PRINT "LOOP";ZQ$;"NQ";ZQ$;"G";ZQ$;"SI";ZQ$;"I";ZQ$;"V";ZQ$ = " "

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2020 :SI = Zm(1)
2040 N% = Zm(12): REM "# OF SEGMENTS
2044 C = 77.4: REM "Ft.SRT
2046 T = 0: REM "TIME=0
2100 Zn(0,0) = 0:Zn(7,0) = I0 ^(- Zm(6)):Zn(8,0) = Zn(7,0) ^Zm(10) / Zm(21): FOR N = 1 TO N%:
FOR M = 0 TO 6:Zn(M,N) = 0: NEXT M:Zn(7,N) = Zn(7,0):Zn(8,N) = Zn(8,0):Zn(9,N) = I:
NEXT N: REM "INITIALISE ARRAY
2120 IF Zn(1,0) = 0 THEN Zn(1,0) = (Zm(16) + Zm(20)) / 2: REM "INITIAL GUESS
2200 LL = 0:G = 32:NQ = 0: REM "LOOP COUNTER & INITIAL VSTEP (MV)
2220 SI = Zm(1):I = 0:LL = LL + I: FOR N = 1 TO N%
2240 GOSUB 10000:TI = Zn(4,N) + Zn(5,N) + Zn(6,N):
REM "CALCULATE INTERFACIALCURRENTS
2250 Zn(2,N) = Zm(8) * (Zm(4) / N%) / (Zm(2) * Zm(3)): REM "RS
2260 Zn(3,N) = Zm(7) / (2 * Zm(2) * (N% + 1 - N) * TAN(Zm(5))): REM "RE
2270 Zn(0,N) = Zn(0,N - 1) + Zn(2,N) * (SI - TI): REM "VS
2280 Zn(1,N) = Zn(1,N - 1) - Zn(3,N) * (SI - TI): REM "VE
2290 I = I + TI: REM "MOVING SUM I
2299 NEXT N
2300 IF ABS(G) < Zm(13) THEN 2500: REM "SUCCESSFUL ITERATION
2301 ZQ$ = " ": PRINT LL:ZQ$:NQ:ZQ$:G:ZQ$:SI:ZQ$:I:ZQ$:Zn(1,0)
2305 GOSUB 9000: REM "READ KEYBOARD
2310 IF I < SI THEN 2400
2320 REM "VOLTAGE TOO LARGE
2330 IF NQ = 1 THEN G = G / 2
2340 NQ = - 1: REM "LAST LOOP FLAG
2350 Zn(1,0) = Zn(1,0) - G / 1000: GOTO 2220
2400 REM "VOLTAGE TOO SMALL
2410 IF NQ = - 1 THEN G = G / 2
2420 NQ = 1:Zn(1,0) = Zn(1,0) + G / 1000: GOTO 2220
2500 REM "SUCCESSFUL ITERATION TO FIND DC CONDITION @ TIME T
2520 PRINT : PRINT " V = ";Zn(1,0);" VOLTS, I/I.SUM = ";Zm(1);"/;" AMPS";", ERROR =
";G;"MV, TIME = ";LT;" HOURS, LENGTH = ";Zm(4);" CM": PRINT " CRACK GROWTH =
";DL / Zm(11);" CM/S, TIP PH = "; - LOG(Zn(7,N%)) / LOG(10): PRINT
2540 LT = LT + Zm(11) / 3600: REM "TIME
2549 PRINT "BEFORE DELTA-C":ZQ$ = " ": FOR N = 0 TO N% STEP N% / 5:
FOR M = 0 TO 6:PRINT Zn(M,N):ZQ$: NEXT M: PRINT N: NEXT N: PRINT : PRINT
2560 FOR N = 1 TO N%: GOSUB 11000: NEXT N: REM "NOW SOLVE
FOR DELTA-CONCENTRATIONS
2580 Zn(4) = Zn(4) + DL: FOR N = 1 TO N%: FOR M = 7 TO 8:Zn(M,N) = Zn(M,N) * ((Zm(4) - DL)
/ Zm(4)) ^2: NEXT M:Zn(9,N) = Zn(9,N) * (Zn(4) - DL) / Zm(4): NEXT N: REM "C
SPREAD-OUT WITH CRACK GROWTH
2599 PRINT "BEFORE DIFFUSION":ZQ$ = " ": FOR N = 0 TO N% STEP N% /
5:PRINTZn(0,N):ZQ$:Zn(1,N):ZQ$: FOR M = 4 TO 9: PRINT Zn(M,N):ZQ$: NEXT M: PRINT
N: NEXT N:PRINT : PRINT
2600 REM "CALCULATE DIFFUSION
2620 ZZ(0) = (N% / Zm(4)) * (Zm(24) * Zm(11) * 3.14) ^ .5: REM CHI
2640 FOR N = N% TO 1 STEP - 1: GOSUB 12000: NEXT N
2699 PRINT "AFTER DIFFUSION":ZQ$ = " ": FOR N = 0 TO N%: FOR M = 1 TO 3 STEP 2: PRINT
Zn(M,N):ZQ$: NEXT M: FOR M = 4 TO 9: PRINT Zn(M,N):ZQ$: NEXT M: PRINT N: NEXT
N: PRINT : PRINT
2920 LL = 0:G = 4:NQ = 0: GOTO 22

3000 HOME : VTAB 4: PRINT "INITIAL GUESS OF VDC = ";Zn(1,0): PRINT : INPUT "CHANGE
TO":ZQ$: IF ZQ$ = "0" THEN 1000
3020 IF VAL(ZQ$) < > 0 AND ABS(VAL(ZQ$)) < 2 THEN Zn(1,0) = VAL(ZQ$)
3040 GOTO 1000

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5000 REM "OUTPUT DATA TO PIPELINE
5010 GOSUB 5020: GOTO 1000
5020 PRINT CHR$ (13); CHR$ (4); "PR#1": PRINT CHR$ (9); "132N": PRINT CHR$ (15)
5040 FOR N = 0 TO N%: FOR M = 0 TO 6: PRINT Zn(M,N); " ";; NEXT M: PRINT N: NEXT N
5080 PRINT CHR$ (13); CHR$ (4); "PR#0": RETURN

9000 REM "READ KEYBOARD
9010 ZZ(3) = PEEK ( - 16384) - 128: POKE - 16386,0: IF ZZ(3) < 1 THEN RETURN
9020 PRINT CHR$ (13); CHR$ (4); "PR#0"
9030 IF ZZ(3) = 16 THEN PRINT "": GOSUB 1510: REM "CHANGE PARAMETERS
9040 IF ZZ(3) = 20 THEN POP : GOTO 1000
9090 PRINT CHR$ (13); CHR$ (4); "PR#1": IF ZZ(3) = 16 THEN GOSUB 9100
9099 RETURN
9100 REM "PRINT PARAMETERS
9110 RESTORE : READ II: FOR I = 1 TO II: READ ZQ$,ZT$,J: PRINT I;"; "ZQ$;" = "Zm(1);" "ZT$;
NEXT I: READ II: FOR I = II + 1 TO II: READ ZQ$,ZT$,J: PRINT I;"; "ZQ$;" = "Zm(1);" "ZT$;
NEXT I: PRINT : RETURN
9999 PRINT CHR$ (13); CHR$ (4); "SAVE SCC TL DC#6A": END

10000 REM "INTERFACIAL ELECTRICS
10100 REM "METAL DISSOLUTION @ CRACK TIP DUE TO STRESS
10110 Zn(4,N) = 0: IF N < N% THEN 10200
10120 ZZ(0) = Zm(15) * Zm(9) * Zm(2) * TAN (Zm(5)):ZZ(1) = Zm(10):ZZ(2) = Zm(16):ZZ(3) =
Zn(8,N): GOSUB 10800: REM "B-V 0=10,1=N,2=V0,3=C
10140 Zn(4,N) = ZZ(5):DL = Zn(4,N) * Zm(11) / (Zm(23) * Zm(9) * Zm(5) * Zm(2)): IF DL < 0 THEN
DL = 0: REM "DELTA-L
10200 REM "CHEMICAL PASSIVATION
10300 REM "HYDROGEN ION REDUCTION
10320 ZZ(0) = Zm(19) * 2 * Zm(2) * (Zm(4) / N%):ZZ(1) = 1:ZZ(2) = Zm(20):ZZ(3) = Zn(7,N): GOSUB
10800: REM "B-V 0=10,1=N,2=V0,3=C
10340 Zn(5,N) = ZZ(5)
10400 REM "METAL OXIDE REDUCTION
10410 ZZ(0) = Zn(9,N): IF ZZ(0) > 1 THEN ZZ(0) = 1
10420 ZZ(0) = ZZ(0) * Zm(17) * 2 * Zm(2) * (Zm(4) / N%):ZZ(1) = Zm(10):ZZ(2) = Zm(18):ZZ(3) =
Zn(7,N): GOSUB 10800: REM "B-V 0=10,1=N,2=V0,3=C
10440 Zn(6,N) = ZZ(5)
10500 REM "METAL DISSOLUTION ON CRACK WALLS
10510 ZZ(9) = (1 - Zn(9,N)): IF ZZ(9) < 0 THEN ZZ(9) = 0: REM "ACTIVE/PASSIVE
10520 ZZ(0) = Zm(15) * 2 * Zm(2) * (Zm(4) / N%):ZZ(1) = Zm(10):ZZ(2) = Zm(16):ZZ(3) = Zn(8,
N): GOSUB 10800: REM "B-V 0=10,1=N,2=V0,3=C
10540 ZZ(0) = (1 - Zn(9,N)): IF ZZ(0) < 0 THEN ZZ(0) = 0: REM THETA
10560 IF ZZ(0) > 0 THEN ZZ(6) = ZZ(5) * ZZ(0): GOTO 10590: REM "ACTIVE KINETICS
10580 ZZ(6) = SGN (ZZ(5)) * ABS (Zm(25) * 2 * Zm(2) * (Zm(4) / N%) * (1 - Zn(8,N)) / Zn(9,N)): IF
ABS (ZZ(5)) < ABS (ZZ(6)) THEN ZZ(6) = ZZ(5): REM "PASSIVE DIFFUSION
10590 Zn(4,N) = Zn(4,N) + ZZ(6)
10600 RETURN
10800 REM "COMPUTE BUTLER-VOLMER I
10805 ZZ(2) = Zn(1,N - 1) - Zn(0,N - 1) - ZZ(2) + (2 / (Zm(10) * C)) * LOG (ZZ(3)): REM "ZETA
INCLUDING CONC.
10810 ZZ(4) = ZZ(1) * C * (ZZ(2)): IF ABS (ZZ(4)) > 30 THEN ZZ(4) = SGN (ZZ(4)) * 30
10820 ZZ(5) = ZZ(0) * ( EXP (ZZ(4)) - EXP ( - ZZ(4)))
10830 ZZ(6) = Zm(2) * Zm(5) * (Zm(4) / N%) ^ 2 * (2 * N% - 2 * N + 1): REM "VOLUME
10839 IF N = N% AND ZZ(5) > 0 THEN 10849: REM "NO LIMIT TO M->MO @ TIP
10840 IF ABS (ZZ(5)) > ABS (99 * ZZ(1) * F * ZZ(3) * ZZ(6) / Zm(11)) THEN ZZ(5) = SGN (ZZ(5)) *
99 * ZZ(1) * 96478 * ZZ(3) * ZZ(6) / Zm(11): REM "MAX DELTA-C

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10849 REM "ZQ$ = " ": FOR NN = 0 TO 6: PRINT ZZ(NN);ZQ$;: NEXT NN: PRINT N
10850 RETURN

11000 REM "INTERFACIAL CHEMISTRY
11020 ZZ(0) = Zm(2) * Zm(5) * (Zm(4) / N%) ^ 2 * (2 * N% - 2 * N + 1): REM "V
11040 ZZ(1) = Zn(4,N) * Zm(11) / (Zm(10) * F * ZZ(0)): IF ZZ(1) > Zn(8,N) / 2 THEN ZZ(1) =
Zn(8,N) / 2: REM "DELTA METAL IONS
11060 ZZ(2) = (Zn(5,N) + Zn(6,N)) * Zm(11) / (F * ZZ(0)): IF ZZ(2) > Zn(7,N) / 2 THEN ZZ(2) =
Zn(7,N) / 2: REM "DELTA PROTONS
11080 ZZ(3) = Zn(6,N) * Zm(11) / (Zm(10) * Zm(22) * Zm(2) * (Zm(4) / N%)): IF ZZ(3) > Zn(9,N) / 2
THEN ZZ(3) = Zn(8,N) / 2: REM "DELTA METAL OXIDE
11100 Zn(7,N) = Zn(7,N) - ZZ(2): Zn(8,N) = Zn(8,N) - ZZ(1): Zn(9,N) = Zn(9,N) - ZZ(3): REM:
"ELECTROCHEMISTRY
11120 ZZ(9) = (Zn(8,N) - ZZ(8)) * F * Zm(10) / (Zm(23) * Zm(2) * (Zm(4) / N%) * 2): IF ZZ(9)
> Zn(9,N) / 2 THEN ZZ(9) = Zn(9,N) / 2: REM "DELTA OXIDE
11140 ZZ(5) = Zn(9,N): IF ZZ(5) > 1 THEN ZZ(5) = 1: REM "MO ACTIVITY
11160 Zn(7,N) = (Zn(8,N) * Zm(21) / ZZ(5)) ^ (1 / Zm(10)): Zn(8,N) = ZZ(5) * (Zn(7,N) ^ Zm(10)) /
Zm(21): Zn(9,N) = Zn(9,N) - ZZ(9): REM "CHEMISTRY
11600 RETURN

12000 REM
12020 ZZ(3) = 2 * (N% - N): ZZ(1) = (ZZ(3) + 3) / (ZZ(3) + 1): REM "V N-1/N
12040 ZZ(2) = (ZZ(3) - 1) / (ZZ(3) + 1): IF ZZ(2) < 0 THEN ZZ(2) = 0: REM "V N+1/N
12080 IF ZZ(0) > .5 THEN 12200
12100 REM "SHORT TIME
12120 FOR M = 7 TO 8: Zn(M,N) = Zn(M,N) * (1 - ZZ(0)) + ZZ(1) * ZZ(0) * (3 * Zn(M,N) + Zn(M,N -
1)) / 4 + ZZ(2) * ZZ(0) * (3 * Zn(M,N) + Zn(M,N + 1)) / 8: NEXT M
12160 RETURN
12200 REM "LONG TIME
12220 FOR M = 7 TO 8: Zn(M,N) = ZZ(1) * (3 * Zn(M,N) + Zn(M,N - 1)) / 8 + ZZ(2) * (3 * Zn(M,N)
+ Zn(M,N + 1)) / 8: NEXT M
12260 RETURN

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